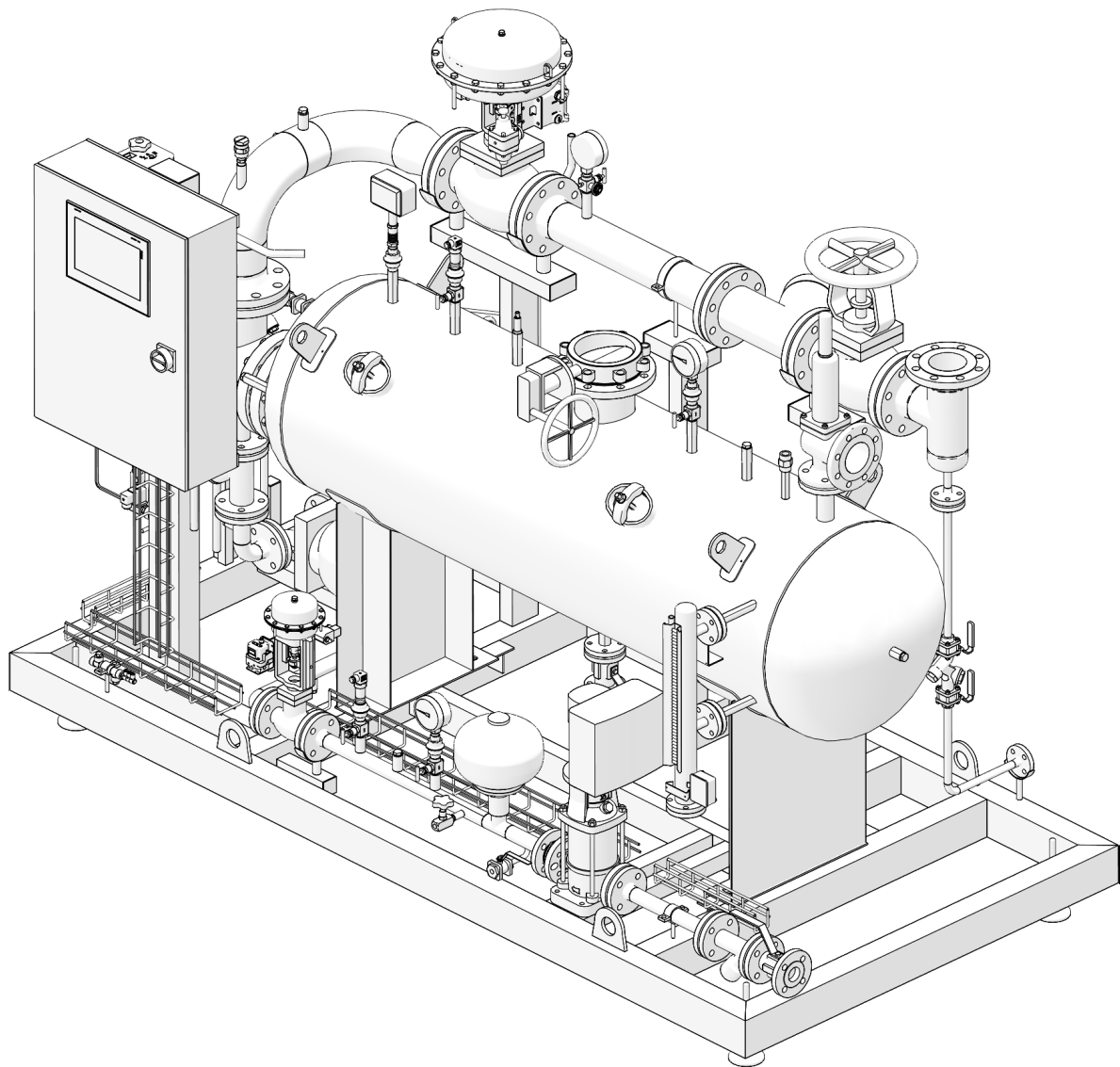




## CSG-FB

# Clean steam generation system for Food & Beverage

## Installation and Maintenance Instructions



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# 1. Safety information

In addition to putting your personnel at risk of death or serious harm, failure to comply with the instructions, recommendations and guidance set out in this document may jeopardise your warranty rights. Further, use of the product(s) otherwise than in accordance with this document will be undertaken entirely at your own risk. To the fullest extent legally permitted, Spirax Sarco excludes all responsibility and liability for any and all loss or damage caused in the event that the practices and procedures detailed in this document have not been followed.

Safe operation of these products can be guaranteed only if they are properly installed, commissioned and maintained by a qualified person (see Section 1.11) in compliance with the related operating instructions. General installation and safety instructions for pipeline and plant construction and also the proper use of tools and safety equipment must also be complied with.

## General safety notes

This manual is intended to cover the installation, start-up and maintenance procedures of the CSG-FB indirect clean steam generator and must be read in conjunction with the installation and maintenance manuals (IM) of the single components of the unit and related additional safety notes.

## Precautions when lifting the unit

The CSG-FB indirect clean steam generator must be lifted from the base depending on the size, adopting a suitable forklift or transpallet for 020 and 050 sizes and using the lifting eye bolts installed on the base frame for 110 and 160 sizes.



**Caution  
or  
Warning**

Do not lift the CSG-FB indirect clean steam generator by any other part except from the base.


Note: always leave sufficient space around the system for future maintenance operations.

## Warnings

1. The unit is designed and constructed to withstand the intensity of work in ordinary use.
2. Use of the product for any other purpose, or failure to install the product in compliance with these Installation and Maintenance Instructions, may damage the product and also cause serious injuries to operating personnel.
3. Before carrying out any installation and maintenance procedure, always check that all primary steam, condensate and water return lines on the secondary have been isolated.
4. Make sure that residual pressure in the system and in pipework has been vented to atmospheric level.
5. To avoid the risk of burns, allow parts to cool before carrying out any type of operation.
6. Always wear suitable protective clothing before carrying out any installation or maintenance activity.
7. This product is intended to be connected into a system that can operate an EC1935 compliant process. To minimise the risk of non-intentionally added substances in the system, it is essential that an appropriate CIP (cleaning in place) cycle is carried out by the end user prior to first use in a food contact application. A list of the materials that could come directly or indirectly into contact with foodstuffs can be found in the Declaration of Compliance available for this product.

## 1.1 Intended use

Referring to the installation and maintenance instructions and the nameplate of the unit and the Technical Specifications, check that the product is suitable for intended use/application.

EMEA - The CSG-FB indirect clean steam generator complies with the requirements of the EU Pressure Equipment Directive/UK Pressure Equipment (Safety) Regulations and is  marked.

America's - The CSG-FB indirect clean steam generator complies with the requirements of the ASME Pressure vessel code and ASME U Stamp upon request.

Asia Pacific - The CSG-FB indirect clean steam generator complies with the requirements of the EU Pressure Equipment Directive/UK Pressure Equipment (Safety) Regulations Conformance to KGS / MOM and DOSH is available upon request.

- i) The product has been specifically designed for use on steam and water belonging to Group 2 of the above-mentioned Pressure Equipment Directive.
- ii) Check suitability of material, pressure and temperature and related maximum and minimum values. If the maximum operating limits of the product are lower than those of the system in which it to be inserted, or if malfunction of the product could generate dangerous overpressure or overtemperature, always insert a safety device in the system to prevent exceeding of such limits.
- iii) Determine the correct installation position and direction of flow of fluids.
- iv) The product is not designed to withstand external stresses induced by the system in which it is fitted. The installer is responsible for taking into account such stresses and for adopting adequate precautions to reduce these to a minimum.
- v) Prior to installation, remove protective covers from all connections and also protective film and packaging elements.

## 1.2 EU Pressure Equipment Directive/UK Pressure Equipment (Safety) Regulations classification

The clean steam generators CSG-FB series are classified as assembly according the EU Pressure Equipment Directive/UK Pressure Equipment (Safety) Regulations:

Product	Fluid Group	Category
CSG-FB-020	2	III
CSG-FB-050	2	III
CSG-FB-110	2	IV
CSG-FB-160	2	IV

For the category of bespoke units, refer to the "EC Declaration of Conformity" supplied with the product. Other component parts of the assembly comply with the relevant European Directives, where necessary. Please refer to specific component literature for further details.

## 1.3 Access

Ensure safe access and, if necessary, a safe working platform (suitably guarded) before attempting any work on the product. Arrange suitable lifting gear if required.

## 1.4 Lighting

Ensure adequate lighting, particularly where detailed or intricate work is required.

## 1.5 Hazardous liquids or gases in the pipeline

Take into account what is currently in the pipeline or what may have been in the pipeline at some previous time. Consider: flammable materials, substances hazardous to health, extreme temperatures.

## 1.6 Hazardous environment around the product

Consider: areas with a risk of explosion, lack of oxygen (e.g. tanks, pits), dangerous gases, extreme temperatures, hot surfaces, fire hazards (e.g. during welding), excessive noise, moving machinery.

The place of installation of the assembly must be equipped with the fire-prevention devices required by current regulations.

## 1.7 The system

Consider the effect of the work to be carried out on the entire system. Consider whether the action proposed (e.g. closing of isolating valves, electrical isolation) may put any other part of the system or personnel at risk.

Hazards may include isolation of vents or protective devices or the rendering ineffective of controls or alarms. Ensure isolating valves are opened and closed gradually to avoid shocks to the system.



### 1.8 Pressure systems

Ensure that any pressure is isolated and safely vented to atmospheric pressure.

Consider double isolation (double block and bleed) and locking or labelling of closed valves. Do not assume that the system has depressurised even when the pressure gauge indicates zero.

### 1.9 Temperature

Allow time for temperature to normalise after isolation to avoid the risk of burns and consider whether protective clothing (including safety glasses) is required.

## 1.10 Tools and consumables

Before starting work, make sure you have suitable tools and/or consumables on hand. Use only genuine Spirax Sarco replacement parts.

## 1.11 Protective clothing

Consider whether you and/or others require protective clothing to protect against hazards, such as chemicals, high/low temperatures, radiation, noise, falling objects and danger to eyes and face.

## 1.12 Permits to work

All work must be carried out or supervised by a suitably competent person. Installation and operating personnel should be trained in correct use of the product according to the Installation and Maintenance Instructions. Any formal work permit system adopted must be complied with. Where no such system is applied, a person responsible should be informed of progress of the work and, where necessary, an assistant with primary responsibility for safety should be appointed. Post "warning signs" if necessary.

## 1.13 Handling

Manual handling of large and /or heavy products may involve a risk of injury. Lifting, pushing, pulling, carrying or supporting a load by bodily force may cause injury, particularly to the back. You are advised to assess the risks, taking into account the task, the individual, the load and the working environment and use appropriate handling methods according to the circumstances of the work to be carried out.

Note: if it is necessary to use slings for lifting, it is good practice to fit these around the plate of the base unit to avoid damage to the unit.

## 1.14 Storage

Note: If the Clean Steam Generator cannot be installed and put into operation immediately upon receipt at the jobsite, certain precautions are necessary to prevent deterioration during storage.

Responsibility for integrity of the heat exchangers must be assumed by the user. Spirax Sarco will not be responsible for damage, corrosion or other deterioration of heat exchanger equipment during transit and storage. Good storage practices are important, considering the high costs of repair or replacement, and the possible delays for items which require long lead times for manufacture. The followings suggested practices are provided solely as a convenience to the user, who shall make his own decision on whether to use all or any of them.

- On receipt of the CSG-FB Steam Generation System, inspect for shipping damage to all protective covers. If damage is evident, inspect for possible contamination and replace protective covers as required. If damage is extensive, notify the carrier immediately and Spirax Sarco.
- If the CSG-FB is not to be placed in immediate service, take precautions to prevent rusting or contamination.
- Store under cover in a heated area, if possible. The ideal storage environment for CSG-FB and accessories is indoors, above grade, in a dry, low humidity atmosphere which is sealed to prevent entry of blowing dust, rain or snow. Maintain temperatures between 20 °C and 50 °C (68 °F and 122 °F) and humidity at 40% relative humidity or lower.

Note: Ambient temperature of the place where the unit will be installed must be above 0 °C (32 °F) and below 40 °C (104 °F).

## 1.15 Freezing

Precautions must be taken to protect products that are not self-draining against frost damage in environments where they may be exposed to temperatures below freezing point.

## 1.16 Disposal

As the product may contain PTFE and Viton, particular precautions must be adopted to avoid potential risks for health caused by decomposition or combustion of such materials. Unless otherwise indicated in the installation and maintenance instructions with regard to the materials of the seals, this product can be recycled and it is considered that no environmental risk exists deriving from disposal thereof provided that suitable precautions are adopted. However, its components can be checked to verify the possibility of safe disposal.

### PTFE:

- This material can be disposed of only using approved systems and never in incinerators.
- PTFE waste to be disposed of must be stocked in separate containers and must never be mixed with other waste.

Please visit the Spirax Sarco product compliance web pages

<https://www.spiraxsarco.com/product-compliance>

for up to date information on any substances of concern that may be contained within this product. Where no additional information is provided on the Spirax Sarco product compliance web page, this product may be safely recycled and/or disposed providing due care is taken. Always check your local recycling and disposal regulations.

### Viton:

- VITON waste can be sent directly to landfills when permitted and accepted by local and national regulations.
- VITON components may also be incinerated but a scrubber must be used to remove the hydrogen fluoride developed by the product, carrying out this procedure in accordance with local and national regulations.  
The components are insoluble in aquatic media.

### Electrical:

Unless otherwise stated, the electrical components within this product are recyclable and no ecological hazard is anticipated with its disposal providing due care is taken. The product should be recycled in line with local legislation.

## 1.17 Return of products

Customers and stockists are reminded that, under EC Health, Safety and Environment Law, when returning products to Spirax Sarco, they must provide information regarding any hazards and precautions to be taken due to contamination residues or mechanical damage which may represent a risk to health, safety or the environmental. This information must be provided in writing, including Health and Safety datasheets relating to any substances identified as hazardous or potentially hazardous.

## 2. General product information

### 2.1 Description

The CSG-FB indirect clean steam generator consists of a complete, safe and functional system package, ready for installation and able to produce up to 200/500/1100/1600 kg/h of clean steam (at normal operating conditions) using industrial steam as a primary energy source.

The CSG-FB series of indirect clean steam generators are designed to produce clean steam for direct injection processes within the food & beverage industry sector, where steam is considered as an ingredient.

The heat exchange is indirect, for which there is no contamination between the primary steam and the 'clean' steam produced.

### Models and applications

Size	Model	Nominal production (kg/h*)	Nominal production (lbs/hr)
	CSG-FB-020	200	441
	CSG-FB-050	500	1102
	CSG-FB-110	1100	2425
	CSG-FB-160	1600	3527

**Applications** Sterilisation of containers, generic use of clean steam.

\* Nominal steam production at reference operating conditions: primary plant steam at 10 bar g (145 psi g), production at 5 bar g (73 psi g), feedwater at 20 °C (68 °F).

### 2.2 Identification of the product

The product is identified by the nameplate fastened to the frame.

The CSG-FB unit, (Figure 1), comprises the following main parts:

- 1 Steam generator and instrumentation/accessories, protection and safety devices
- 2 Primary steam control
- 3 Condensate removal
- 4 Feedwater inlet
- 5 Electrical control panel

For a detailed list of equipment and specifications, refer to the P&ID and documentation provided.

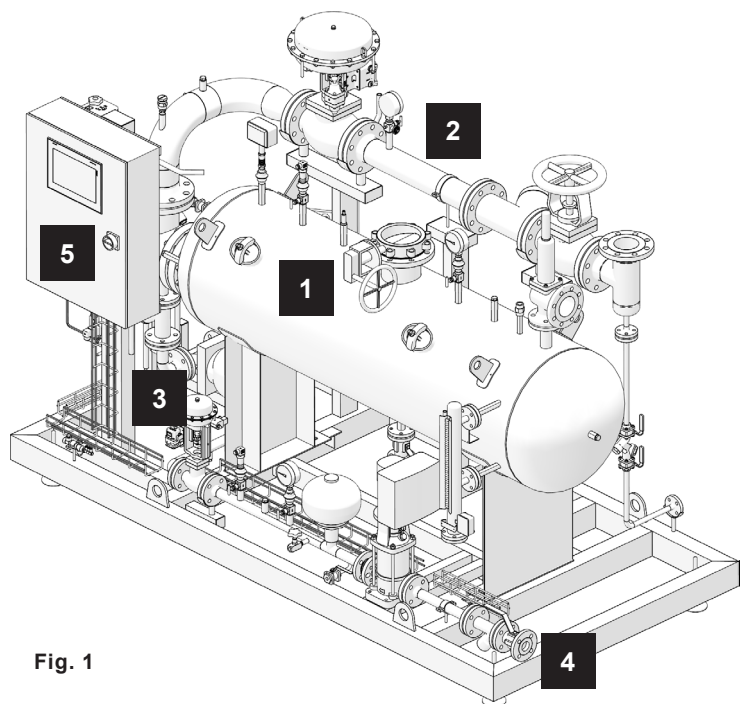


Fig. 1

#### Notes:

1. For further information concerning individual components refer to the specific technical documentation of each product.
2. Further technical information regarding the CSG-FB indirect clean steam generator can be found in TI-P664-01.

**Example of nameplate:**

**1. "CE" marking and Id. of notified body**

Unit PED category

**2. Unit model**

**3. Product Nomenclature - Series**

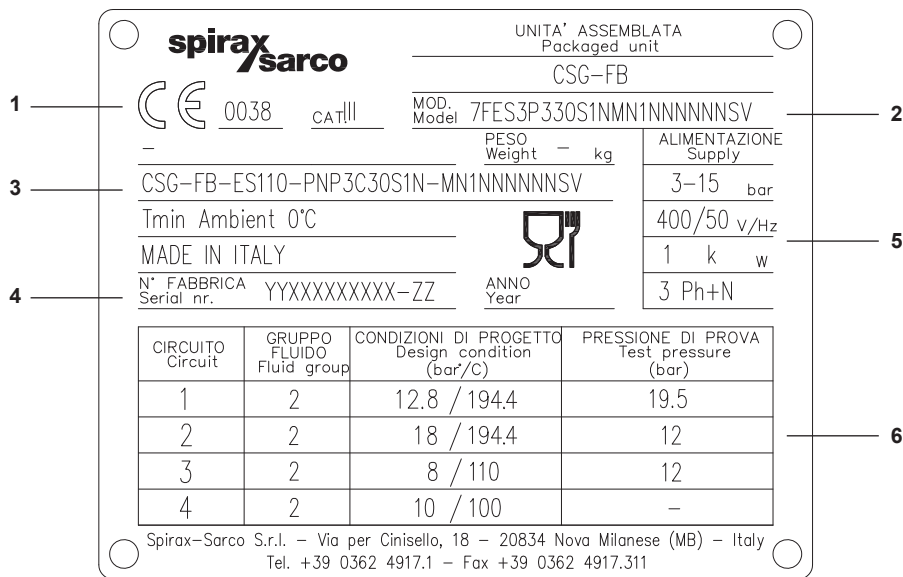
- Size
- Configuration
- Options

**4. Unit serial No.:**

- YY: year
- XXXXXX: identification number (6 or 9 digits)
- ZZ: unit progressive number
- Year of construction

**5. Electric and air supply specifications (where required)**

**6. Fluid group (PED), design conditions and circuit hydro test pressure**



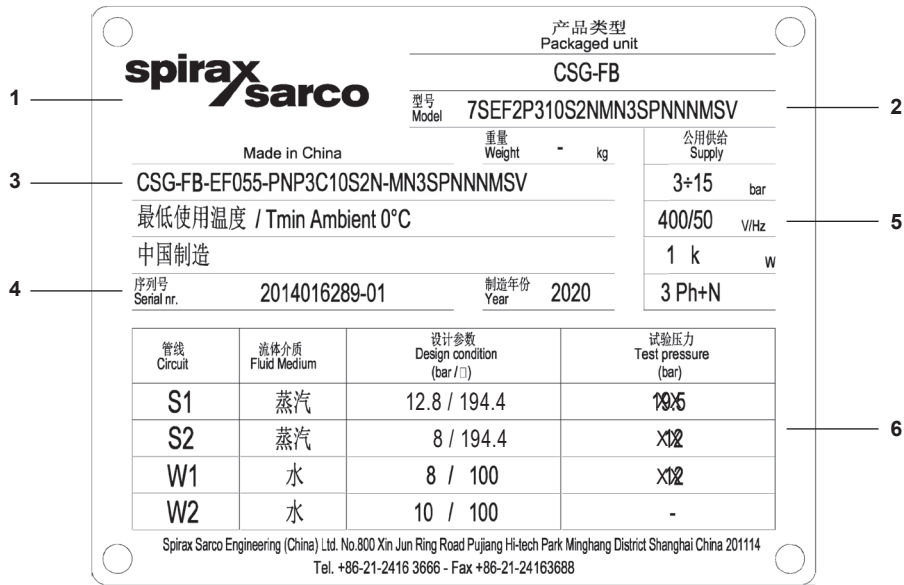
**Fig. 2**

**Note:** the pressure values in the nameplate are expressed in 'bar g'.



**Note:** the pressure values in the nameplate are expressed in 'psi g'.

**Fig. 2.1 - Americas' nameplate**



**Fig. 2.2 - Asia Pacific nameplate**

## 2.3 Product nomenclature and selection guide

The product nomenclature is based on the characteristics of the main elements and options, identified as follows:

Basic configuration	
Design code	E EN
	A ASME
	G GB
	J JBA
Shell type	S Flanged openable-shell and tube, flanged openable without integrated deaerator
Unit size	020 Up to 200 kg/h (441 lbs/hr) (at the reference operating conditions)
	050 Up to 500 kg/h (1102 lbs/hr)
	110 Up to 1100 kg/h (2425 lbs/hr)
	160 Up to 1600 kg/h (3527 lbs/hr)
Valve actuation type	PN Pneumatic (fail-safe)
	EL Electric (fail-safe)
Control	P1 ABB AC500 series + 7" display
	P2 Allen-Bradley CompactLogix 1700 series + 7" display
	P3 Siemens S7.1200 series + 7" display
	P4 Selective Control Panel (with PLC ABB AC500 series + 7" display)
Communication interface	C0 None
	C1 BACnet IP
	C2 Profinet
	C3 Modbus TCP/IP
	C4 BACnet MSTP
	C5 Profibus
	C6 Modbus RTU
	C7 BACnet (BTL cert.) IP
C8 BACnet (BTL cert.) MSTP	
Unit frame/Electrical cabinet	0 Base and cabinet made of carbon steel, painted
	1 Open frame and cabinet made of carbon steel, painted
	2 Frame w. side panels and cabinet made of carb. steel, painted
	3 Base and cabinet made of stainless steel (304) *
	4 Open frame and cabinet made of stainless steel (304) *
	5 Frame with side panels and cabinet made of stainless steel (304) *
	7 Seismic, Base and cabinet made of carb. steel, painted

\* This option/configuration is not allowed with P4 control (Selective Control Panel)

Product nomenclature and selection guide continues on next page

## 2.3 Product nomenclature and selection guide (continued)

Basic configuration		
<b>Control Panel location</b>	S	Side
<b>Insulation</b>	1	Steam generator body only
	2	Steam generator and hot piping
	3	Insulation to EnEV specification
	0	Not insulated
<b>Handling wheels and feet</b>	N	None (only plates with anchor holes are provided)
	F	Adjustable feet
	W	Pivoting wheels, lockable, with feet
<b>Plant steam inlet shut-off valve</b>	M	Manual stop valve
	AE	Automatic electric isolation valve*
<b>Plant steam line trapping</b>	N	None
	T	Plant steam line trapping station
<b>TDS control system</b>	1	Timed TDS blowdown
	2	TDS control with external probe (discontinuous metering) *
<b>Sampling cooler</b>	N	None
	S	Sample-cooler and sampling valve
<b>Feedwater pressurisation system</b>	N	None (water P > clean steam P + 0,5 bar g)
	P	Pump with VFD *
<b>Independent downstream plant protection</b>	N	None
	T	Temperature limiter *
<b>Feedwater pre-heating</b>	N	None ***
<b>Intelligent diagnostics</b>	N	None
	I1	System diagnostics *
	I3	Integrity test *
	I4	System diagnostics + Integrity test *
<b>Clean steam outlet shut-off valve</b>	N	None
	M	Manual stop valve
	AE	Automatic electric isolation valve*

\* This option/configuration is not allowed with P4 control (Selective Control Panel)

\*\*\* Bespoke energy recovery options can be developed, tailored to specific operating conditions (eg condensate subcooling or flash recovery)

Product nomenclature and selection guide continues on next page

## 2.3 Product nomenclature and selection guide (continued)

Basic configuration		
Test and certifications	S	EU PED test and CE marking of the assembly
	U	ASME U stamp
	M	MOM compliance
	K	KGS compliance
	D	DOSH compliance
	GC	GB standard in Chinese language
	GE	GB standard in English language
	SF	None (as assembly)
Level indicator	V	Viscorol (Magnetic Level Indicator)

### Product nomenclature example

CSG-FB E S 020-PN P3 C1-1 S 2 F-AE T-2 S P T N I1-AE S V

Not all configurations are available in every country. Please contact your local Spirax Sarco representative for more details.

## 2.4 Design conditions

Primary side	Design pressure	12.8 bar g	(187 psi g)	The complete condition of the design of the supplied units are reported on the P&ID.
	Design temperature	194.4 °C	(382 °F)	
Secondary side	Design pressure	8 bar g	(116 psi g)	
	Design temperature	194.4 °C	(382 °F)	
	Safety valve set pressure	7 bar g	(101.5 psi g)	
Feedwater	Design pressure	8 bar g	(116 psi g)	
	Design temperature	without pump	110 °C (230 °F)	
		with pump		

## 2.5 Operating limits

	Without pump	With pump
<b>Production</b>	Clean saturated steam, up to 6 bar g/165.0 °C (Clean saturated steam, up to 97 psi g/206 °F)	
<b>Primary side</b>	Plant steam, up to 12 bar g/191.7 °C (Plant steam, up to 174 psi g/345 °F)	
<b>Feedwater</b>	P min. ≥ P clean steam + 0.5 bar g (P min. ≥ P clean steam + 7.2 psi g)	Minimum Supply Pressure (see below)
	P max 8 bar g/T max 110 °C (P max 116 psi g/T max 230 °F)	P max 8 bar g/T max 100 °C (P max 116 psi g/T max 212 °F)

Minimum pressure of the feedwater at the inlet flange of the units equipped with pump, to avoid cavitation (NPSHR) = P' min. + dP  
dP: pressure drop along the water feed pipework, at maximum flow-rate.

P' min. depending on the water temperature:

T	°C	≤ 85	90	95	100	(*) Under water head
	(°F)	(185)	(194)	(203)	(212)	
<b>P' min.</b>	bar g	0*	0.05	0.20	0.35	
	(psi g)	(0)	(0.72)	(2.90)	(5.07)	

Minimum ambient temperature: 0 °C (32 °F).

Maximum ambient temperature: 40 °C (104 °F)

Unit designed for indoor installation, protect from freezing.

To ensure the correct operation of the clean steam generator, the inlet feed water should have the following characteristics. An excess on these values can compromise the lifetime, maintenance and efficiency of the steam generator.

**pH** 5.5 ÷ 7.5 (at 20 °C) **Hardness** ≤ 0.02 mmol/l  
(5.5 ÷ 7.5 (at 68 °F))

**Chloride** Please refer to table below **Conductivity** ≤ 20 µS/cm

Chlorides concentration limit in inlet feed water

Blowdown set	Inlet feed water pH		
	pH = 5,5	pH = 6,5	pH = 7,5
5%	≤ 0,5 mg/l	≤ 1 mg/l	≤ 3 mg/l
10%	≤ 1 mg/l	≤ 2 mg/l	≤ 6 mg/l

\* All the other characteristics and values of feed water are up to end user of the plant.

In addition to the above, for monitored TDS blowdown, a maintained concentration below a maximum of 100µS/cm is required during operation.

## 2.6 Dimensions and weights

approximate in mm (inches) and kg (lbs) of a standard unit

	Dimensions mm (inches)				Weights kg (lbs)		
	L Length	W Width	H Height	E Clearance for tube bundle extraction	Empty	In operation	Maximum
<b>CSG-FB 020</b>	2000 (79)	850 (33)	1840 (72)	1250 (49)	550 (1213)	650 (1433)	800 (1764)
<b>CSG-FB 050</b>	2350 (93)	850 (33)	1840 (72)	1300 (51)	850 (1874)	1050 (2315)	1250 (2756)
<b>CSG-FB 110</b>	2450 (96)	1450 (57)	2060 (81)	1600 (63)	1100 (2425)	1450 (3197)	1700 (3748)
<b>CSG-FB 160</b>	2950 (116)	1450 (57)	2060 (81)	2000 (78)	1550 (3417)	2050 (4519)	2450 (5401)

## 2.7 Dimensions and weights of the units with EnEV option - insulation 100 mm

approximate in mm (inches) and kg (lbs)

	Dimensions mm (inches)				Weights kg (lbs)		
	L Length	W Width	H Height	E Clearance for tube bundle extraction	Empty	In operation	Maximum
<b>CSG-FB 020</b>	2100 (83)	950 (37)	1950 (77)	1250 (49)	700 (1543)	800 (1764)	950 (2094)
<b>CSG-FB 050</b>	2500 (98)	1100 (43)	2000 (79)	1300 (51)	1000 (2205)	1200 (2646)	1400 (3086)
<b>CSG-FB 110</b>	2550 (100)	1450 (57)	2250 (89)	1600 (63)	1300 (2866)	1600 (3527)	1850 (4079)
<b>CSG-FB 160</b>	3100 (122)	1500 (59)	2250 (89)	2000 (79)	1650 (3638)	2200 (4850)	2550 (5622)

For detailed dimensions of the unit, size and position of the connections, clearance for the tube bundle extraction, weights and other constructive information, refer to the specific general arrangement drawing of the product.

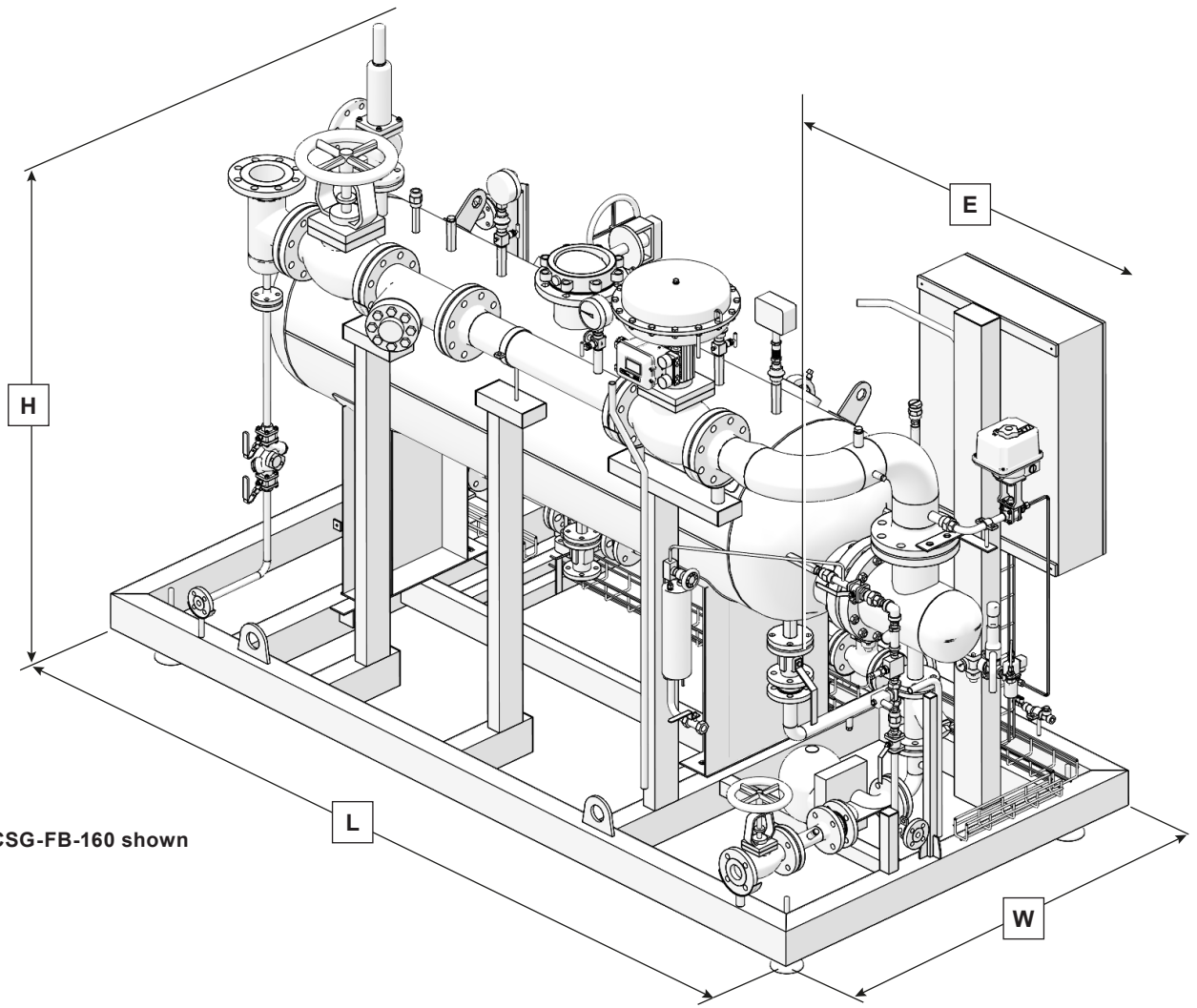


Fig. 3a CSG-FB-160 shown

# 3. Installation

## 3.1 Installation site

The correct installation of the CSG is required to ensure the safety of the package and to realise the full performance (clean steam flowrate, pressure, dryness). Therefore, it's important to consider the entire installation (see section 3.4 - Process pipework and vents).

The CSG-FB unit is designed for installation indoors with a minimum ambient temperature of 0 °C (32 °F). Installation outdoors is permitted provided that the unit is suitably protected against adverse weather conditions and freezing.

The unit is not suitable for installation in potentially hazardous zones classified as ATEX. Specific solutions can be provided on request.

## 3.2 Handling

**020/050 sizes:** The CSG-FB unit must be lifted from the base using suitable forklift or transpallet. Do not use any eyebolts of equipment on board the unit. If fitted with wheels for handling (option), the unit must be moved in safe conditions and then secured in position using the integrated mounting feet.

**110/160 sizes:** The CSG-FB unit must be lifted from the lifting eyebolts mounted on the base of the unit.



**Do not lift the unit by other parts or in any manner other than as indicated above.**

**During lifting, take into account the high centre of gravity of the unit and adopt all the necessary precautions to avoid accidental tipping over of the unit.**

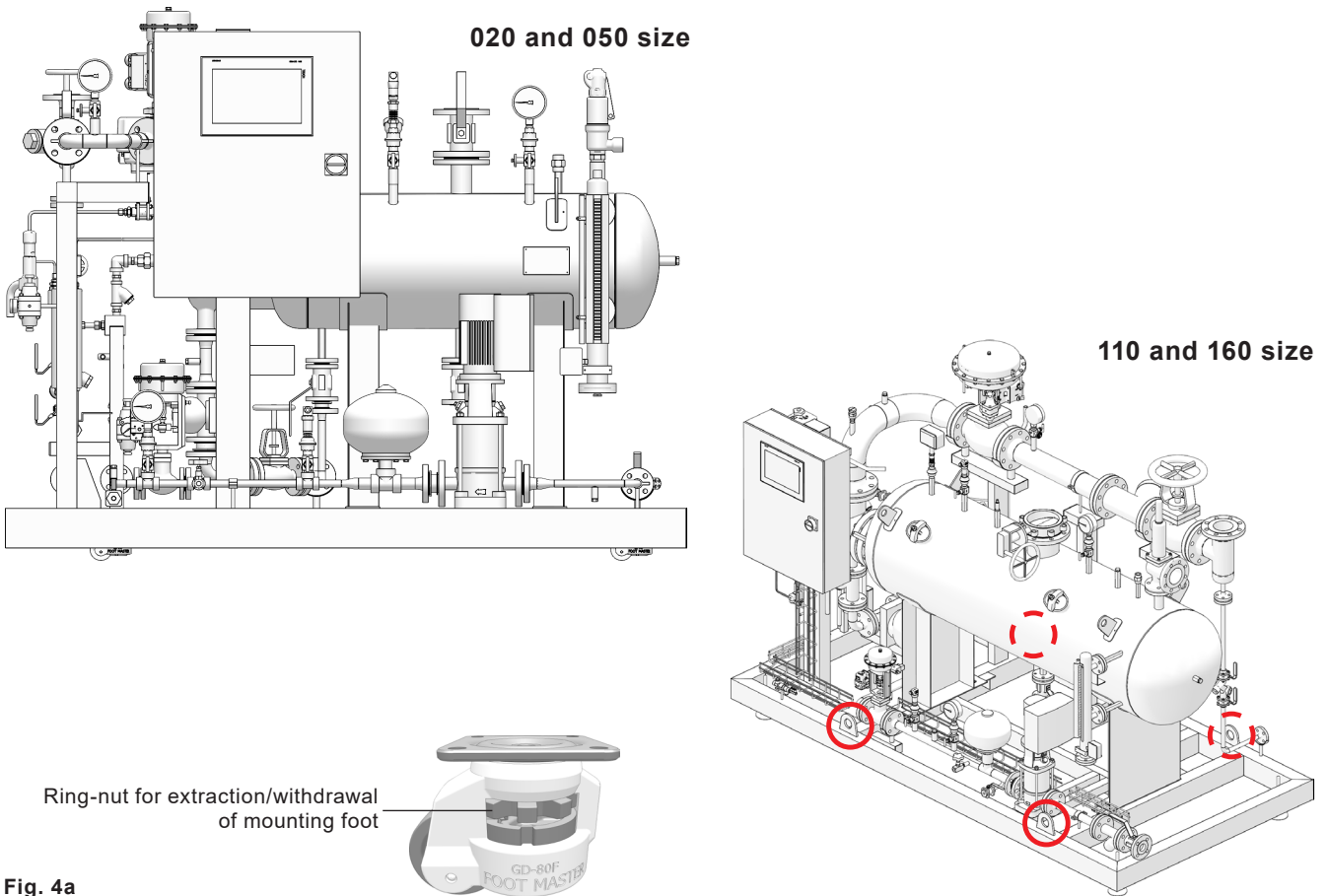


Fig. 4a

### 3.3 Positioning and fastening

The unit must be positioned on a completely flat, horizontal surface able to support its entire weight at full load. A level surface is important as the water level is used in the control system. For access to the unit, provide at least one metre of clearance around, and 0.5 m (1.64 ft) above. A space for tube bundle removal has to be considered.

### 3.4 Process pipework and vents

Each unit is provided complete with drawings indicating the position and specifications of connections to be made according to configuration and options ordered.

The main connections of the unit are as follows:

UNI-EN 1092-1 PN16/25/40 connection flanges

ASME/ANSI B16.5 connection flanges

**For other pipework, according to options installed, refer to the dimensional (or G.A.) drawing of the unit provided.**

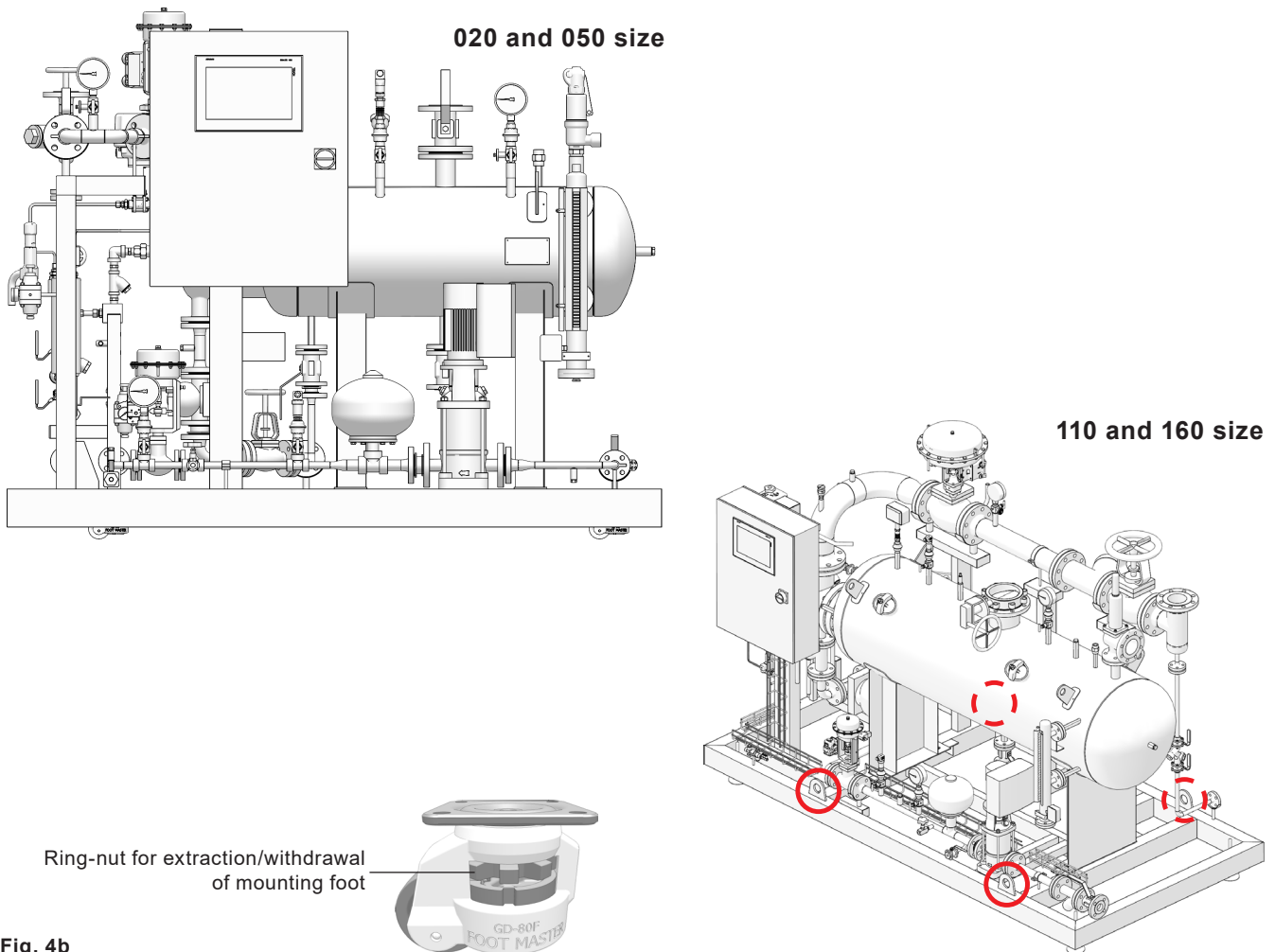


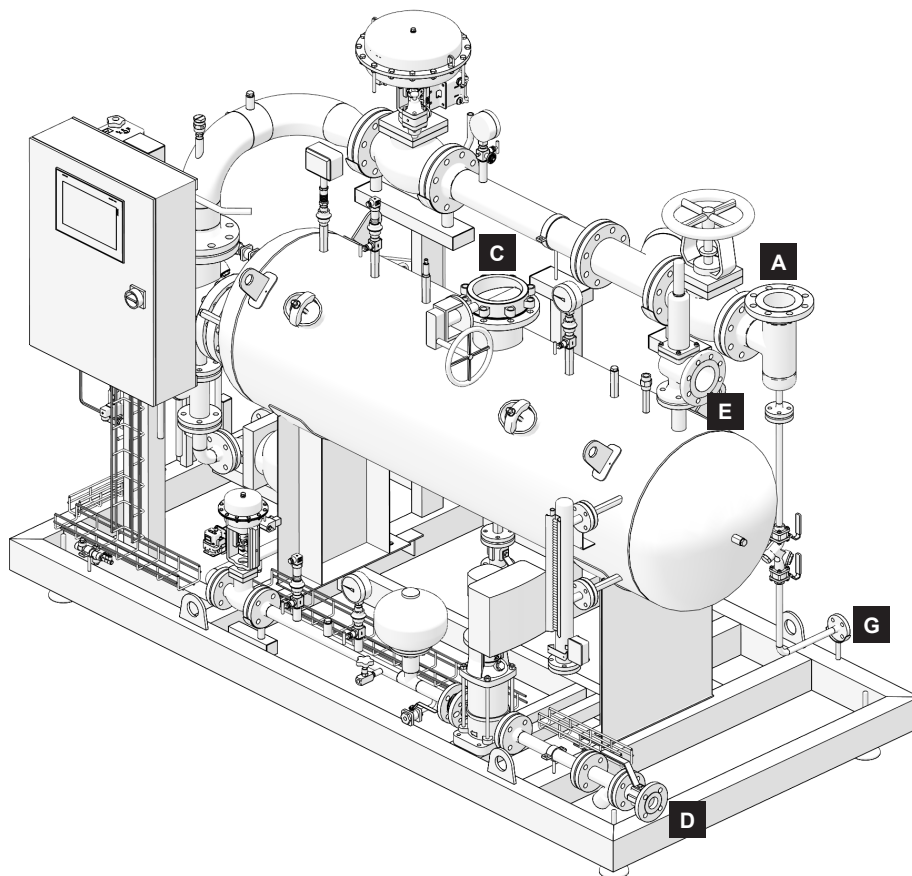
Fig. 4b

## Connections

		Metric				Imperial			
		020	050	110	160	020	050	110	160
<b>A</b>	Plant steam inlet connection	DN32 PN16	DN50 PN16	DN80 PN16	DN100 PN16	1¼" ANSI 150	2" ANSI 150	3" ANSI 150	4" ANSI 150
<b>C</b>	Clean steam outlet connection	DN50 PN40	DN80 PN40	DN125 PN16	DN150 PN16	2" ANSI 300	3" ANSI 300	5" ANSI 300	6" ANSI 300
<b>D</b>	Feedwater inlet connection	DN15 PN40	DN20 PN40	DN25 PN40	DN32 PN40	½" ANSI 300	¾" ANSI 300	1" ANSI 300	1¼" ANSI 300
<b>E</b>	Safety valve discharge	1" G-f	DN50 PN16	DN80 PN16	DN80 PN16	1" NPT	1¼" NPT*	3" NPT	3" NPT
<b>G</b>	Plant steam condensate drain connection	DN15 PN40	DN15 PN40	DN15 PN40	DN15 PN40	½" ANSI 150	½" ANSI 150	½" ANSI 150	½" ANSI 150

**Options**

Fig. 5



Connections continued on next page

## Connections (continued)

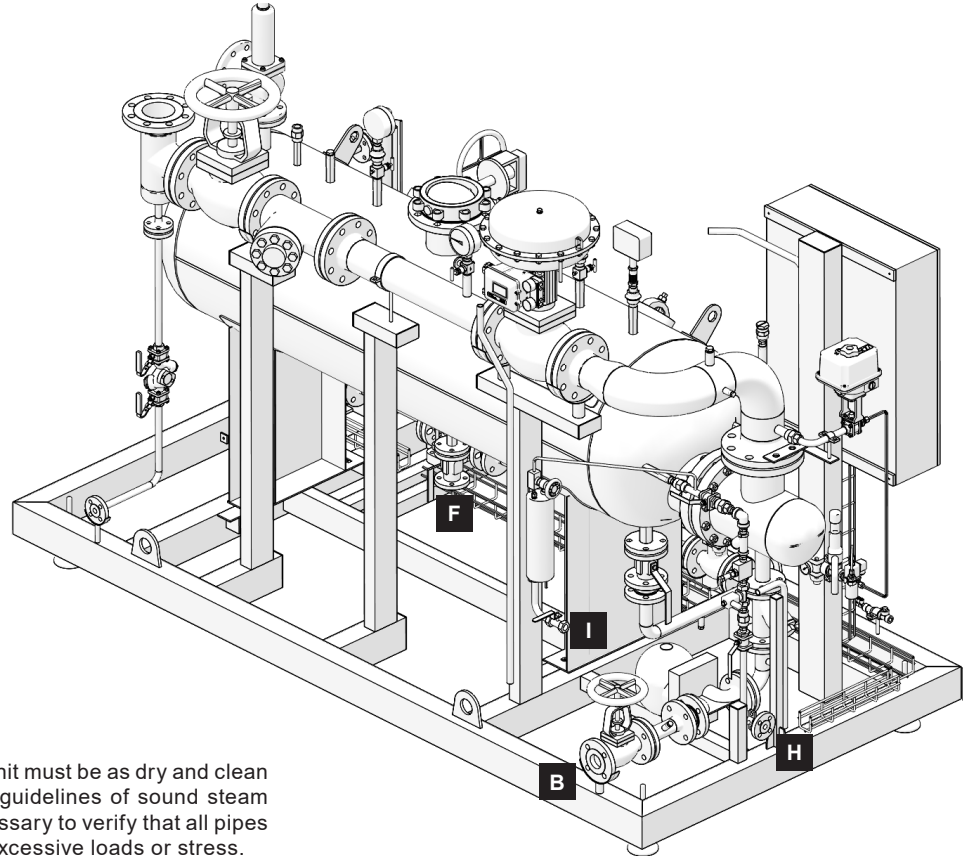
		Metric				Imperial			
		020	050	110	160	020	050	110	160
<b>B</b>	Condensate outlet connection	DN25 PN40	DN25 PN40	DN40 PN40	DN40 PN40	1" ANSI 300	1" ANSI 300	1½" ANSI 300	1½" ANSI 300
<b>F</b>	Drain connection	DN25 PN40	DN25 PN40	DN25 PN40	DN25 PN40	1" ANSI 300	¾" ANSI 300	1" ANSI 300	1" ANSI 300
<b>H</b>	TDS Blowdown connection	DN15 PN40	DN15 PN40	DN15 PN40	DN15 PN40	½" ANSI 150	½" ANSI 150	½" ANSI 150	½" ANSI 150
<b>I</b>	Sampling system (cooling water in/out - sample out)	½" BSP - 6 mm	½" BSP - 6 mm	½" BSP - 6 mm	½" BSP - 6 mm	½" BSP	½" BSP	½" BSP	½" BSP
<b>Options</b>									



Before making any connection, check that all pipework is clean and free of foreign material or scale that may adversely affect functioning and/or the performance of the unit.

The steam supplied must always be maintained within design operating pressure and temperature limits. The unit shall not work above the design pressures and temperatures indicated on the name plate on the package.

The drawings provided in this manual are for guidance purposes only. For connections of the unit, always consult the attached drawings.



The steam supplied to the CSG-FB unit must be as dry and clean as possible in accordance with the guidelines of sound steam engineering practices. It is also necessary to verify that all pipes are suitably supported without any excessive loads or stress.

### 3.4.1 Feedwater inlet

The first step of the installation procedure consists in connecting the unit to the cold feedwater line. The manual isolating valve on the feedwater control line of the unit must remain closed until installation has been completed. The precise position of the feedwater inlet connections, the pipe diameter and size of the attachment flange can be deduced from the drawings provided with the unit.

The feedwater system must be able to supply the correct volume of water to the package whilst meeting the design criteria (see 2.5 Operating limits - temperature, supply pressure, feedwater quality).

### 3.4.2 Clean steam outlet

The next step in the installation procedure is to connect the clean steam outlet of the generator to the clean steam distribution network of the plant. The precise position of the clean steam outlet, the pipe diameter and size of the attachment flange can be deduced from the drawings provided with the unit. A manual isolating valve (if option is not selected) should be installed downstream of the unit on the clean steam line to permit isolation of the generator. This valve must remain closed until installation has been completed.

**Note: In the case of units installed in parallel with another generator(s) (common clean steam distribution line), a check valve must be installed on the steam outlet of each generator.**

### 3.4.3 Primary energy source (industrial steam)

Connect the inlet of the primary fluid of the unit to the technological steam distribution network of the plant. The manual (if fitted) isolating valve installed on the primary fluid control line must be closed and remain closed during installation. The precise position of the primary fluid connection, the pipe diameter and size of the attachment flange can be deduced from the drawings provided with the unit.

If there is a risk of overpressure to the package, it is good practice for the customer to install a safety relief valve upstream of the package. This may impact the supply pressure that can be supplied to the package and therefore may also have an impact on the clean steam generator's performance (kg/h).

If the plant steam supply pressure drops this will impact on the clean steam performance (pressure/dryness/flowrate).



**Potential risk of injury and/or fatality**

### 3.4.4 Condensate removal

Transfer of heat from the primary steam to the produced clean steam generates condensate. The condensate removal from the unit must therefore be connected to the condensate return line of the plant. The manual isolating valve installed on the condensate removal line of the unit must be closed and remain closed during installation. The precise position of the condensate removal connection and size of the attachment flange can be deduced from the drawings provided with the unit.

The condensate trap on the system has been sized considering the upstream pressure. The condensate system (pipework, condensate tank and pumps) downstream of this trap should be designed and sized independently, with consideration given to the downstream pressure and the amount of flash steam that may be produced from the clean steam generator. See TI-GM-11 Condensate Pipe Sizing for more information.

### 3.4.5 Piping the pressure relief valve to vent and drain

As required by current regulations, CSG-FB unit generators are equipped with a pressure relief valve to protect against the risk of overpressure. Venting of the pressure relief valve (steam) shall be directed towards a safe area to avoid injuries or damage. In most applications, the pressure safety valves should be vented to atmosphere (generally through the roof). The piping used in the vent system shall be of adequate size to handle the capacity of the pressure safety valve. The vent piping system shall be suitably drained to prevent formation of condensate inside this. **The vent pipe of the pressure relief valve shall not be intercepted in any way or even partially obstructed.** For further information and prescriptions regarding connection of the vent piping of the pressure safety valve, refer to the related use and maintenance manual. Venting of the pressure relief valve shall comply with current legislation. The purchaser/installer is responsible for such conformity.

### 3.4.6 Drainage of the generator

The CSG-FB steam generators are equipped with a drain/bottom blowdown line with manual valve installed on the lower part of the vessel. The blowdown from this valve is at the same pressure and temperature of the generated steam and can cause severe injury or death if not properly piped. In accordance with local regulations or standards, it is recommended that the blowdown lines be connected to a blowdown vessel or condensate cooler before being discharged to drain.

The precise position of the drainage of the generator connection and also pipe diameter and size of the attachment flange can be taken from the drawings supplied with the unit.

The drains of the generator cannot be placed back in the circuit return condensate or feedwater.

### **3.4.7 Other blowdown, venting, drainage facilities (where required)**

The CSG-FB can be equipped with optional systems for blowdown, drainage and venting, such as for example a TDS control system, primary steam drainage line. In accordance with current legislation, blowdown from the TDS control system should be connected to a blowdown vessel or condensate cooler before being discharged to drain. TDS blowdown shall not be connected to the condensate return line. Primary steam blowdown can be connected to the condensate return line of the plant.

Any purge/drain should not be recovered reintegrating the line/water storage tank of feedwater.

The sample cooler option is strongly recommended, especially when the timed TDS option is selected, to assist calibration of the blowdown conductivity.

### **3.4.8 Commissioning infrastructure**

It is useful to be able to vent to atmosphere during commissioning as this helps to set PID settings and to prove the package performance. If possible, include a vent to atmosphere to facilitate this. A valve on this line is useful to simulate process demands.


### **3.4.9 Cleanliness**

This product is intended to be connected into a system that can operate an EC1935 compliant process.

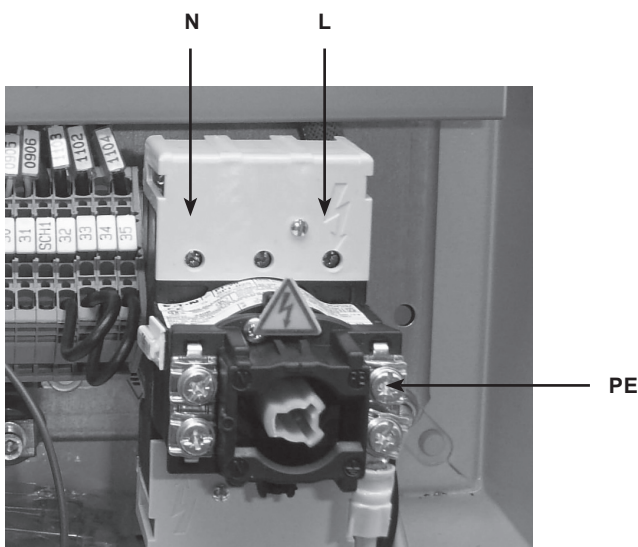
Take care to not introduce any contaminants during installation. When making connections to the clean steam side, keep covers on the connections until the connection is ready to be made. During installation, use only products that meet EC1935 requirements, for example gaskets with EC1935 compliance. A list of the materials that could come directly or indirectly into contact with foodstuffs can be found in the Declaration of Compliance available for this product.

### 3.5 Connection of the power supply

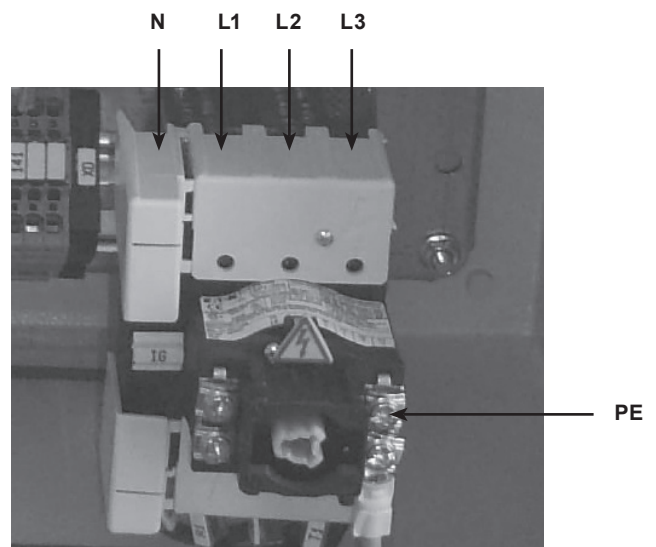
For voltage connections, consult the wiring diagram provided for the unit.

	<p><b>Possible injury or death</b>  <b>Before connecting the power supply, check that the main power switch and system start selector are off (0 position).</b></p>
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Where indicated in the wiring diagram, single phase or 3 phase power supplies are to be connected directly to the main isolation switch. Earth points are provided and must always be connected. Power supplies and earth connections must pass through the appropriate number of cable glands to maintain the IP rating for the electrical panel.



**Fig. 6**  
Version with single-phase power supply



**Fig. 7**  
Version with three-phase + N power supply

	<p><b>All electrical connections must be made by qualified electricians.</b></p> <p><b>The user is responsible for the suitability of electrical connections outside the unit and for their conformity with current legislation.</b></p> <p><b>Before drilling holes in the cabinet of the control panel to connect the power cables and any interface with an external system, open the door very carefully and check that there are no obstacles inside the cabinet. Ensure that there is no contact between electrical cables inside the panel with drilling residues or with metal.</b></p> <p><b>Signal cables must not be laid together with power cables outside the unit to avoid disturbances and interference during operation. Failure to comply may cause also irreparable damage to the equipment.</b></p> <p><b>The user must install a device between the power supply and control panel able to cut off the power if necessary. It is important to check compatibility of the mains supply with that required by the control panel, verifying correspondence with voltage and frequency data indicated on the nameplate.</b></p> <p><b>Unused wires in conduit must be grounded at both ends to avoid a possible shock hazard caused by induced voltages.</b></p> <p><b>The user is responsible for power connections outside the unit and their compliance with current legislation.</b></p>
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### 3.6 Connection of air supply (where necessary)

If pneumatic actuators or integrity test options are selected, the compressed air must be as dry and clean as possible in accordance with the guidelines of sound engineering practice.

Connect the compressed air supply (minimum 5 bar g-maximum 7 bar g (72.5 psi g-101.5 psi g)) to the pressure regulators fitted on the valves (CV1 and CV2).

So, before starting, adjust the downstream pressure reducers at least 1 bar g above the spring range of pneumatic actuators (if any):

Actuator spring ranges	Primary steam control valve CV1 with electro-pneumatic positioner (smart positioner as option)	Feedwater control valve CV2 with I/P converter (smart positioner as option)
020	2 – 4 bar g (29-58 psi g)	0.4 – 1.2 bar g (5.8-17.4 psi g)
050	1 – 2 bar g (14.5-29 psi g)	0.4 – 1.2 bar g (5.8-17.4 psi g)
110	2 – 4 bar g (29-58 psi g)	1 – 2 bar g (14.5-29 psi g)
160	2.5 – 3.5 bar g (36.2-50.7 psi g)	1 – 2 bar g (14.5-29 psi g)

### 3.7 Electrical specifications

For detailed electrical information, consult the wiring diagram supplied with the unit.

Type	Rated power	Suggested supply protection
Single Phase 1 x 90-132 V AC or 1 x 180-264 V AC (no pump)	0.5 kW	8A, C Curve MCB
3 Phase, 200-230 Vac with pump	5 kW	20A, C Curve MCB
3 Phase, 380-460 Vac with pump	5 kW	16A, C Curve MCB

\* **Note:** A single leg is taken from the three phase supply to power the PSU, ensure the single leg will have a voltage in the range required for single phase.

### 3.8 Digital inputs/outputs (on all versions)

For wiring, consult wiring diagram provided with the unit.

The control system for the CSG-FB can provide signals to the customer to enable monitoring of the processes. This is facilitated by the use of industrial communications. The communications protocols are included in the nomenclature and are listed below.

## 4. Commissioning

For correct commissioning, we recommend the service and support of a Spirax Sarco engineer. Please contact your local Spirax Sarco representative for more details.

### 4.1 Pre-commissioning inspection (initial start-up)

- Most of the new installations during the construction of pipelines and the installation of the system, may inadvertently collect dirt particles inside the pipes. It is essential to carefully remove any residual impurities and dirt in them before starting the commissioning. Upon receipt of CSG-FB begin the SAT check (Site Acceptance Test) by completing 6.1.1 - Document Review.
- Check that all the manual isolating valves (on primary stream, on condensate blowdown, on clean steam intake and on feedwater) are closed.
- Clean the filters upstream of the regulation valves.
- Check that the bottom drain valve VM11 (or VE11) of the unit is closed.
- Make sure that the unit power supply is disconnected.
- Check that primary steam and feedwater design conditions do not exceed the rated values of the unit.
- Check that the design conditions of the downstream system, clean steam side, are not lower than the rated data of the unit or in any case not lower than the calibration pressure of the safety valve installed on the unit, secondary side.
- Check that the feedwater line is properly pressurised and has been vented.
- Check that the supply steam (primary) line is properly pressurised and has been drained/ vented.
- Check that the clean steam line has been drained/vented.
- Check that the air supply line, if any, complies with system requirements.
- Check that the power supply complies with the system requirements.
- Make a double check to verify that all connections to steam, condensate and water lines have been made correctly.
- Check that the bolts of the flanged attachments are correctly torqued.
- Check that all the electrical connections outside the unit, are verifying compliance with the wiring diagram (see wiring diagram supplied with the unit).
- Check the air supply of the filters/reducers of the valves (actuated pneumatically where established) and that it complies with the system requirements.
- Check that the base has been properly electrically grounded.
- Cut the cable ties on the safety valve, remove and store the attached documentation.
- Remove the viscorol float from the bag, reinsert the float with the arrow pointing upwards.
- Check safety valve has been plumbed to a safe location, and that pipes are of a suitable size.
- Perform a walk-the-plant to ensure the wider installation is safe.
- Check for sufficient insulation on steam pipes around the control panel and any wiring.
- Using the P&ID, ensure all components are present.
- Check the details of all the sensors.
- Check all subsystems to the package are installed correctly, eg condensate cooler.
- Continue the SAT test by completing up to and including 6.1.5 - Pneumatic component check.

### 4.1.2 Cleaning cycles

The clean steam generator is supplied after a pickling and passivation cycle., however, during the construction of pipelines and the installation of the system may inadvertently collect dirt particles inside the pipes. To account for this, there are two cleaning cycles to be completed as part of the commissioning process. The first cleaning cycle will flush the feedwater line and the generator, and a second purge cycle is performed once the system is at operating pressure.

The first cycle is performed by partially filling the generator, isolating the feedwater supply and then opening the bottom drain to fully drain the generator. See 4.2 On-site commissioning procedure for when to perform this cleaning cycle.

The second cleaning cycle:

Before the first use a purge cycle must be performed. This takes place after a CIP (cleaning in place) or other procedure that is performed by following the process in the below table that shows the time each cycle should last for in order to sufficiently flush the CSG. The point at which to perform the purge cycle is given in the commissioning procedure.

Clean steam pressure (bar g)	No. of 30s open, 30s off intervals (full minutes for test)	Clean steam pressure (bar g)	No. of 30s open, 30s off intervals (full minutes for test)
1	16	5	7
2	11	6	6
3	9	7	6
4	8	8	6

## 4.2 On-site commissioning procedure

The CSG-FB control system has an integrated commissioning sequence designed to guide the user through configuring, starting and tuning the systems PID settings from factory.

It is assumed at this point that all required pipe connections and services have been connected. To begin the commissioning sequence, all connected services must be available and all critical alarms must be cleared.

Have the package nomenclature ready as it is needed during commissioning.

1. Using the Bolt torque table, ensure that all fittings and flanges are tightened to their correct settings. Ideally, these should be identified with a marking compound to allow checks before proceeding.
2. Close all manually operated steam isolation valves and provide steam to that part in the line. If automated isolation valves have been fitted, open all manually operated steam isolation valves.
3. Open all manually operated condensate valves from the customer's connection.  
**Note:** To reduce water hammer during start-up, it can be useful to crack the condensate valve open slightly to allow the system to warm up before opening the valve fully once the package is up to operating temperature.
4. Open any manually operated valves downstream of the TDS valve VE12.
5. If Integrity test option is fitted, open any manually operated valves connected the Drain Valve VE11.
6. Open any manually operated valves upstream water inlet to the CSG-FB.
  - Bleed the pump and prime the feedwater line.
  - Open any ports for gauges and sensors.
  - Open the clean steam manual isolation valve (if fitted).
7. Ensure that all trip switches inside the control panel are set to on.
8. Switch the control panel isolator to the On position.
9. Check that all pneumatic positioners (if fitted) are set to Auto.

10. Power on the control panel and wait for the Spirax Sarco welcome page.
- Continue the SAT test up to and including 6.1.13 - Generator Manual Operation.
  - Perform the first cleaning cycle (see 4.1.2 cleaning cycles).
  - Open the plant steam manual isolation valve (if fitted) to let steam into the package.
11. Tap the welcome page to view the Home Screen.
12. At the home screen, select the Main Menu button.



13. Select the System Menu button.



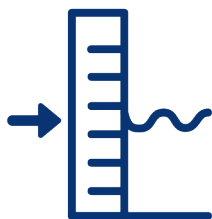
14. Select the Service screen button.



15. Select "First Start Up" button and confirm.
16. Input the correct clean steam pressure set point



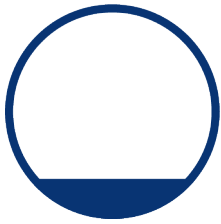
and water level



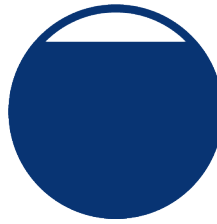
and press the start button.

17. Follow the on screen instructions.
18. If, as part of an integrity test, a leak is detected, repair the leak and repeat the test. It may be necessary to turn off the control panel to fix the leak. Repeat steps 17-21 to restart the commissioning sequence and re-check for any leaks.

19. At the PID Tuning screen, the control system can now simulate high loads and low loads to allow the PID settings to be changed to ensure correct running of the unit.



Low demand simulation button



High demand simulation button

20. At least one high demand simulation and one low demand simulation is required to complete the commissioning sequence. Select the green tick button to complete.



The commissioning sequence is now complete and the unit will continue to run at the selected pressure and level set points.

The default settings loaded during the commissioning sequence should be sufficient for the majority of simple applications. However, process settings and alarm settings should always be adjusted to suit individual applications and installations.

Once the commissioning sequence has been completed, the settings should be saved from the Factory settings screen. These settings can be updated or loaded from the Factory settings screen on the HMI.



21. Once the CSG-FB is running at the operating pressure, perform the second cleaning cycle (see 4.1.2 cleaning cycles), and then the CAH01 Blowdown Controller can be calibrated. Refer to IM-P693-39 BCR3150 Blowdown Controller to do this.

Note - If the operating pressure of the CSG-FB is changed, the CAH01 Blowdown Controller will need to be recalibrated. See 4.6 Changing the operating pressure.

22. Complete the remaining SAT tests and the Test Summary Sheet.

### 4.3 Start-up procedure

Once the commissioning procedure is complete, the CSG-FB can now be started from the Home screen.

- If automated plant steam isolation valves have been selected, open any manually controlled valves upstream.
- Follow any on screen instructions.



## 4.4 Shut-down procedure


Once the unit has begun its start-up sequence, the start button is replaced with the Stop button.

- Follow any on screen instructions.



## 4.5 Ambient conditions

When the unit is out of service in a low ambient temperature space, with a risk of freezing, it is necessary to completely empty the unit.

	<p><b>Ice inside the generator and inside primary steam line/condensate and feedwater can severely damage the equipment</b></p>
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## 4.6 Changing the operating pressure

When a change is required to the CSG\_FB operating pressure, some of the equipment will need recalibration. Ensure the following points are met every time there is a change to the operating pressure:

- Set pressure in Babystar expansion vessel to 0.7x pump pressure (only when pump is specified).
- Calibrate TDS blowdown controller (when conductivity probe is spec'd).
- Tune PID settings for the operating conditions.
- May require different valve trims in feedwater control valve and plant steam control valve.

## 5. System controls

The CSG-FB control system has a range of controls and functions to ensure the safe and stable running of the unit. Not all functions are available depending upon the configuration of the CSG-FB, these are denoted by the \* symbol.

### 5.1 Runtime controls

Runtime controls affect the response of the CSG-FB and are only active whilst the unit is 'running'. During standby, these controls are not enabled.

#### 5.1.1 Automated start-up

The Automated start-up sequence controls the safe start-up of the CSG-FB from cold and empty condition all the way through to fully pressurised and correct water level.

Detailed instructions can be provided by a Spirax Sarco engineer, however a simplified sequence can be found below.

- Raise water level to low level.
- Open automated clean steam outlet isolation valve (if fitted).
- Open automated plant steam isolation valve (if fitted).
- Control valve opens a small amount to warm up unit.
- 105 °C (221 °F) clean steam temperature is measured.
- 0.5 bar g (7.25 psi g) clean steam pressure is measured.
- Ramp up pressure to set point.
- Raise water level to set point.
- Check for pressure and water at correct set point.
- End sequence and start Run sequence.

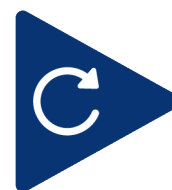


#### 5.1.2 Automated recovery

If the CSG-FB is still hot or pressurised from previous use, the control system can restart the unit without having to gently warm up the heating coils.

Detailed instructions can be provided by a Spirax Sarco engineer, however a simplified sequence can be found below.

- Maintain current water level or raise to low level.
- Open automated clean steam outlet isolation valve (if fitted).
- Open automated plant steam isolation valve (if fitted).
- Ramp up pressure to set point.
- Raise water level to set point.
- Check for pressure and water at correct set point.
- End sequence and start Run sequence.



### 5.1.3 Automated sequenced shut-down

The automated shut-down sequence ensures that the unit is in an optimal condition such that, when it begins the start-up sequence, the time taken to reach running conditions is as little as possible.

This includes reducing the water level to the 'low level' so that less time is required to reach saturation temperature.

Detailed instructions can be provided by a Spirax Sarco engineer, however a simplified sequence can be found below.

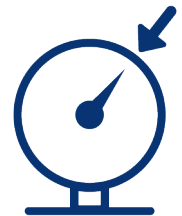
- Reduce water level to low level or wait for timer limit.
- Ramp down steam set point to 0.
- Close automated plant steam inlet (if fitted).
- Wait for water temperature to drop below 110 °C (212 °F).
- Stop water control.
- Close outlet isolation valve (if fitted).
- End sequence and start standby.



### 5.1.4 Clean steam pressure control

Control of the clean steam pressure is maintained by use of a PID control loop program in the PLC using pressure sensor PA21 as the process variable. See section 8 for component map. The steam PID set point (set during commissioning sequence) can be adjusted from the Process Settings screen. The steam PID control value is sent directly to the steam control valve VB31.

The Steam PID set point value can be overridden by the PLC during several processes. These include Ramp up/down (see section 5.1.7), Forward controls (see section 5.1.8) and PID tuning (see section 5.3).

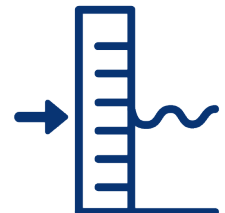


### 5.1.5 Water level control

Control of the water level within the clean steam side of the CSG-FB is maintained by use of a PID control loop program in the PLC using level sensor LA11 as the process variable. The water level PID set point (set during commissioning sequence) can be adjusted from the Process settings screen. The water level PID control value is sent directly to the water control valve VB01. If a pre-heater is fitted, the water control valve can maintain a minimum opening (0% default valve) to reduce thermal cycle fatigue on the pre-heater.

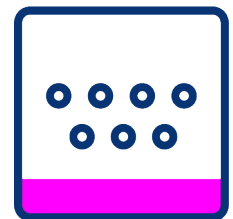
The water level PID set point can be overridden by the PLC during several processes.

These include Forward controls (see section 5.1.8), Automated start-up (see section 5.1.1), Automated recovery (see section 5.1.2) and Automated shutdown (see section 5.1.3).



### 5.1.6 TDS control

Some TDS controls are only available with the correct options fitted when ordering the CSG-FB. The following options may be available on screen if fitted. All automated TDS controls are only enabled when in Run mode. All settings are accessible from the TDS Settings screen in the Process settings area.



#### 5.1.6.1 Interval control

Available across all TDS control options, Interval control relies on a 2 timers to open and close the TDS valve VE12.

If either of the conductivity sensor options are fitted, a limit value for the TDS is still be set on screen and used for process diagnostics.



### 5.1.6.2 Pulsed hysteresis control\*

With the inclusion of a conductivity sensor CA11 fitted in the TDS blowdown line of the CSG-FB, the conductivity of the water can only be monitored when the TDS valve VE12 is open. The interval and duration of these checks must be set to allow a reliable TDS value to be read.

If, whilst the TDS valve is open, the conductivity reading is above the TDS set-point, the valve will remain open until the conductivity reading reduces by the Hysteresis set-point.

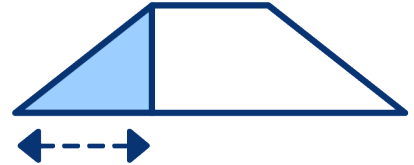


### 5.1.7 Ramp up/down

At the initiation of the Clean Steam pressure control, the set-point sent to the PID program is always ramped up from 0 to the desired set-point over a period of time. This ramp up is used in the automated start-up and recovery sequences.

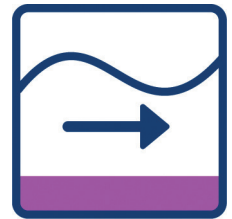
Similarly, if the clean steam pressure set-point is altered whilst the CSG-FB is running, the ramp sequence will alter the set-point over the ramp period.

The ramp up and ramp down time period can be altered on the Process Settings screen.



### 5.1.8 Forward controls

Forward controls are used to anticipate extra-ordinary running conditions in order to ensure safe and reliable running of the CSG-FB. There are two conditions that are monitored and two respective controls processes designed to handle them. The Forward Controls settings page can be found in the Process Settings area.



#### 5.1.8.1 Rapid high demand

If a significant and prolonged period of high demand results in a drop of Clean Steam pressure PA21, then the water level set-point is temporarily raised. This is designed to anticipate the rapid level loss due to flash boiling of the water in the CSG-FB due to the drop in pressure.

The values used for the Clean Steam pressure drop, duration of the drop, the raise in water level set-point and the duration of the set-point raise can all be set from the Forward Controls settings screen.



#### 5.1.8.2 Rapid low demand

If a rapid spike in Clean Steam pressure PA21 is detected, then the set-point used for the Clean Steam pressure is temporarily lowered. This is designed to reduce the amount of energy in the CSG-FB and reduce the risk of over-pressurisation.

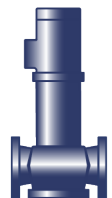
The values used for the Clean Steam pressure raise rate, reduction of the Clean Steam pressure set-point and duration of the set-point raise can all be set from the Forward Controls settings screen.



### 5.1.9 Water pump\*

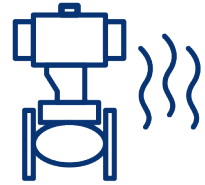
If the integrated booster pump is fitted, CSG-FB can independently control water pressure fed directly to the Clean Steam side. The control signal sent to the pump is a target pressure to which the pump drives to. The target pressure is calculated as the pressure currently detected Clean Steam Pressure PA21 + Pump offset. The pump can also be set to maintain a continuous pressure rather than an offset. This is option is only available at commissioning by a Spirax Sarco Engineer. The Pump offset or fixed setpoint can be set from the Water PID settings page in the Process Settings area.

As the pump has its own control system, no bypass loop is required to prevent over-pressurisation.



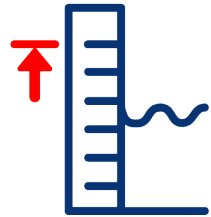
### 5.1.10 Ball Valve anti-binding\*

The ball valve anti-binding sequence ensures that ball valves which are subjected to prolonged periods in the open position do not stick. To do this, any ball valves fitted to the CSG-FB that are in the open position at midnight each day are given a closed signal for 1 second. After this 1 second closed signal, valves will return to their open position.



### 5.1.11 Water level overflow\*

If the water level reaches the overflow level setpoint whilst in Run mode, the TDS valve (VE12) will open. This will override any TDS control as stated in 5.1.6. Once the water level has dropped below the overflow level setpoint, the TDS valve (VE12) will revert to normal TDS control.



### 5.1.12 Level Cutoff\*

If the water level reaches the level cutoff setpoint whilst in Run mode, the water level control valve (VB01) will try to move to 0%, overriding the normal PID control signal for the minimum opening value. When the level drops below the level cutoff setpoint, normal PID will resume and the minimum opening position will return to the previous setting.

The level cutoff setpoint can be the same position or greater than the water level overflow setpoint, but cannot be lower.

## 5.2 Manual controls

All manual controls are accessible from the Override screen in the System area. All fitted automated valves fitted to the CSG-FB are able to be controlled manually whilst the system is in Standby mode. Whilst the system is in any other mode, manual controls are not available.

On/off valves can be opened or closed using their respective toggle button on the screen. Control valves can be moved to a specified position once the valve has been enabled. Disabling the valve will return the valve to closed position. Whilst manual controls are enabled, the CSG-FB will not begin Automated Start-up or Recovery. All manual controls must be reset before continuing. A warning is displayed if the clean steam temperature inside the CSG-FB has exceeded 100 °C (212 °F). This is to prevent accidental discharge of hot water or steam.



## 5.3 PID Tuning

PID Tuning is a series of processes that allow the system to simulate loads rises and drops on a running CSG-FB. In order to do this, the PID Tuning sequence reduces the current Clean Steam Pressure set-point by 1 bar g (14.5 psi g).

Once the CSG-FB is running at the PID Tuning set-point, the user can either instantaneously; increase the set-point by 0.5 bar g (7.3 psi g) to simulate high demand, or decrease the set-point by 0.5 bar g (7.3 psi g) to simulate low demand. With either of the simulations, the PID controller will now react accordingly allowing the user to set P, I and D values for both water control and steam control to ensure safe and stable running.

The PID Tuning screen is accessible as part of the commissioning sequence, from standby by selecting the 'PID Tuning Sequence' button, and whilst running by selecting 'Running PID Tuning'.

If PID tuning is initiated from standby or commissioning, the CSG-FB will start normally using the Automated Start-up sequence as described in section 4.2.

If Running PID tuning is selected, the system will reduce the clean steam pressure set-point by 1 bar g (14.5 psi g) and the PID tuning screen will be visible.

If a system has been oversized and the valve is operating at a fraction of the opening percentage, changing the trim of the control valve may help to improve the stability of system.



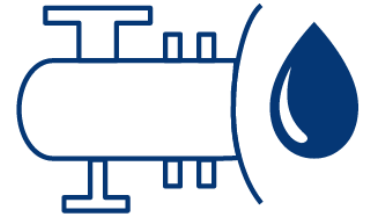
## 5.4 Optional functions

All functions in this section are part of the optional features packs and will not be available without the correct configuration.

### 5.4.1 Integrity test\*

The integrity test option includes all the necessary valves and measurement equipment to fully isolate the inlet steam side of the CSG-FB from the Steam Control valve VB31 to the Condensate Isolation valve VE51 and perform a pneumatic pressure decay test. This test, when selected will be conducted at the beginning of the next Automated Start-up sequence.

At the end of a failed Integrity Test, the user will be prompted to either re-test, stop the start-up sequence or ignore the test and continue the Automated Start-up. Successful test will not provide any feedback and continue with the Automated Start-up sequence.



An Integrity test will always be performed at the First Start-up as part of the commissioning sequence. This test cannot be ignored. The Integrity test can only be re-started or stop the Automated Start-up sequence entirely.

### 5.4.2 Service sequence\*

In order to facilitate the safe and easy maintenance of the CSG-FB, a guided service sequence is available to give a servicing engineer the ability to verify valve operation and clean the heating elements.

Whilst the service sequence is in operation, the CSG-FB cannot go into run mode or begin Automated Start-up.

The Service Sequence initialisation is located in the Service screen in the System area. Operators are instructed to manually isolate all external connections to and from the CSG-FB. This includes plant steam, drain, water, condensate and clean steam lines.



In order to ensure that components are safe to operate independently, a series of temperature and pressure sensors are located throughout the CSG-FB. If a temperature above 25 °C (77 °F) or pressure of 0.1 bar g (1.45 psi g) is detected at any point, all controls are automatically set to a safe position and the service sequence is halted.

Prior to and during the 'Cleaning' phase, the screen will indicate a safe (green), not safe (red) indicator next to each sensor monitored around the CSG-FB to allow the engineer to identify if it is safe to remove components on the unit. At this stage, if the control panel is powered down, the service sequence is retained within the memory of the controller and will return to the same point when power is returned to the panel. This ensures that the Automated Start-up sequence cannot be initiated if components are missing from the CSG-FB.

### 5.4.3 Performance monitoring\*

Performance monitoring is a series of sampling, calculation and comparison algorithms that map the performance of the CSG-FB over the full range of operation flow ranges. The flow ranges for each model of the CSG-FB are preloaded into the program and are automatically loaded during the commissioning sequence. With a performance map, the performance of the CSG-FB can be monitored for leaks in or scaling on the heating elements.



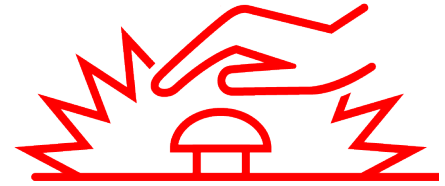
The sampling period is limited to a maximum of 10 samples over the flow range or 100 hours of running. After this period the CSG-FB is assumed to no longer be operating under best conditions. Without a minimum of 3 samples, the calculation and comparison algorithms will not operate. Once sufficient data has been collected and the calculation algorithm has been allowed to run, the comparison algorithm can now compare the current run conditions with the ideal model created by the sampling algorithm.

The Performance Ratio Fault Tolerance value is a percentage difference when comparing the mapped value to the current sampled value. Samples exceeding the positive tolerance value are experiencing a drop in performance (typically due to scale build up), while samples dropping below the negative tolerance value are experiencing abnormal increase in energy transfer (typically due to a leak from the plant steam directly into the clean steam). Respective alarms are shown in the alarm screens when tolerances are exceeded. Settings, live readouts and mapped data from the Performance Monitoring algorithms can be found on the Performance Data area of the HMI.

**HINT:** Key to the accuracy of the Performance Monitoring is the accuracy of the sample data. Specifically ensuring that the measured water flow is as steady as possible. To facilitate this, a series of data filters are available to ensure that flow readings are kept free from anomalous spikes and drops.

## 5.5 Emergency stop

The emergency stop program constantly monitors a set of diagnostic systems and will prevent the running of the CSG-FB if any of these diagnostics triggers and alarm. The emergency stop can only reset and allow the running of the system when the cause of the alarm is cleared. In addition to the cleared alarms, the Reset pushbutton must also be pressed to clear the Emergency Stop.



When the emergency stop is triggered, the status of the CSG-FB is changed directly to 'Emergency Stop', overriding any previous run status. Additionally, all automated isolation valves are reset, control valves are closed and the water pump (if fitted) is disabled.

The diagnostics systems monitored vary depending upon the current run status. For any run status other than Running (i.e. Automated start-up, restart, sequenced shutdown, integrity test and standby) the systems are listed below. See section 6 for more details on individual diagnostics.

- Emergency stop push button
- Major Instrument failure (Section 6.20.1)
- Steam control valve failure (Section 6.20.2)
- Water control valve failure (Section 6.20.3)
- Water pump failure\* (Section 6.8)
- Process limit switches (Sections 6.6)
- Air pressure failure\* (Section 6.10)
- Water supply failure.\* (Section 6.9)

When the CSG-FB is in Running mode, the following alarms are monitored:

- Emergency stop push button
- Major Instrument failure
- Steam control valve failure
- Water control valve failure
- Water pump failure\*
- Process limit switches
- Air pressure failure\*
- Water level low limit\* (section 6.7)
- Supply pressure failure\* (Section 6.11)
- Water level control failure (Section 6.3)
- Water supply failure\*
- Water level high limit (Section 6.4)
- Optional E-stops (Section 6.19)

\*Diagnostic triggers only available if optional equipment fitted.

## 6. Diagnostics

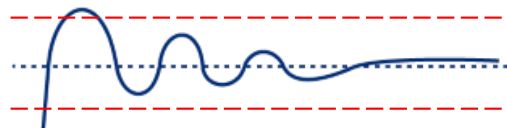
All diagnostic troubleshooting can be found in Section 11.

Not all diagnostics are available depending upon the configuration of the CSG-FB, these are denoted by the\* symbol.

### 6.1 Control bands

Clean Steam Pressure Control and Water Level Control are both monitored by separate Control Bands, however both control bands operate the same way.

Control Bands monitor their respective process value and compare to the set-point. Upper and lower bands are defined by percentage value from the set-point. If the process value exceeds either the high or low band tolerances a timer is started. If the timer exceeds the Band Alert time a Control Band Alert is issued to the Alarms screen.



If the process value continues to exceed the band tolerances and the timer continues past the Band Alarm time, then a Control Band Alarm is issued to the Alarms screen. If the process value returns to within the band tolerances, the timer is reset.

Control Bands only monitor in Run mode and not in the PID Tuning sequence. Alarms and Alerts reset when the process value returns to within the upper and lower bands. When water level high band alarm is triggered, the water control valve minimum opening is set to 0% to eliminate the possibility of over filling the CSG-FB.

**Note:** Control Band alarms are used by other diagnostic systems. Correct setup at commissioning is critical to robust controls, accurate diagnostics and reduction of nuisance alarms.

### 6.2 Control capacity

The Control capacity diagnostic monitors both the control value from the PID program and the Control band high alarm for the respective process. This provides engineers with a tool to identify if the capacity of either of the control system is at its limit and thus impacting performance of the CSG-FB.

Clean steam pressure control and Water level control are both monitored by separate Control Capacity diagnostics, however both operate the same way.

If the control valve is fully open for a period of time and the Control band high alarm is active, then the Control Capacity alarm is triggered. If the control valve is fully open for a period of time and the Control Band high alarm is not active, the Control capacity alert is triggered.

Alarms and Alerts reset when the control valve closes from being fully open.



### 6.3 Water Level Failure

The Water Level Failure diagnostic monitors the High Water Level Control system (see section 5.1.11). If the High Water Level cycle is triggered a number of times within a certain time period, the Water Level Failure alarm is triggered.

The number of repeated triggers and timer period are editable on the HMI.

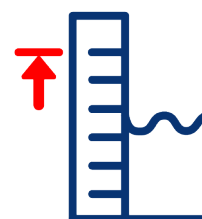
The alarm is only reset when the Reset pushbutton is pressed.

### 6.4 High water limit

The High water limit diagnostic monitors the Level sensor LA11 to stop the CSG-FB over filling. When the water level sensor reads the measurable limit, the High Water Level alarm is triggered.

The alarm is reset when the water level reduces below the measurable limit.

When high water limit is triggered, the water control valve minimum opening is set to 0% to eliminate the possibility of filling the CSG-FB.



### 6.5 Panel temperature limit

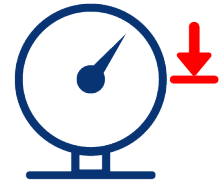
The panel temperature of the CSG-FB is monitored by a PT100 temperature sensor located inside cable trunking of the electrical panel TAX1. If the temperature exceeds the maximum ambient operating temperature of 55 °C (131 °F), the Panel Temperature Alarm is triggered.

The alarm is reset when the measured temperature reduces below 50 °C (122 °F).

## 6.6 High pressure limit

Each CSG-FB is fitted with a mechanical pressure switch PD21 set to the maximum operating pressure for the unit. This switch is set by the manufacturer prior to dispatch. This pressure switch triggers the Process limit switch alarm.

The alarm is reset when the clean steam pressure is low enough for the mechanical pressure switch to reset.

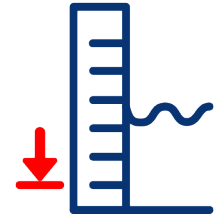


## 6.7 Low water level limit\*

The Low water level limit diagnostic prevents the exposure of the heating elements.

If the level sensor LA11 gives a reading of less than 40% the Low water level limit alarm is triggered.

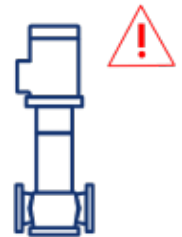
The alarm is reset by the water level raising enough to be above 40% on the level sensor.



## 6.8 Water pump fault\*

The optional integrated water pump MB01 provides a simple diagnostic feedback signal MD01 which is only triggered when there is a fault with the pump or the control of the pump pressure.

The alarm is cleared when the fault is cleared from the water pump.



## 6.9 Water supply failure\*

The Water supply failure diagnostic monitors the water supply pressure PA01 and is only activated when the integrated water pump is not fitted.

When active, the water supply pressure is compared to the control pressure that would be sent to the integrated pump (see section 5.1.9). If the supply pressure is below the control signal, the Water supply failure alarm is triggered.

The alarm is cleared when the supply pressure exceeds the control signal that is generated for the water pump.

## 6.10 Pneumatic supply failure\*

When fitted, the Pneumatic supply pressure switch PDX1 is used to monitor the compressed air supply to the CSG-FB. If the air supply pressure drops below the minimum required pressure, the alarm is triggered.

The alarm is cleared when the pneumatic supply pressure increases above the minimum required pressure.

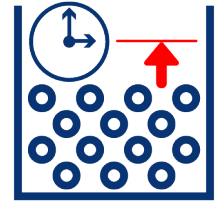
## 6.11 Supply steam failure\*

The Supply steam failure diagnostic monitors the control signal sent to the Steam control valve VB31 and the Steam inlet pressure PA13 whilst in the 'Running' state. When the control signal requests the control valve to be fully open for longer than 60 seconds and the Steam Inlet pressure is below the current clean steam pressure set-point. The alarm is triggered.

The alarm is cleared once the pressure rises above the clean steam pressure set-point.

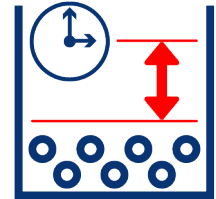
## 6.12 TDS limit\*

When fitted with a conductivity sensor CA11, the TDS limit diagnostic monitors the conductivity and will trigger an alarm if the TDS set-point is exceeded for a period of time. The alarm is cleared when the measured conductivity is reduced below the TDS set-point.



## 6.13 TDS hysteresis fault\*

The TDS hysteresis fault diagnostic closely monitors the TDS control system, specifically the Hysteresis controls. When hysteresis is engaged and the TDS valve is opened, a timer is started. If the timer expires before the measured conductivity reduces by the hysteresis setting, the alarm is triggered. The alarm is reset when the measured conductivity reduces by the hysteresis setting.



## 6.14 Trap alarms\*

The Trap alarm diagnostics can be split into two conditions based around the two alarms. The alarm for either condition is reset by pressing the Reset pushbutton.



### 6.14.1 Trap fail open

During normal running conditions, the trap of the CSG-FB will be constantly discharging condensate. As such a failed open trap would not be easily detectable. However, at low flow conditions, it is easier to identify the trap discharging excessive amount of condensate and eventually live steam.



The Trap Failed Open alarm is triggered when the control valve is only open a small amount, and the condensate temperature sensor TA51 and the drain temperature sensor TA52 are similar temperatures. The maximum valve temperature and maximum difference between temperature sensors can be set on the HMI.

### 6.14.2 Trap fail closed

The Trap failed closed alarm monitors the drain temperature sensor TA52. Based on the below calculation, the minimum operating temperature of the drain condensate after the trap can be determined. If, whilst in Running status, the condensate temperature drops below this temperature, the Trap Failed Closed alarm will activate.

**Note:** there are many causes of blockages in the condensate line that can cause the measured drain temperature to drop below minimum operating condensate temperature. If after investigation, the trap is operating properly, there may be another cause for the backup of condensate, including external to the CSG-FB.

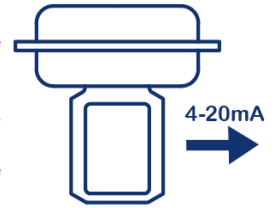


## 6.15 Valve feedback\*

The Steam control valve VB31 and the Water level control valve VB01 are both monitored by separate Valve Feedback diagnostics, however both operate the same way. The valve feedback diagnostics are disabled during the Service Sequence (see section 5.4.2).

The valve feedback diagnostic monitors the control values sent to the control valve compares this to the valve feedback signal for their respective control valves (Steam control valve feedback VA31, Water level control valve feedback VA01). A positive and negative tolerance from the control signal is calculated. If the valve feedback is not within that tolerance, a timer is started. If the timer expires, the alarm is triggered.

The alarm is reset when the control valve feedback reads within the position tolerance.



## 6.16 Isolation valve feedback\*

The Steam inlet VE31, Clean steam outlet VE01, Bottom drain valve VE11 are independently monitored by separate Isolation valve feedback diagnostics.

### 6.16.1 Fail closed

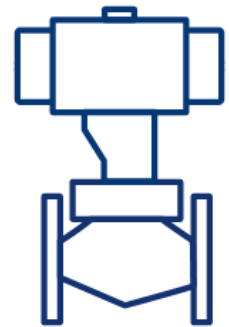
If the valve does not rotate enough to come off the valve closed limit switch within a time limit when commanded, the valve failed closed alarm is triggered.

The alarm is reset when the valve rotates enough to turn off the valve closed limit switch.

### 6.16.2 Fail open

If the valve does not rotate enough to come off the valve open limit switch within a time limit when commanded, the valve failed open alarm is triggered.

The alarm is reset when the valve rotates enough to turn off the valve open limit switch.



### 6.16.3 Partial open failure

If, when commanded, the valve takes too long to transition from closed to open, or from open to closed, the Partial open failure alarm is triggered.

The alarm is reset if the valve completes the rotation and triggers the correct limit switch.

### 6.16.4 Open speed

If, when commanded, the valve opens too quickly, the Open speed alarm is triggered. The alarm is reset when the correct valve opening speed is achieved.

## 6.17 Analogue input diagnostic

The Analogue input diagnostic is able to detect if an analogue input signal has been electrically disconnected from the system (sensor failure, wires disconnected, etc), or if the signal wires have been directly connected (wires pinched or damaged). The Open circuit alarm and Short circuit alarms are triggered respectively.

The alarms are reset when a correct input signal is detected.

## 6.18 Optional E-stop triggers

All alarms, not already included in the Emergency stop sequence (see section 5.5), have the option of triggering an emergency stop. When enabled, the alarms must be cleared before the emergency stop sequence can be reset.

## 6.19 Umbrella alarms

Umbrella alarms are not directly displayed on the Alarms page of the HMI. These alarms are collective names given to alarms used in the Emergency stop sequence (see section 5.5)

### 6.19.1 Major instrument fault

The Major instrument fault covers the analogue input alarms for all sensors that are essential the safe running of the CSG-FB. If any of these analogue input alarms are triggered, the Emergency Stop sequence will be started and will not be able to be reset until the alarms are cleared.

The following Analogue Input Diagnostic alarms are included in the Major Instrument Fault umbrella alarms:

- Clean steam temperature TA21
- Control panel temperature TAX1
- Water pressure PA01‡
- Clean steam pressure PA21
- Water level LA11

### 6.19.2 Steam control valve failure

The Steam control valve failure covers all diagnostics related to the Steam control valve VB31. If any of the alarms associated with these diagnostics are triggered, the Emergency stop sequence will be started and will not be able to be reset until the alarms are cleared.

The following diagnostic alarms are included in the Steam control valve failure umbrella alarm:

- Valve Feedback analogue input diagnostics VA31
- Valve Feedback diagnostic VA31



### 6.19.3 Water level control valve failure

The Water level control valve failure covers all diagnostics related to the Water level control valve (VB01). If any of the alarms associated with these diagnostics are triggered, the Emergency stop sequence will be started and will not be able to be reset until the alarms are cleared.

The following diagnostic alarms are included in the Water level control valve failure umbrella alarm:

- Valve feedback analogue input diagnostics VA01
- Valve feedback diagnostic VA01



# 7. Maintenance



Before starting any maintenance operation, carefully read the general safety information in Section 1 of this document.

Before starting any installation or maintenance operation, make sure that power has been shut-off.

To carry out many maintenance procedures, the unit shall be isolated from the system. The unit can be re-inserted in the system only after completing all the procedures. It is recommended that maintenance personnel carry out the shut-down and start-up procedures described in this manual.

After the maintenance activities is required a washing cycle with a CIP (cleaning in place), or other procedure required by the process/plant directives.

## 7.1 General information

The maintenance of single system components must be carried out as indicated in the individual installation and maintenance manuals (IM).

## 7.2 Inspection/replacement of the tube bundle of the generator

The U-shaped tube bundle is the core of the steam generator. It must be removed and inspected every two years or as established by the terms of the warranty. The plate of the tube bundle is secured between the flanges of the vessel of the generator and the primary steam head. It is fitted with two gaskets:

- 1 shell side of the generator, between the tube bundle plate and body/shell of the generator.
- 1 head side (2-passes), between the tube bundle plate and primary steam head.

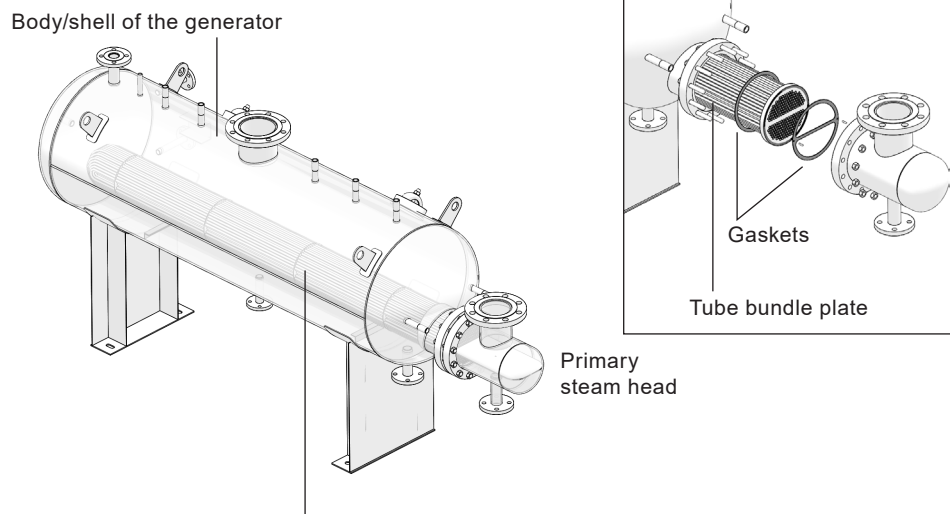


Fig. 8 "U" shaped tube bundle

### 7.2.1 Disassembly of the tube bundle:

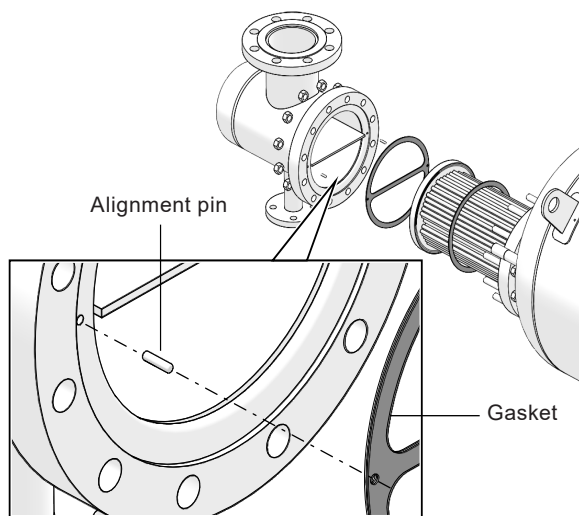
- Check that primary steam, condensate return line, feedwater inlet and clean steam outlet are isolated; that both circuits (primary and secondary) are not pressurized; that the generator has been completely drained and all components and surfaces are cold.
- Carefully remove the insulation from the header of the generator unscrewing the bolts on the aluminium cladding.
- Carefully disconnect the piping between the head of the generator and the primary steam inlet and condensate blowdown lines, with the utmost care so that no part of the line has damage.
- Separate the head from the generator, removing the bolts that secure it to the body.
- Carefully pull the tube bundle and hold it with the proper mechanical equipment slightly raised above the lower rim of the body flange, allowing a correct extraction without interferences.

### 7.2.2 Inspection of the tube bundle:

- Inspect the tube bundle for scale and/or leaks. In the absence of leaks, remove scale and carefully clean the tube bundle before preparing this for installation.
- If detected, even a leakage, contact Spirax Sarco to repair or replace the tube bundle.

### 7.2.3 Re-assembly of the tube bundle:

- Remove the old gaskets, thoroughly clean mating surfaces and install two new gaskets: one between the tube plate and generator (shell side), the other with the sector divider between the tube plate and the head (head side).
- Carefully insert the tube bundle in the generator body, use alignment pins for correct positioning of head/gasket/bundle.



- After making sure that the tube is properly in place, assemble the primary steam head by aligning the divider at the dividing line between the two passes of the tubes (expected perfectly parallel to the horizontal plane), then tighten the bolts.
- Reconnect the inlet and outlet primary lines to the steam head. Check that these have been reconnected also where they may have been detached to facilitate extraction of the tube bundle.
- Carefully check all connections to detect any leaks during start-up.

## 7.3 Inspection/Replacement of the pressure safety switch

The safety pressure switch acts as a fail-safe for Spirax Sarco Clean Steam Generators. The alarm and shut down for high pressure is set at a value lower than the set of the safety valve. If the pressure safety switch mounted on the tank is not functioning correctly and must be replaced, follow the procedures outlined below.

### 7.3.1 Disassembly of the pressure switch:

- Follow the shutdown procedure to take the unit off-line before attempting to replace the safety pressure switch.
- Turn off/disconnect all electric power before attempting any maintenance procedures.
- Check that primary steam, condensate return line, feedwater inlet, NCG vent and clean steam outlet are isolated; that both circuits (primary and secondary) are not pressurized; that the generator has been completely drained and all components and surfaces are cold.
- Carefully disconnect the wires leading from/to the control cabinet.
- Loosen the connections until the pressure probe can be removed.

### 7.3.2 Inspection of the pressure switch:

- Examine the probes for damage or incorrect positioning. For the exact procedure for examination, refer to the Spirax Sarco manual information included with the unit.

### 7.3.3 Re-assembly of the pressure switch:

- To install a new unit, follow recommendations contained in the manufacturer's documentation.
- After ensuring that the unit is correctly installed, tighten the fittings.
- Follow the start-up procedures to put the unit back on-line. Carefully check all connections for any sign of leakage.

## 7.4 Replacement of the Pressure Safety Valve (Generator)

The pressure safety valve acts as a fail-safe for Spirax Sarco Compact Steam Generators. The valve will open for high pressure to protect the system from explosion. If the pressure safety valve mounted on the pressure vessel is not functioning correctly and must be replaced, follow the procedures outlined below.

### 7.4.1 Disassembly of the safety valve:

- Follow the shutdown procedure to take the unit off-line before attempting to replace the safety pressure switch.
- Turn off/disconnect all electric power before attempting any maintenance procedures.
- Check that primary steam, condensate return line, feedwater inlet, NCG vent and clean steam outlet are isolated; that both circuits (primary and secondary) are not pressurized; that the generator has been completely drained and all components and surfaces are cold.
- After assuring that the pressure has been relieved from the tank, disconnect the vent line leading from the pressure relief valve to atmosphere (usually through the roof), and via a drip elbow, to drain.
- Carefully disconnect the pressure relief valve from between the generator vessel and feed tank.

### 7.4.2 Re-assembly of the safety valve:

- Install the new valve. Follow recommendations contained in the manufacturer's documentation, local codes, or accepted contractor practices as to the use of joint compound or sealer at the connections.
- Reconnect the vent line leading from the pressure safety valve to atmosphere and, via drip elbow, to drain.
- Follow the start-up procedures to put the unit back on-line. Carefully check all connections for any sign of leakage.

## 7.5 Spare parts

For recommended spare parts for commissioning or maintenance, please contact our Service Department.

## 7.6 Recommend inspection

The following table indicate the suggested interval times for the inspection on the clean steam generator and of all the other components installed on the package.

Inspection	Refer to product IMI	Daily	Weekly	Quarter	
Blowdown		•			** To verify the difference between the measure of the transmittal against the indicator
Control valve	•				
Water level**		•			
Pressure level**				•	
Level control	•				
Inlet and outlet line				•	
Pneumatic connections				•	
Electrical connection				•	
Primary and secondary side pressure		•			
Safety valve	•				
Manual isolation valve			•		
Strainers				•	

## 7.7 Spirax Sarco Service maintenance

Spirax Sarco can provide on request of routine scheduled maintenance contract with the following steps. The maintenance contract usually includes two visits per year.

Maintenance Test	6 month visit	12 month visit	18 month visit	24 month visit
Visual inspection of control valves and actuators	•	•	•	•
Dismantle control valves, clean and visually inspect valve internals, replace valve stem seals		•		•
Check valve/actuator/positioners, zero and stroke, adjust if necessary	•		•	
Visual inspection of all wiring and terminations	•	•	•	•
Check all electrical connections for tightness	•	•	•	•
Ensure correct operation of pump (if present)		•		•
Pressure, temperature and level transmittal control		•		•
Functional inspection of safety components and PLC			•	•
Visual inspection of heat exchanger for external leakage	•	•	•	•
Tube bundle dismantled and inspection, gasket replacement				•
Check and clean all strainer screens, re-fit using new cap gaskets	•		•	
TDS test and probe check	•	•	•	•
TDS re-calibration		•		•
Fully functional test of the unit	•	•	•	•

# 8. Component map

The Components detailed below may not be fitted to all versions of the CSG-FB. Refer to section 8.2 for Component configuration lists. Optional items are designated with \*.

## 8.1 System P&ID

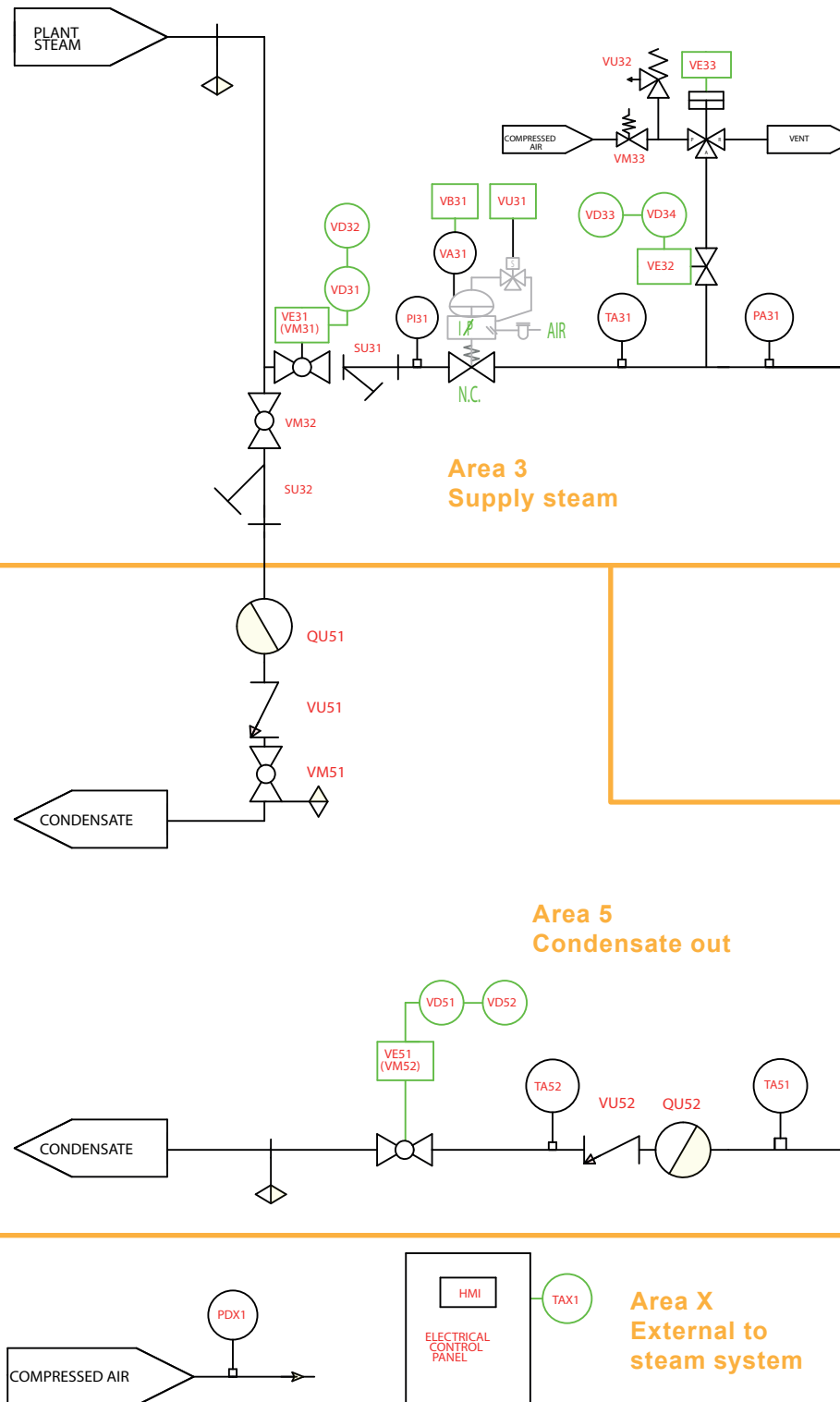
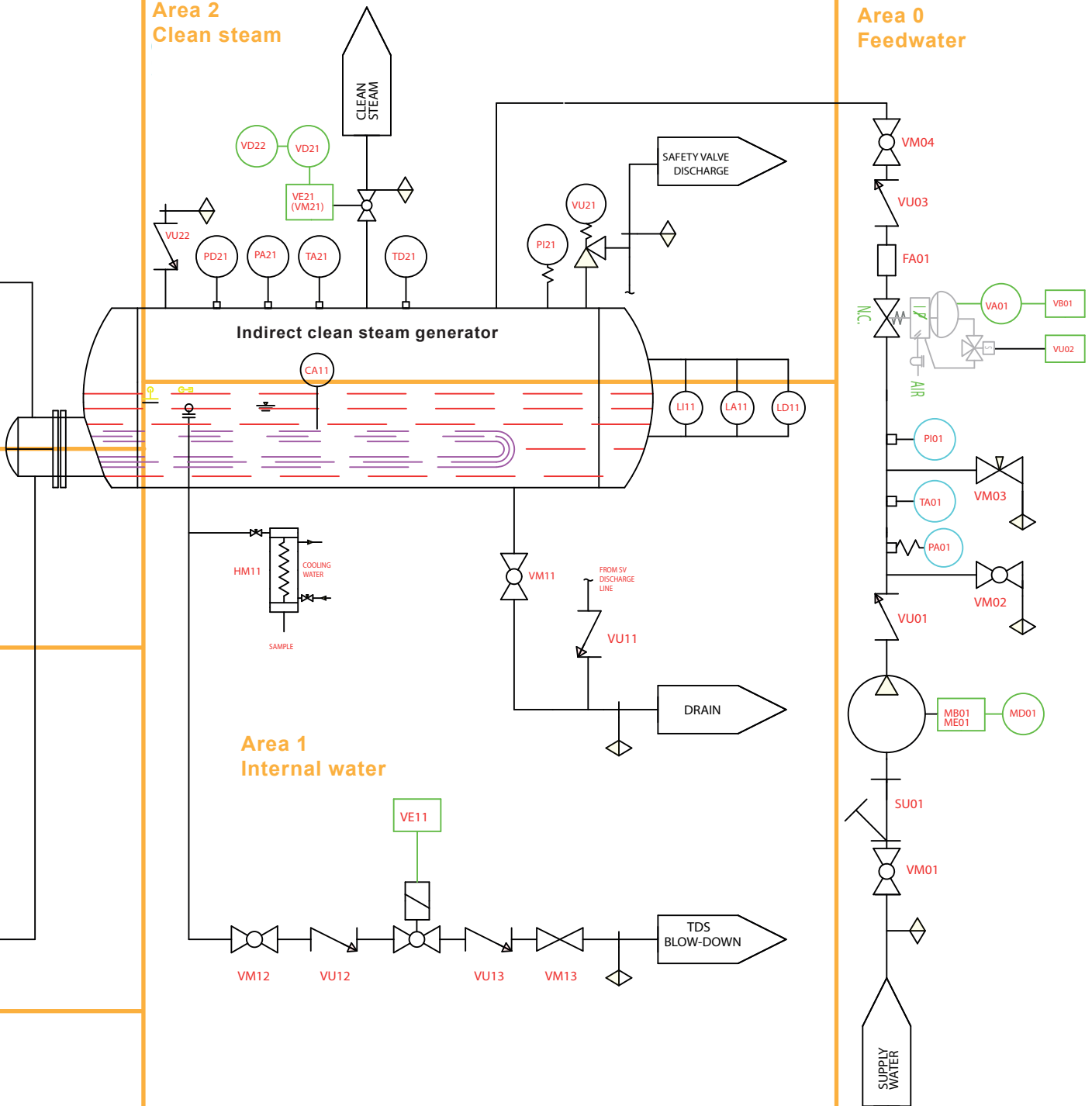


Fig. 9

**Area 2  
Clean steam**

**Area 0  
Feedwater**



CSG-FB Clean steam generation system for Food & Beverage

## 8.2 Component Configuration

The options available for the CSG-FB are listed in section 2.3. Many of the available options will utilise additional equipment fitted the system. The components specifically required for each option are listed below. Default items fitted as standard are identified with\*

### Plant steam inlet isolation valve

- Manual valve\*: VM31
- Automated valve: VM31 replaced by VE31, VD31, and VD32

### TDS control system

- Timer control\*: VE11
- Pulsed and continuous hysteresis control: VE12 and CA11

### Feedwater pressurisation system

- None\*
- Integrated pump: MA01, MD01

### Independent downstream plant protection

- None\*
- Low level limit switch: LD11
- Saturated temperature limit switch: TD21

### Intelligent Diagnostics

- None\*
- Integrity test: VM51 replace by VE51, VM11 replace by VE11, PA31, TA31, VE32, VE33
- Performance monitoring: TA01, TA21, TA31, TA51, TA52, FA01, PA31 and PA01
- System diagnostics: VB01, VB31, PA31, TA01, TA31, TA51 and TA51
  - With pneumatic control or Integrity test: PDX1
  - Without integrated pump: PA01

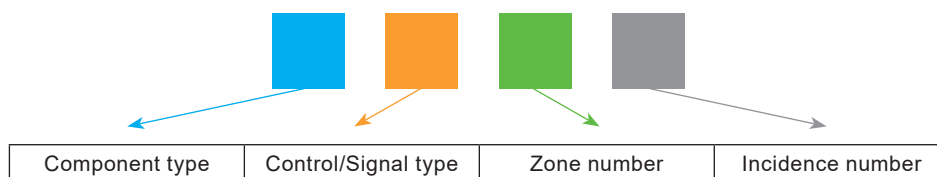
### Clean steam outlet isolation valve

- None\*
- Manual Valve: VM21
- Automated valve: VE21, VD21 and VD22

## 8.3 Component naming convention

The naming convention for the system map do not correlate to the specific parts and part numbers. The tag names are specific to the CSG-FB system and are not tied to specific component models. To identify a particular component, reference the component tag number to the Bill Of Materials for the specific model of CSG-FB.

The tag numbers can be deciphered to aid identification and location of the component on the CSG-FB.



### 8.3.1 Component types

Opposite is a table of currently identified component types.

Letter	Component type
C	Conductivity
F	Flow sensor
H	Heat exchanger (sample cooler, etc)
L	Level sensor
P	Pressure sensor
Q	Trap (steam, air eliminator, etc)
S	Separator
T	Temperature sensor
V	Valve (globe, ball, check, vacuum breaker, butterfly, etc)
W	Water vessel (pressure buffer, storage, etc)
Y	Strainer

### 8.3.2 Control/signal type

Opposite is a table of currently identified Control and Signal types. The direction of signals is always reference in relation to the PLC or process controller.

Letter	Control/Signal type
A	Analogue input (signal)
B	Analogue output (control)
D	Digital input
E	Digital output
I	Indicator (non-electrical, dial, etc)
M	Manual control
U	Un-controlled (check valve, strainer, separator, etc)

### 8.3.3 Zone allocation

Zones are used to segregate areas of the package into sub-areas based around state changes of the process of the package.

Numbering of the Zones begins with the inlet flow of the process fluid at Zone 0. When the process fluid undergoes a change or state change, the Zone number increases until it leaves the CSG-FB.

The inlet of the control fluid begins with the next available Zone number. At each state change of the control fluid, increase the Zone number until the control fluid leaves the package.

Components located externally to the steam system are always labelled as Zone X.

### 8.3.4 Incidence number

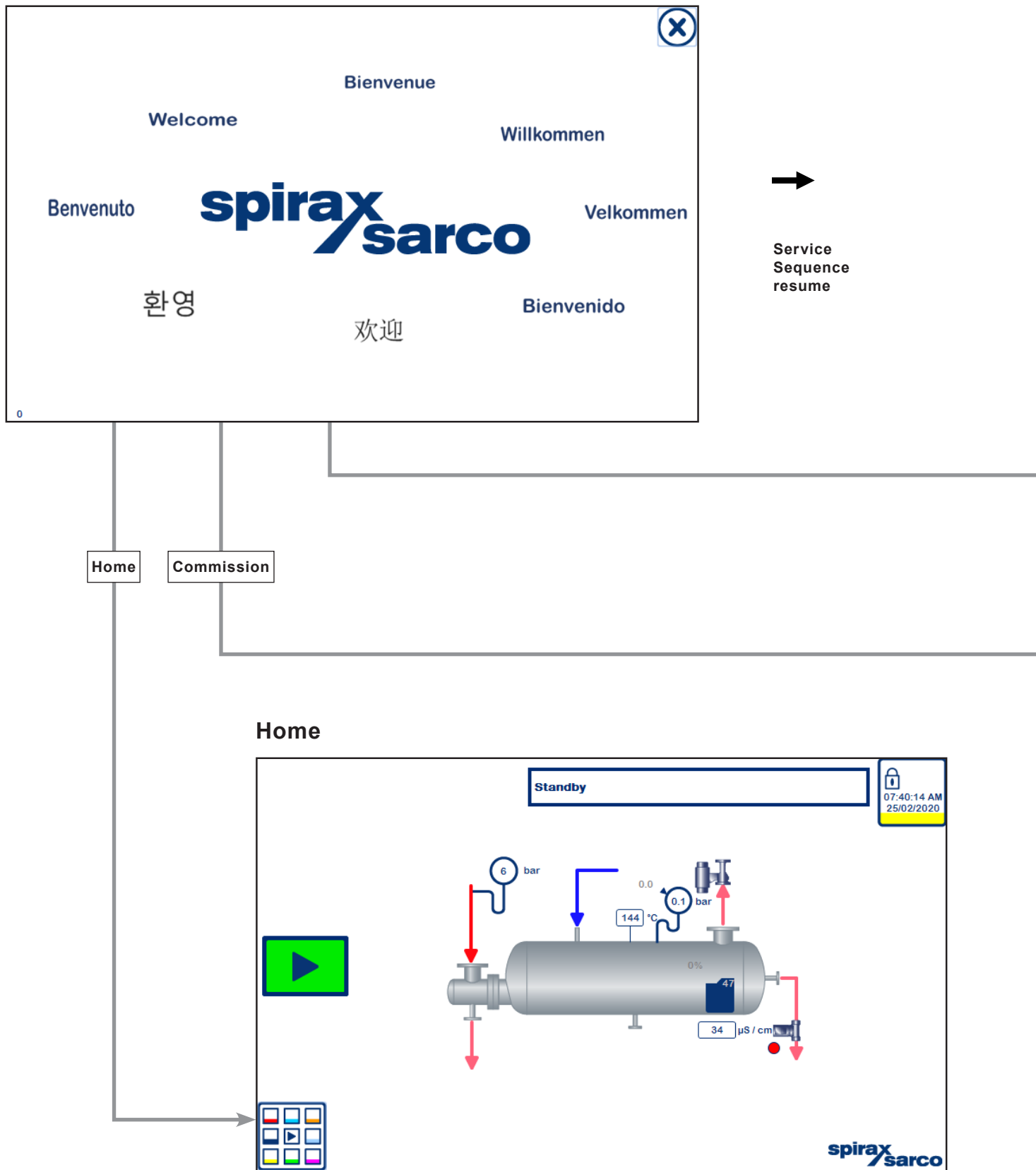
Where multiples of similar devices and parts occur in the same zone, incidence numbers are used to distinguish between them.

Starting points for incidence numbers always start from the component closest the entry of the Zone area.

e.g. On a condensate line, 2 manual valves are identified in Zone 5. The first of the manual valves to come into contact with the condensate as it passes through zone 5 will be given the Incidence number 1.

# 9. HMI map

The following map shows the screens available to all users. Some screens will require a security password to access. The minimum required level is highlighted with the Key shown opposite.



## Level key

1 Level 1: Customer User

2 Level 2: Customer engineer

3 Level 3: Spirax Sarco engineer

## Pre-commission alarm

**Active Alarms**

No.	Time	Text
13	03:50:23 PM	Water level analogue input alarm circuit open
9	03:50:23 PM	Feedwater flow rate analogue input alarm circuit open
5	03:50:23 PM	Water conductivity analogue input alarm circuit open
20	03:50:23 PM	Supply steam in pressure analogue input alarm circuit open
18	03:50:23 PM	Clean steam pressure analogue input alarm circuit open
47	03:50:23 PM	Condensate out temperature analogue input alarm circuit open
45	03:50:23 PM	Condensate temperature analogue input alarm circuit open
43	03:50:23 PM	Supply steam temperature analogue input alarm circuit open
41	03:50:23 PM	Clean steam temperature analogue input alarm circuit open
38	03:50:23 PM	Panel temperature limit alarm
36	03:50:23 PM	Panel temperature analogue input alarm circuit open
34	03:50:23 PM	Feedwater temperature analogue input alarm circuit open
58	03:50:23 PM	Supply steam control valve feedback analogue input alarm
56	03:50:23 PM	Water level control valve feedback analogue input alarm
49	03:50:23 PM	Drain temperature analogue input alarm circuit open
77	03:50:23 PM	Clean steam isolation valve fail stuck

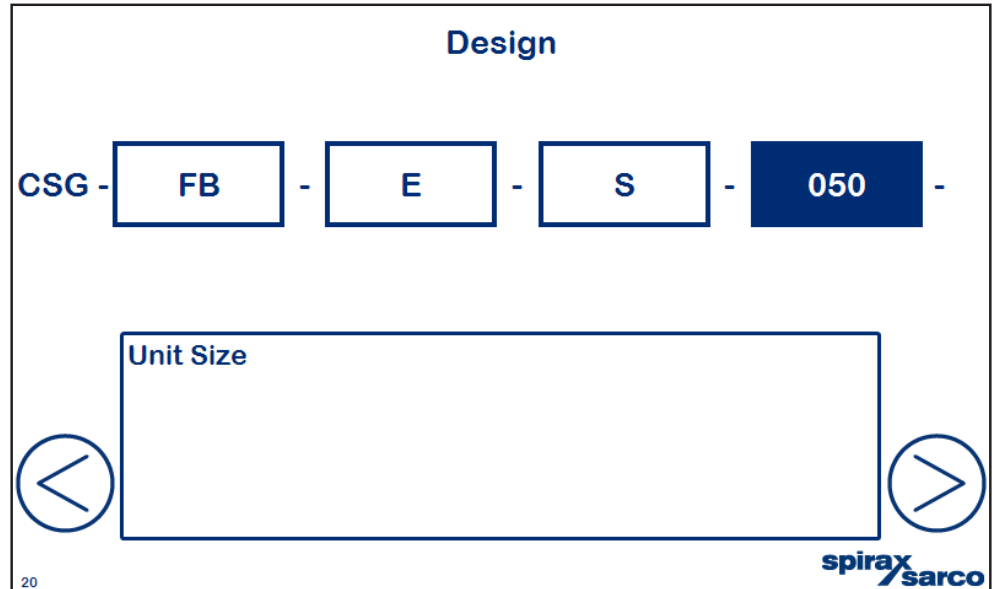
## Commission

Select language

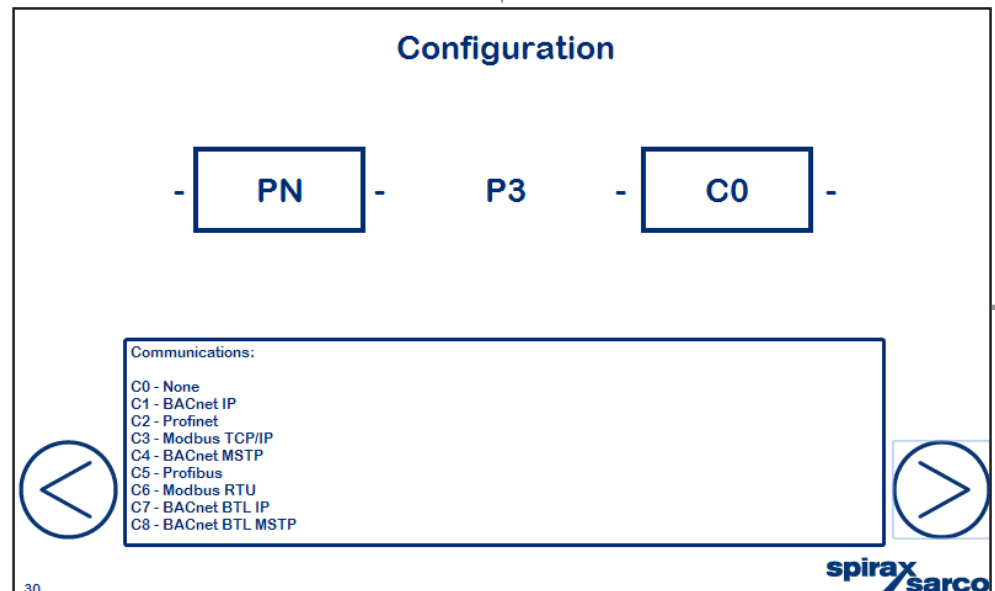
10

## 9.1 Commissioning screens

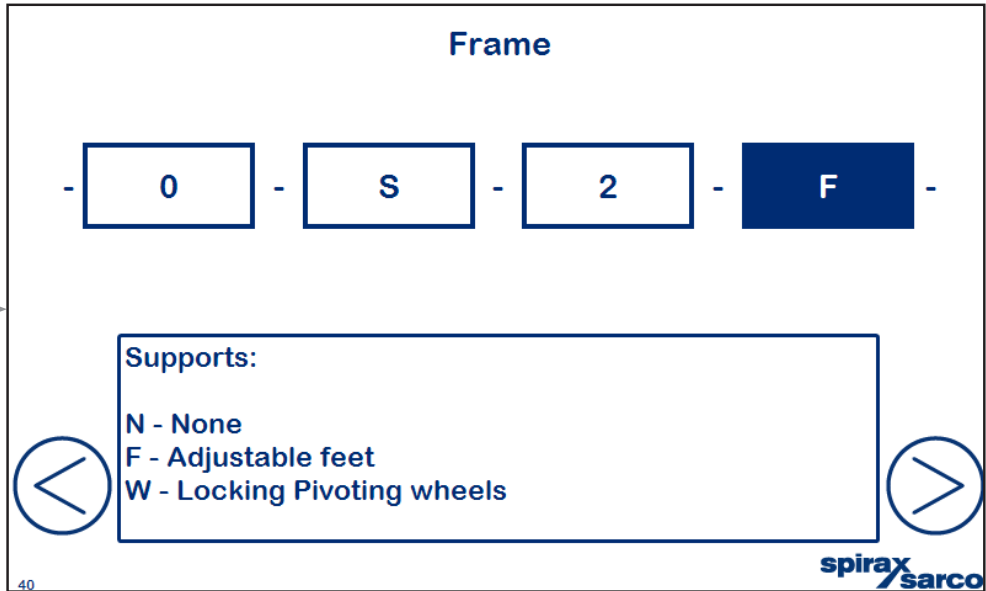
The commissioning screens allow users to input the configuration of the CSG-FB into the control system using the model specific nomenclature. These are generated at the point of ordering and must be referenced to ensure correct operation of the CSG-FB.



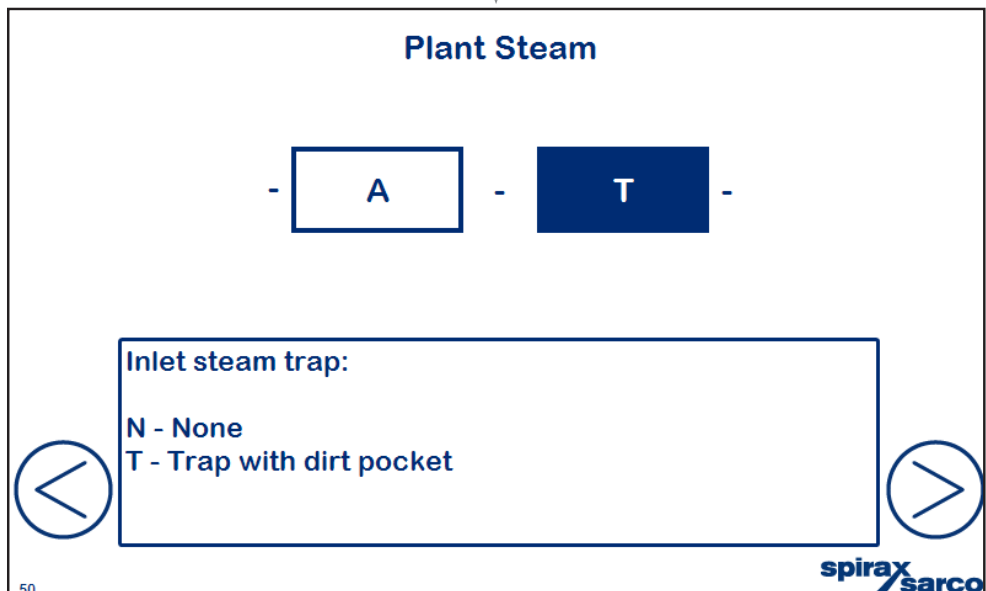
Design



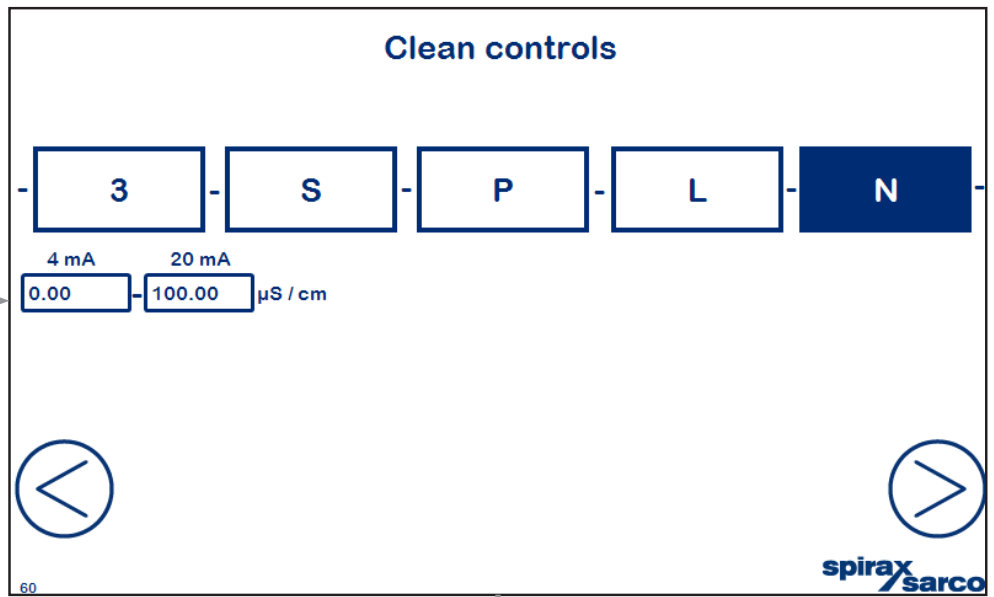
Configuration



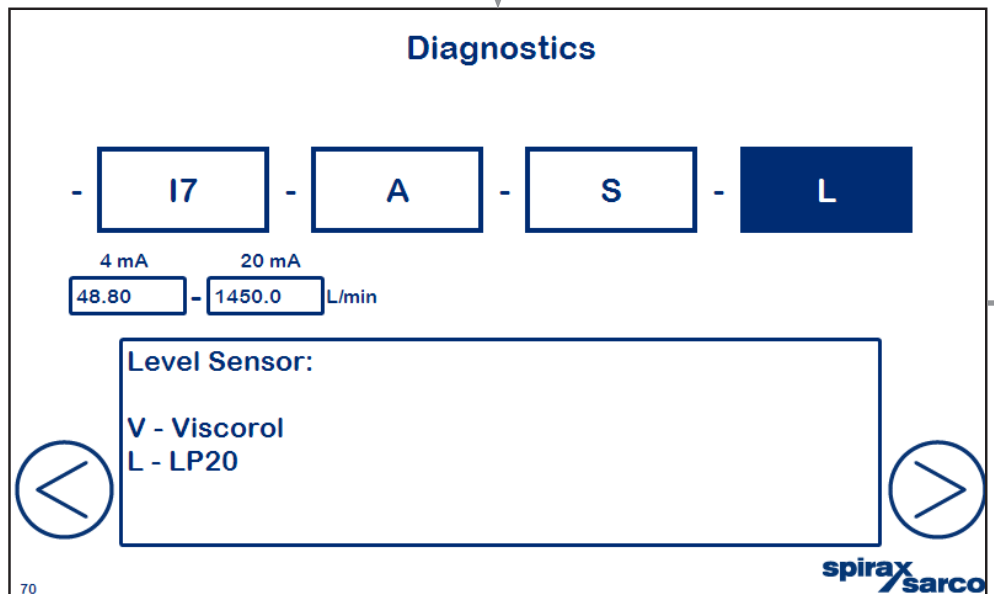
Frame



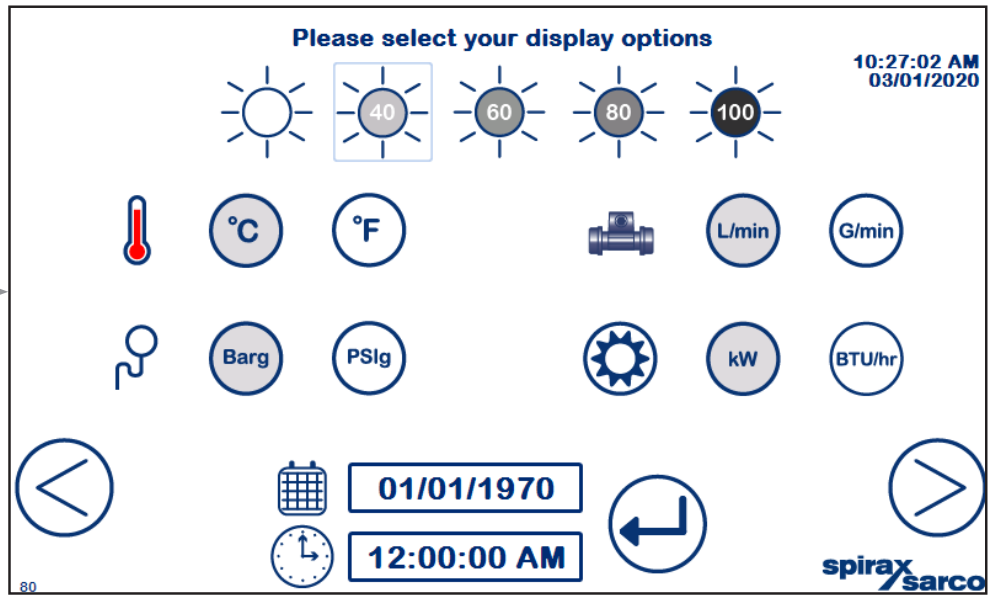
Plant steam



Clean controls



Diagnostics



Display settings

## 9.2 Home screen

The home screen (100) gives the user the ability to quickly view the essential parameters and run status of the CSG-FB. Additionally, more detailed parameters and process values are quickly and easily accessible.

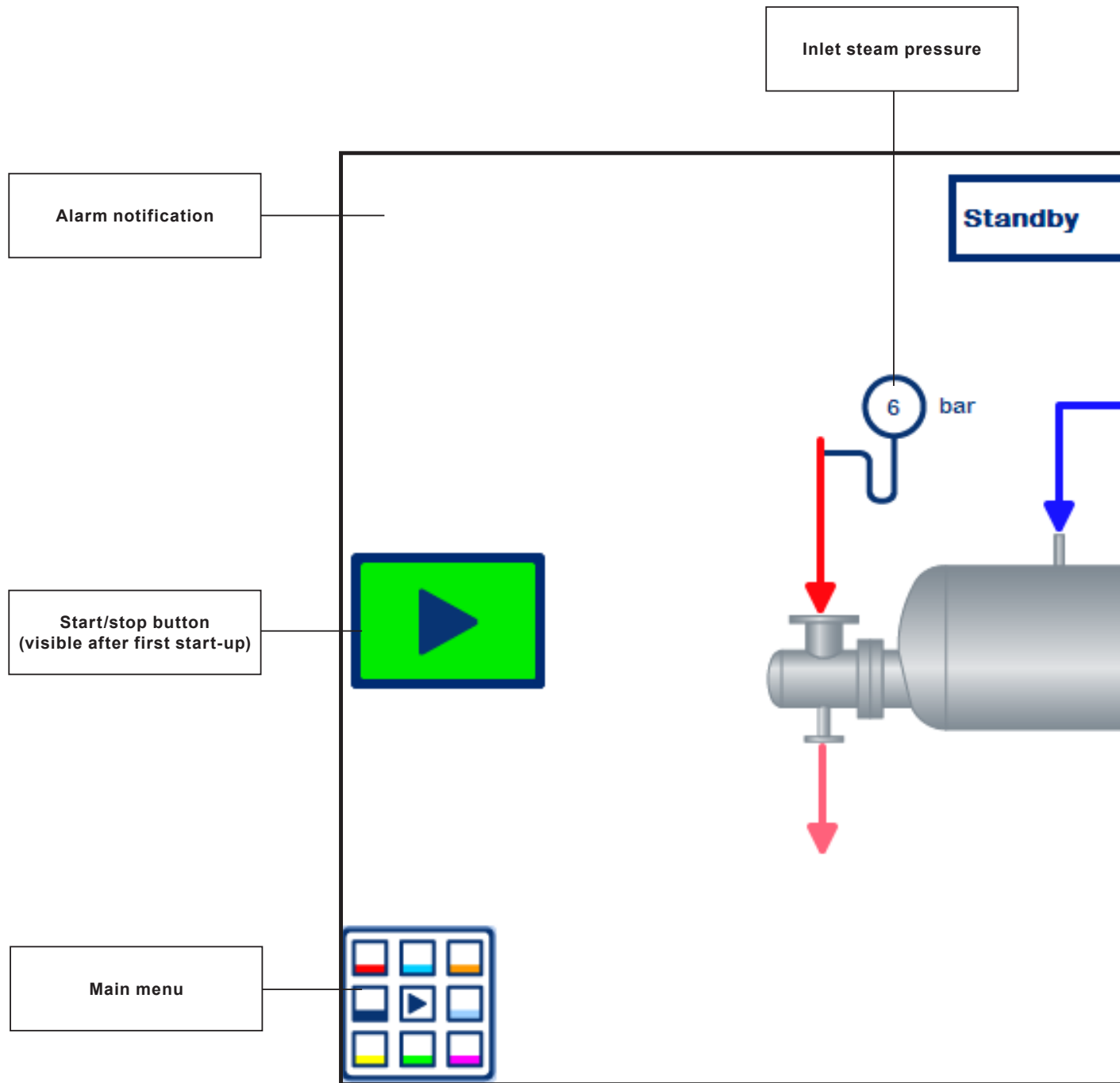
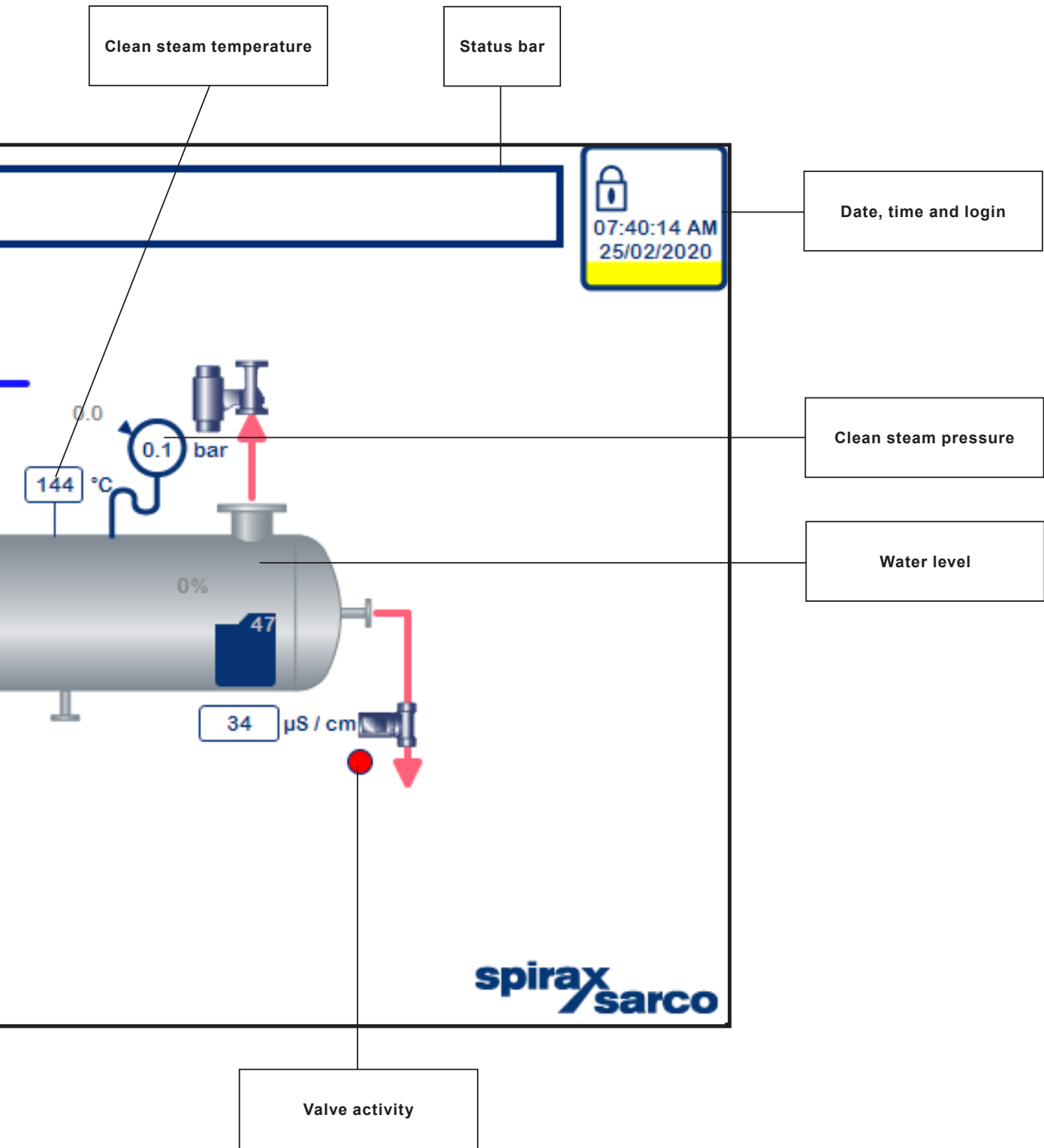
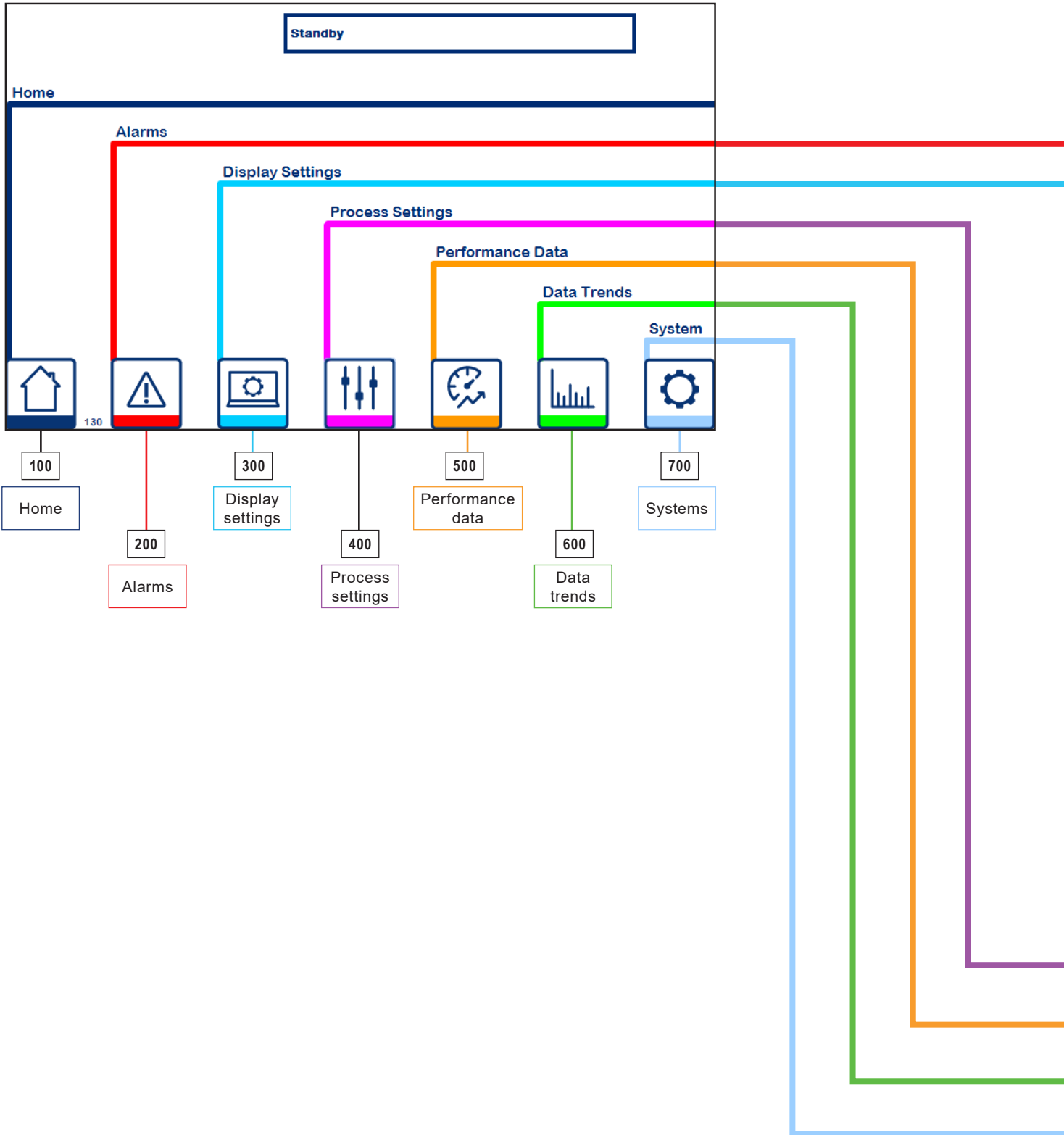


Fig. 10



### 9.3 Main menu

By selecting the Main Menu button from the Home screen, the user has access to settings, alarms and diagnostics screens. These are split in to 6 sub-menus as described below.





**Active Alarms** Standby

No.	Time	Text
13	02:52:59 PM	Water level analogue input alarm circuit open
9	02:52:59 PM	Feedwater flow rate analogue input alarm circuit open
5	02:52:59 PM	Water conductivity analogue input alarm circuit open
20	02:52:59 PM	Supply steam in pressure analogue input alarm circuit open
18	02:52:59 PM	Clean steam pressure analogue input alarm circuit open
47	02:52:59 PM	Condensate out temperature analogue input alarm circuit open
45	02:52:59 PM	Condensate temperature analogue input alarm circuit open
43	02:52:59 PM	Supply steam temperature analogue input alarm circuit open
41	02:52:59 PM	Clean steam temperature analogue input alarm circuit open
38	02:52:59 PM	Panel temperature limit alarm
36	02:52:59 PM	Panel temperature analogue input alarm circuit open
34	02:52:59 PM	Feedwater temperature analogue input alarm circuit open
58	02:52:59 PM	Supply steam control valve feedback analogue input alarm circuit open

12:42:32 AM  
03/01/1970

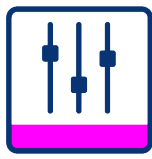
200



**Display** Standby

12:47:16 AM  
03/01/1970

300



2

400 Main 2 Tune 0 11.85 bar 237.03°C  
Standby 10:32:18 AM 03/01/2020

1.0 bar 5 mins  
70% 5 mins

23 : 59

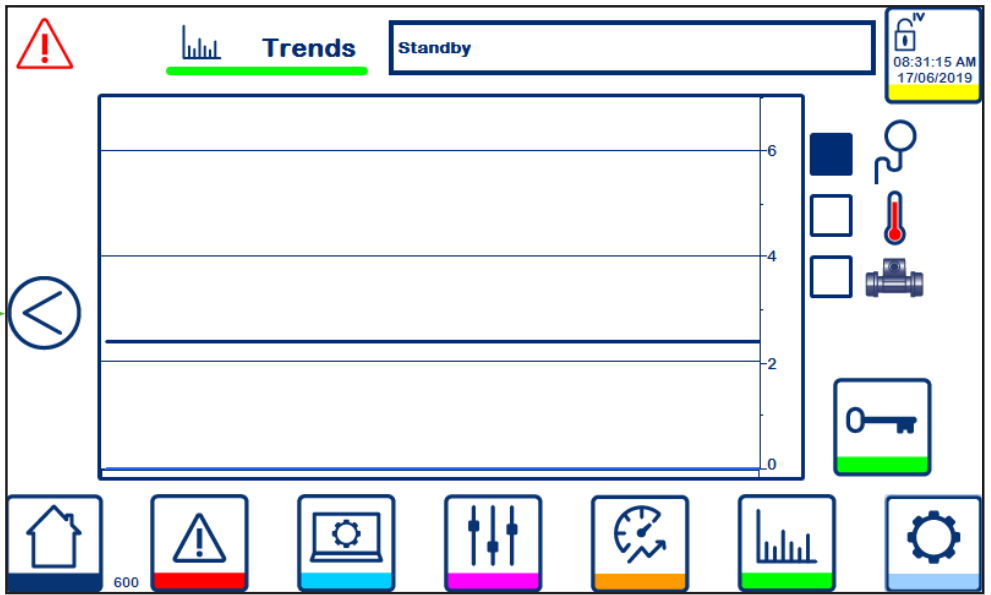
Process settings



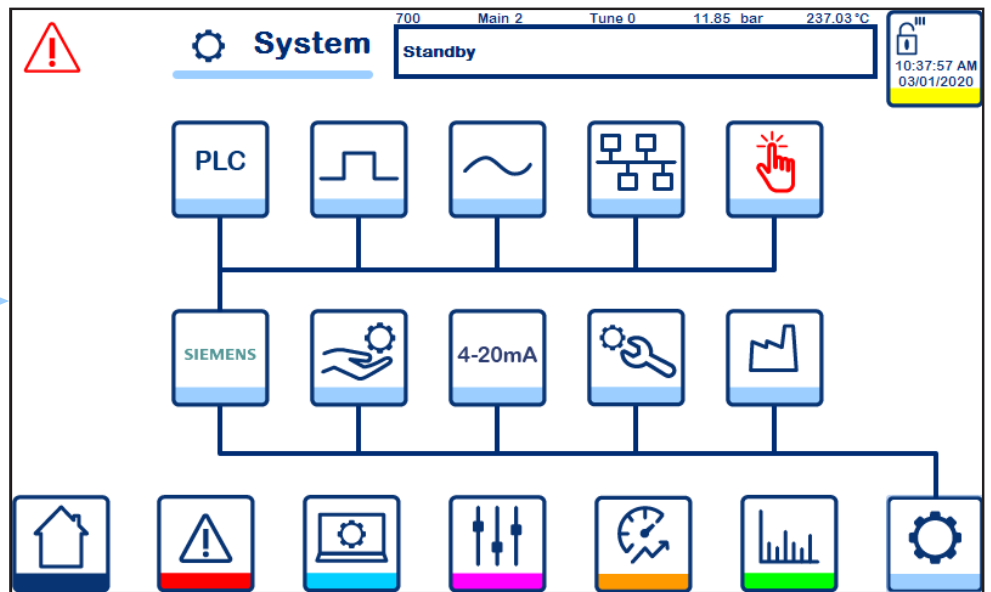
500 Main 2 Tune 0 11.85 bar 237.03°C  
Standby 10:35:36 AM 03/01/2020

Performance delta 0.00  
Sample stop 0 HRS  
Last test #### mins

Performance



2



## 9.4 Alarms

The alarm screens display active and historic alarms as well as all the settings for the diagnostics alarms.

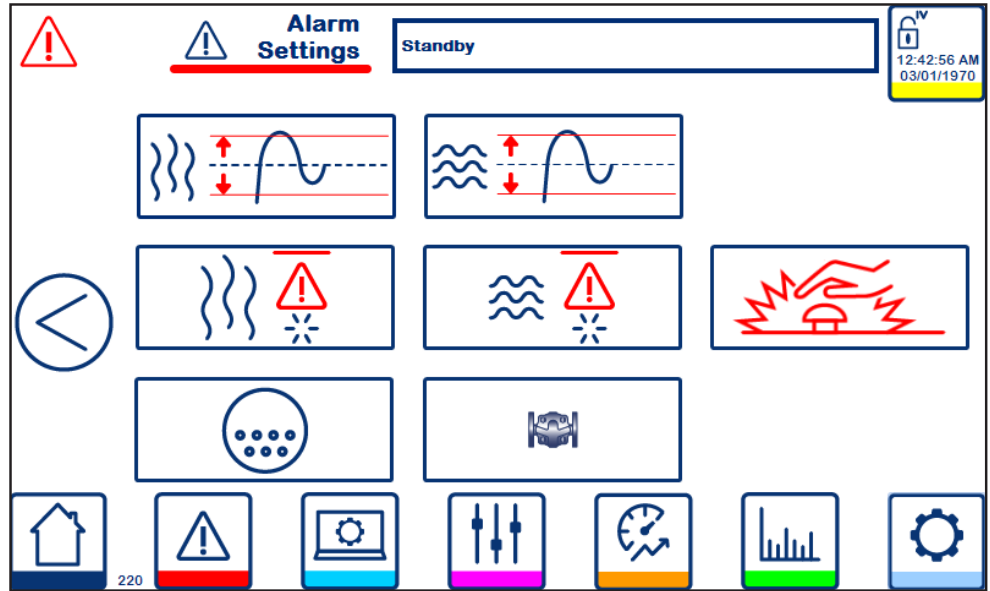


No.	Time	Text
13	02:52:59 PM	Water level analogue input alarm circuit open
9	02:52:59 PM	Feedwater flow rate analogue input alarm circuit open
5	02:52:59 PM	Water conductivity analogue input alarm circuit open
20	02:52:59 PM	Supply steam in pressure analogue input alarm circuit open
18	02:52:59 PM	Clean steam pressure analogue input alarm circuit open
47	02:52:59 PM	Condensate out temperature analogue input alarm circuit open
45	02:52:59 PM	Condensate temperature analogue input alarm circuit open
43	02:52:59 PM	Supply steam temperature analogue input alarm circuit open
41	02:52:59 PM	Clean steam temperature analogue input alarm circuit open
38	02:52:59 PM	Panel temperature limit alarm
36	02:52:59 PM	Panel temperature analogue input alarm circuit open
34	02:52:59 PM	Feedwater temperature analogue input alarm circuit open
58	02:52:59 PM	Supply steam control valve feedback analogue input alarm

Active alarms (200) remains on screen until they are acknowledged by the user.

No.	Time	Text
! 13	02:52:59 PM	Water level analogue input alarm circuit open
! 9	02:52:59 PM	Feedwater flow rate analogue input alarm circuit open
! 5	02:52:59 PM	Water conductivity analogue input alarm circuit open
! 20	02:52:59 PM	Supply steam in pressure analogue input alarm circuit open
! 18	02:52:59 PM	Clean steam pressure analogue input alarm circuit open
! 47	02:52:59 PM	Condensate out temperature analogue input alarm circuit open
! 45	02:52:59 PM	Condensate temperature analogue input alarm circuit open
! 43	02:52:59 PM	Supply steam temperature analogue input alarm circuit open
! 41	02:52:59 PM	Clean steam temperature analogue input alarm circuit open
! 38	02:52:59 PM	Panel temperature limit alarm
! 36	02:52:59 PM	Panel temperature analogue input alarm circuit open
! 34	02:52:59 PM	Feedwater temperature analogue input alarm circuit open
! 58	02:52:59 PM	Supply steam control valve feedback analogue input alarm

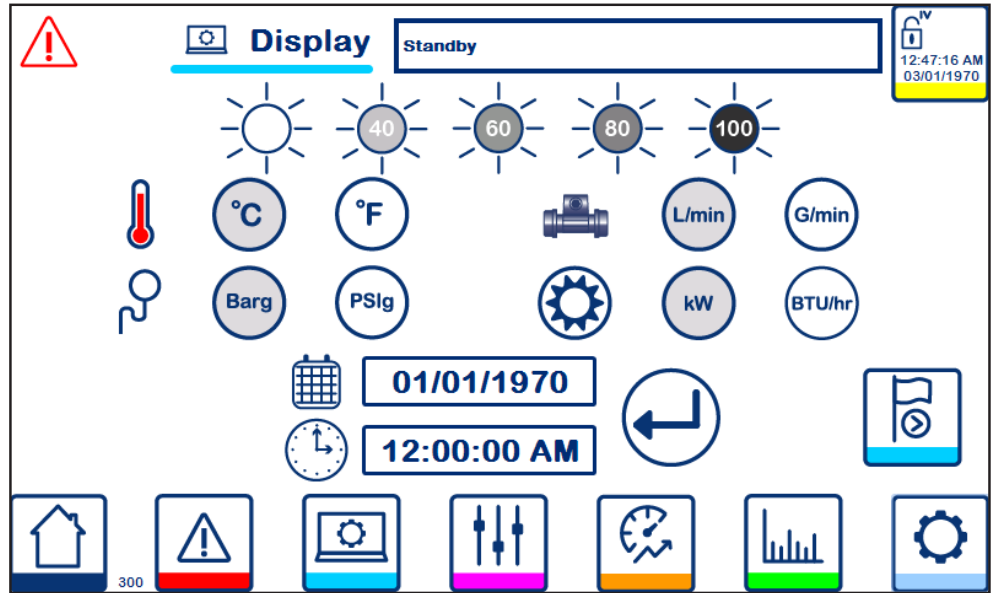
Alarms history (210) provides an historic log of previous alarms including time and date stamp for clarification and diagnosis. A rolling total of 1024 alarms are retained until a power cycle of the CSG-FB.



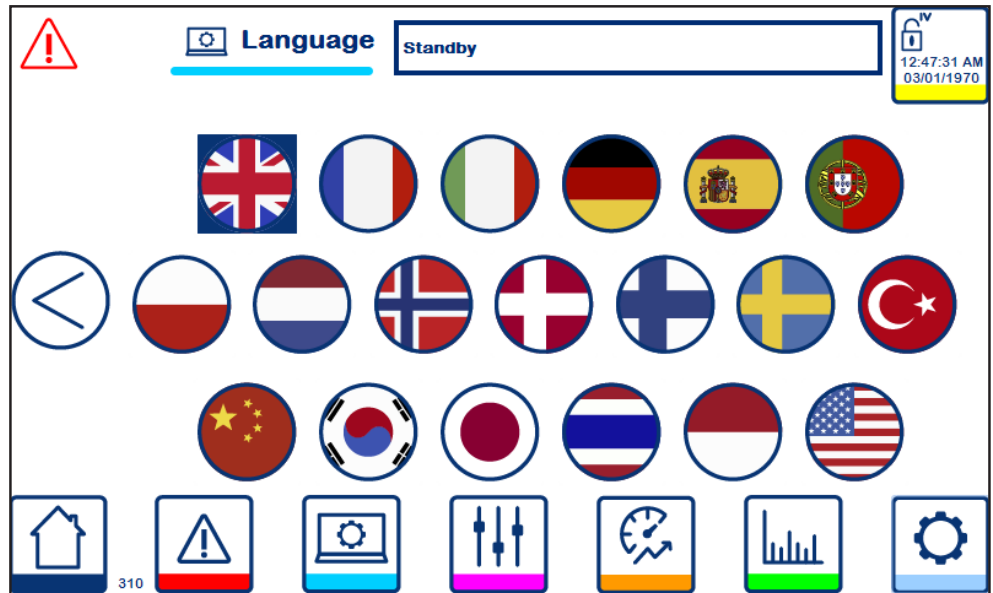
Alarm settings (220)

## 9.5 Display settings

The display settings screen, as well as altering the display units for the HMI, the user can also alter the time, date and language.



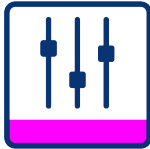
Display settings (300)



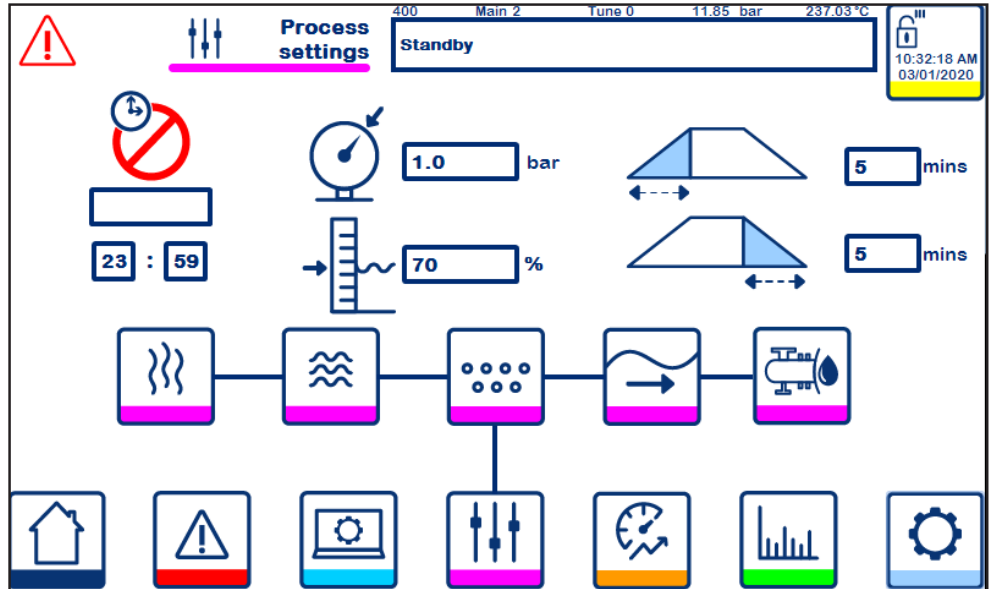
Language (310)

## 9.6 Process settings

The settings available across the process settings screens directly affect the running of the CSG-FB and the effective output of clean steam.



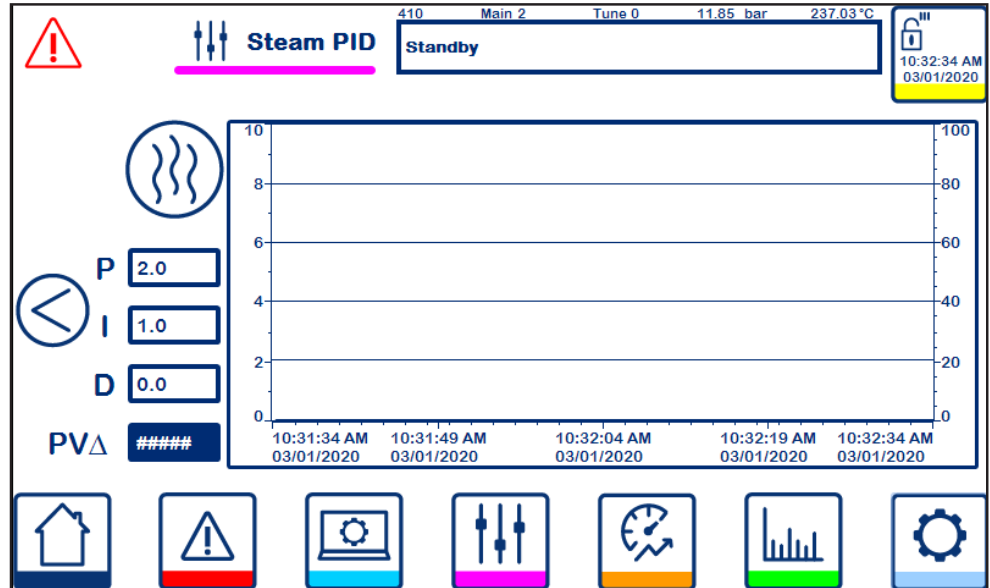
2



Main process set-points (400). Including clean steam pressure, water level, ramp up time and ramp down time.



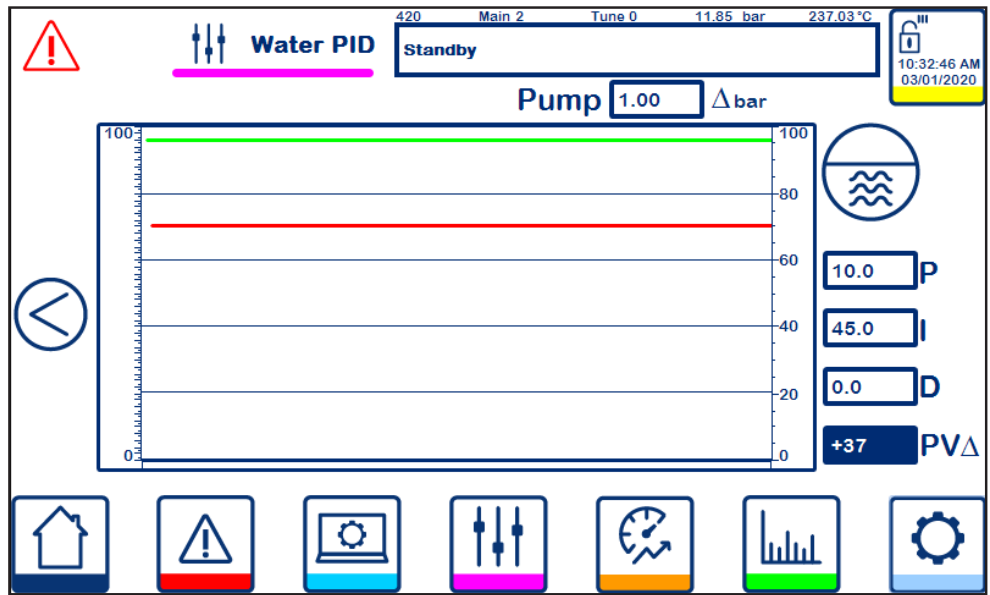
2



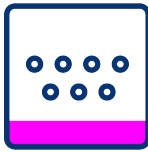
Steam PID settings (410) also includes a live PID graph showing the process and control values, and the process set-point.



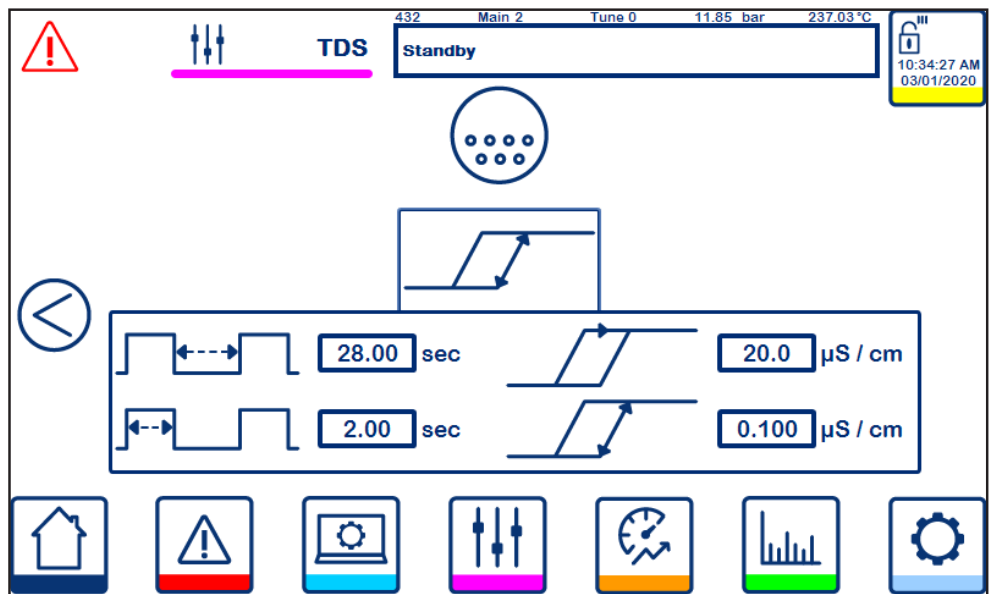
2



Water PID settings (420) also includes the pump offset value and a live PID graph showing the process and control values, and the process set-point.



2



TDS settings (430-432) allows the user to set and select the TDS control they require.



2

440 Main 2 Tune 0 11.85 bar 237.03°C

Standby

10:33:31 AM  
03/01/2020

High Demand drop  %

Low Demand rate

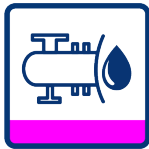
Level SP rise  %

Pressure SP drop  %

Demand duration  sec

Demand enable time  sec

Forward controls (440)



2

450 Main 2 Tune 0 11.85 bar 237.03°C

Standby

10:33:46 AM  
03/01/2020

Enable

Integrity test duration  sec

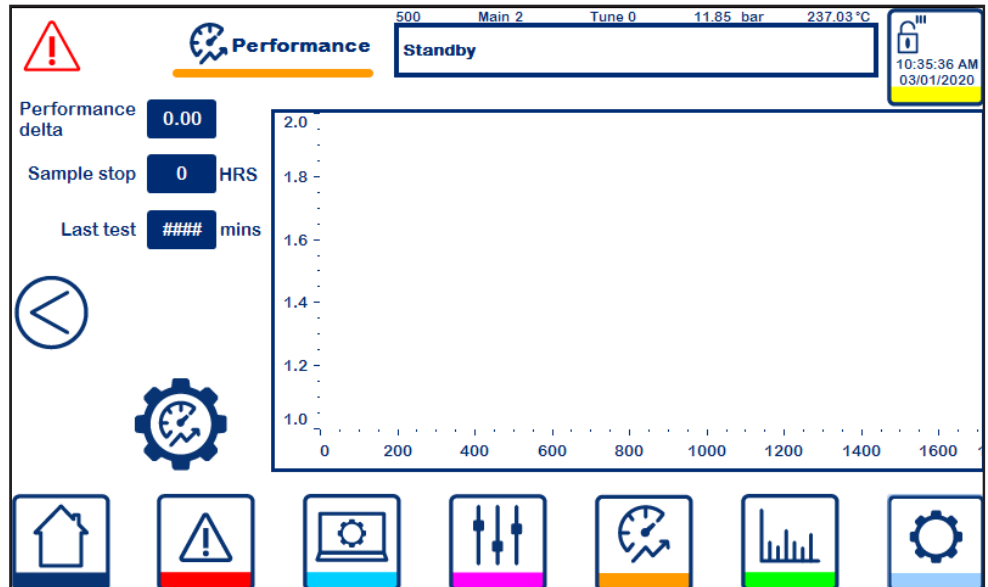
Pressure drop limit  %

Pressure rise limit  %

Integrity test (450)

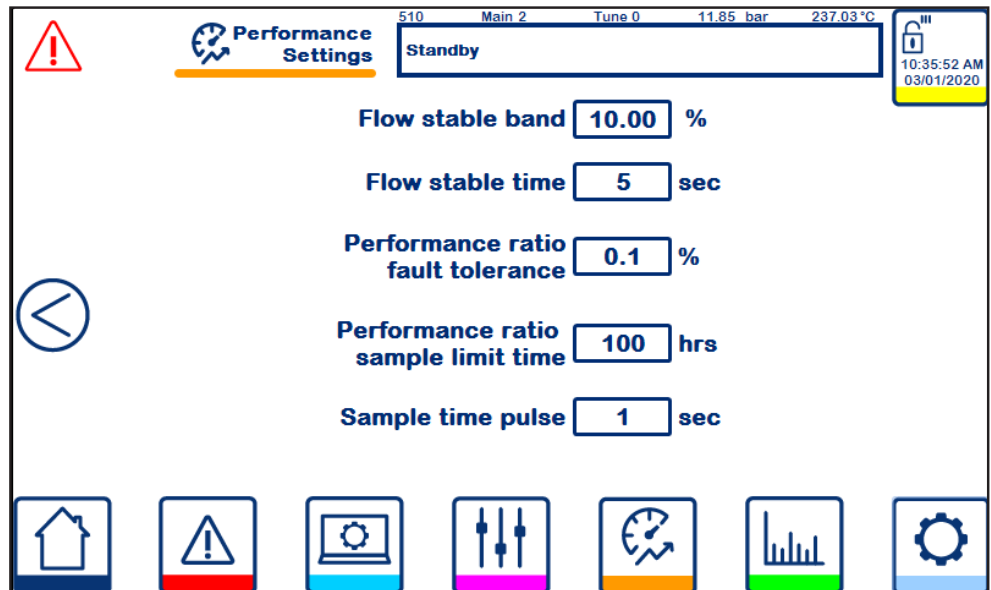
## 9.7 Performance data

The performance data screen will only display the performance profile of the CSG-FB whist in Running mode and once sufficient data has been collected. If the Performance Monitoring options pack has not been installed, no information will be available.



Performance data (500), as well as showing the current performance profile of the CSG-FB also shows the current data sample and data times.

2



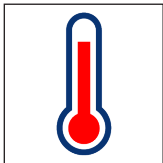
Performance data settings (510) allows users to alter the sampling process and performance tolerance.

## 9.8 Data trends

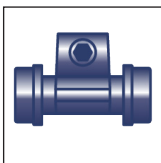
The live data displayed on the Trends screen is grouped in to similar process values.



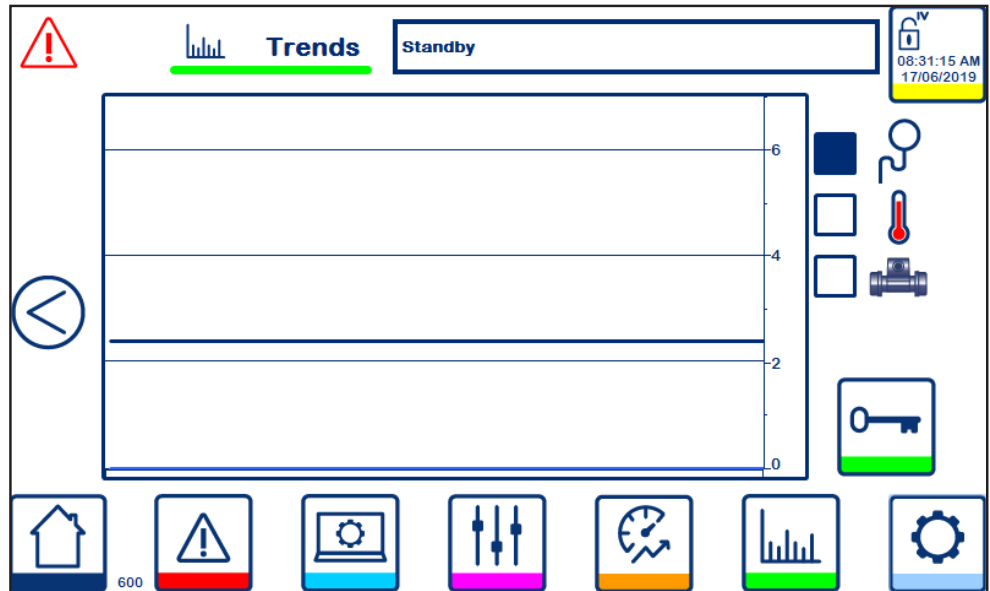
Pressure variables.  
All currently installed  
pressure sensors.



Temperature variables.  
All currently installed  
temperature sensors.



Flow variable from FA01 if  
installed.



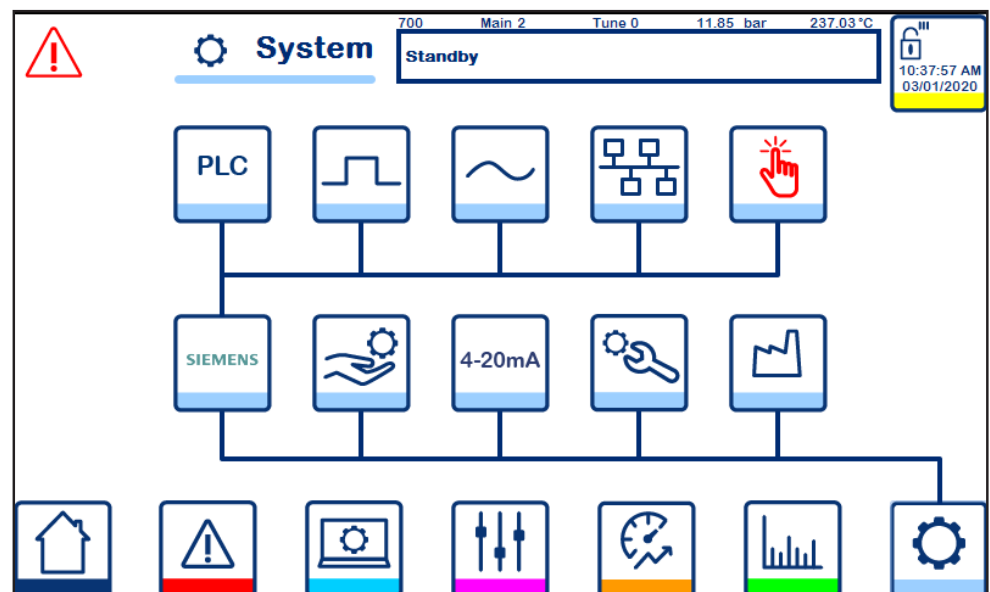
Trends (600) provided a live feed of the selected process variables.

## 9.9 System

System related controls and settings are available for the advanced user to alter the CSG-FB away from a pre-configured settings.



2



System sub menu (700)



2

PLC status (710) displays any PLC error codes and the stored PLC date and time.

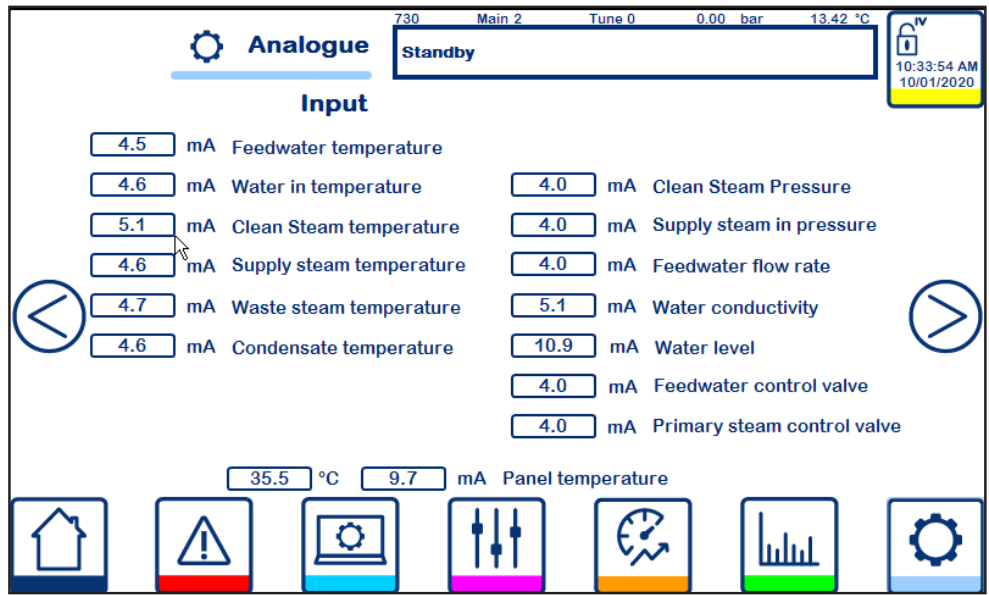


2

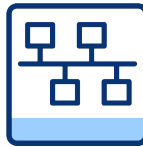
Digital Input status (720) and digital output status (721)



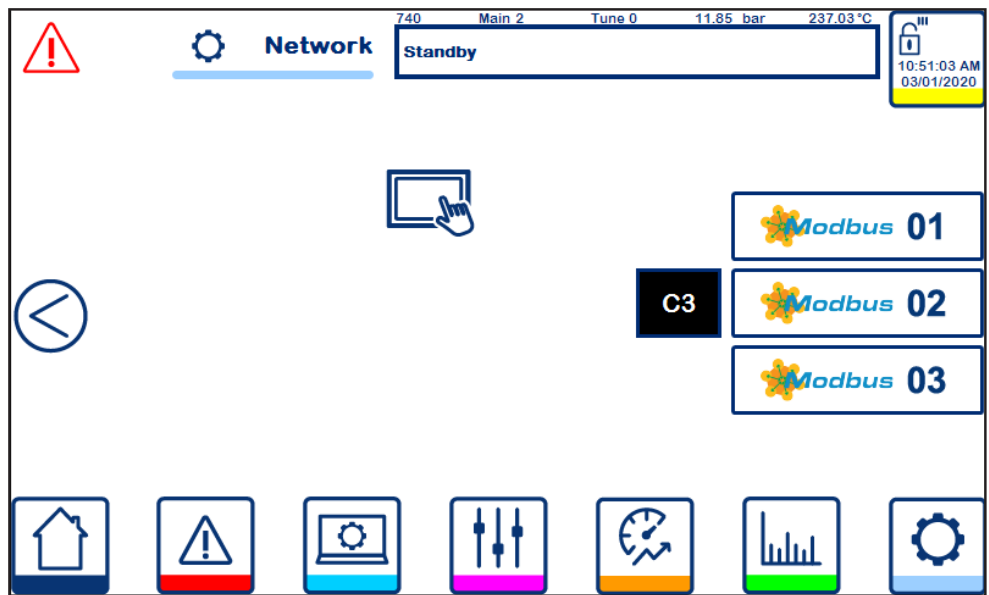
2



Analogue input status (730) and analogue output status (731)



2



Network status (740)

2

741 Main 2 Tune 0 11.85 bar 237.03°C

Standby

11:40:58 AM 03/01/2020

Address	Description	Value
1	PA01 feedwater pressure	1185
2	PA21 clean steam pressure	1185
3	TA01 feedwater temp	23703
4	TA21 clean steam temp	23703
5	FA01 feedwater flow rate	17094
6	CA11 conductivity	11851
7	LA21 Water level	9567
8	VB01 Feedwater control value	0
9	VA01 Feedwater control valve feedback	11851
10	VB31 Supply steam control value	0

Modbus 01  
Modbus 02  
Modbus 03

Communications tables and status (741-745)

2

742 Main 2 Tune 0 11.85 bar 237.03°C

Standby

11:41:11 AM 03/01/2020

Address	Description	Value
11	VA31 Supply steam control valve feedback	11851
12	Clean steam pressure PID SP	0
13	Water level PID SP	7000
14	TDS SP	2000
15	Clean steam superheat	2401
16	NCG %	50864
17	Run timer	0
18	Diagnostic WORD	640
19	Alarms 1 WORD	20880
20	Alarms 2 WORD	10

Modbus 01  
Modbus 02  
Modbus 03

2

Address	Description	Value
21	Alarms 3 WORD	17706
22	Alarms 4 WORD	6785
23	Alarms 5 WORD	4393
24	Alarms 6 WORD	130
25	Run status	2
26	Watchdog out	41
27	Watchdog return	99
28	Command WORD	0
29	Remote Clean Steam Pressure Set-point	0
30	Spare	0

2

- VE12 TDS valve
- VE21 Outlet Isolation valve
- VE31 Inlet Isolation valve
- VE32 Test, level isolation valve
- VE33 Test, compressed air/vent valve
- VE51 Test, condensate isolation valve

Digital override (750) open and close fitted and available isolation valves (only available in standby mode)



2

751 Main 2 Tune 0 11.85 bar 237.03°C

Standby

10:54:00 AM  
03/01/2020

VB01 Feedwater supply valve 0.0 %

VB31 Primary steam control valve 0.0 %

MB01 Feedwater pump pressure 0.0 bar

Analogue override (751) enable and move control valves to specific position. (only available in standby mode)



2

760 Main 2 Tune 0 11.85 bar 237.03°C

Standby

11:29:24 AM  
03/01/2020

Service (760) allows users to begin service sequence, enter PID Tuning mode (only available in standby mode) or Running Tuning mode (only available when in Run mode).

4-20mA

2

Variable	4 mA	20 mA
FA01 Feedwater Flow rate	48.8	1450.0
PA21 Clean Steam pressure	0.0	10.0
PA31 Supply steam pressure	0.0	10.0
CA11 Water conductivity	0.00	100.00
LA11 Water level	16.7	83.3
FA01 Feedwater flow smoothing	2 x 0.2sec	10 x samples
LA11 Water level smoothing	1 x 0.2sec	2 x samples

Scaling (770) allows alteration of the 4-20 mA input scaling and the input smoothing of FA01 and LA11 (only available in standby mode).

3

CSG - 1 HS 2 E 3 F 4 055 - 5 PN P3 7 C3 - Water setpoint delta select

8 0 9 S 10 2 11 F - 12 A 13 T - Warmup pressure check

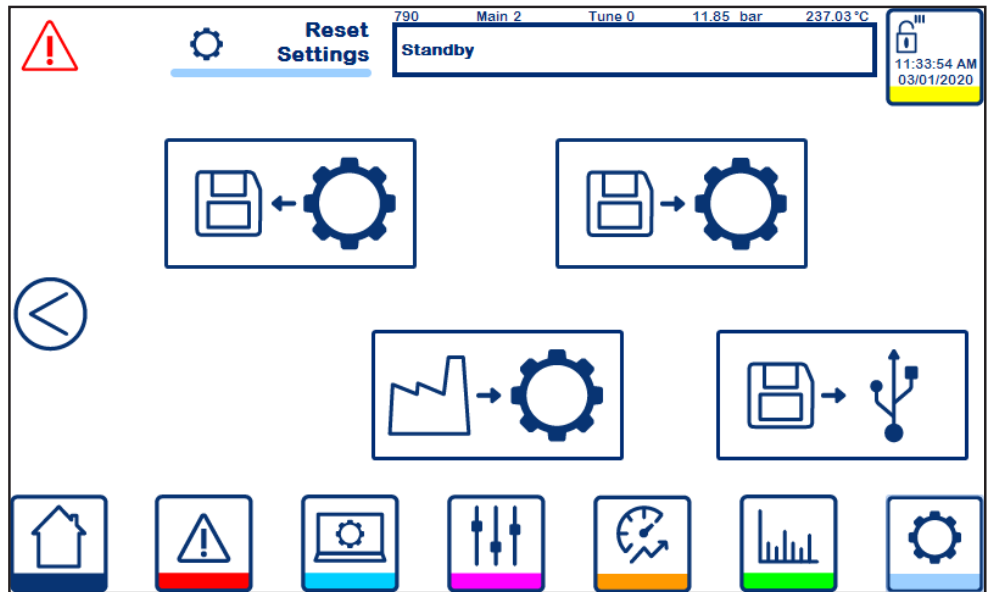
14 3 15 S 16 P 17 L 18 N 19 I7 - VB31 Warm 10.0 %

20 A 21 S 22 L Pressure SP 1.0 - 6.0 bar

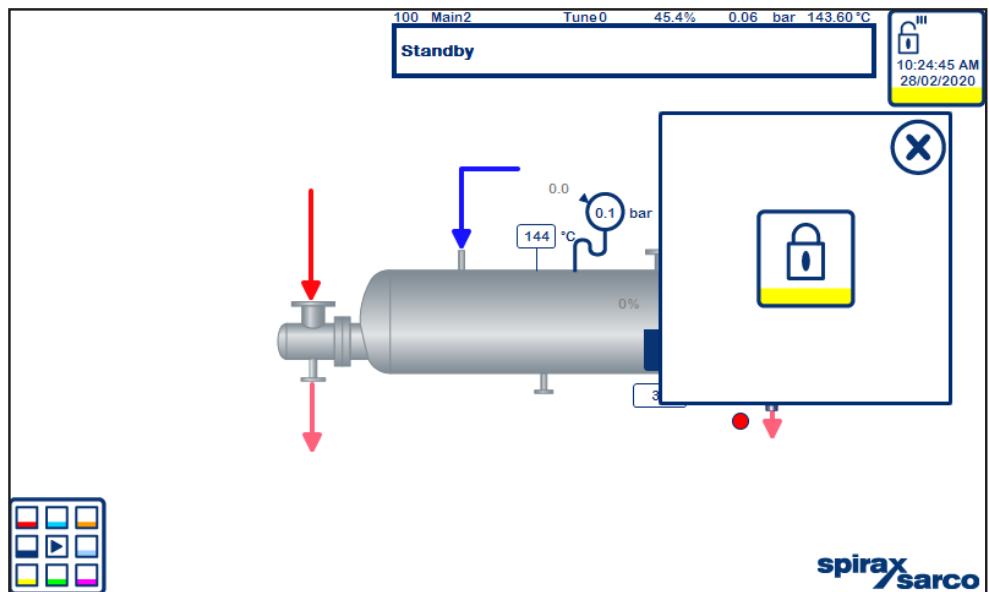
Atmospheric pressure 1.013 bar



2



Factory reset (790) allows users to save, load and reset the current settings and configuration of the CSG-FB. (only available in standby mode)



Security screen (800), allows users to logoff from the current user.

# 10. Appendix

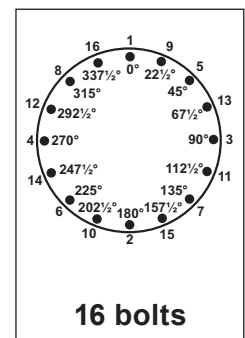
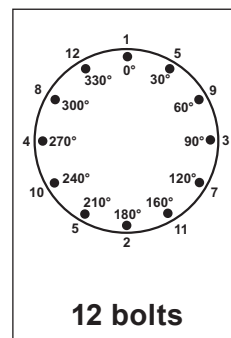
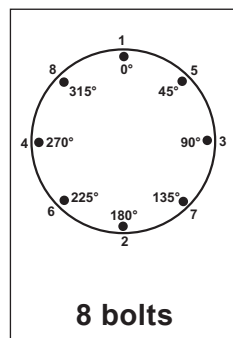
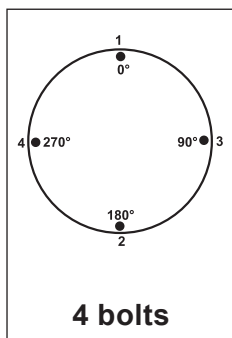
The torquing procedure should follow the steps detailed in this Appendix:

- Lubricate the bolt threads and the nut faces with a suitable lubricant.
- Insert the bolts through the flanges and finger tighten the nuts.
- Number all bolts so that torquing requirements can be followed.
- Apply torque in 20%, 1/5 steps of required final torque, loading all bolts at each step before proceeding to the next step.
- Use rotational tightening until all bolts are stable at final torque level.

The torque tightening values for the clean steam generator header and deareator flanges are detailed in the following table:

	Header flange bolts			Deaerator flange bolts		
	Quantity	Ø	Torque* (N m)	Quantity	Ø	Torque* (N m)
<b>GVS400</b>	4	M14	25	12	M20	50
<b>GVS500</b>	8	M16	40	12	M24	80
<b>GVS601</b>	12	M16	45	16	M27	125
<b>GVS602</b>	12	M16	45	16	M27	125

\* Gaskets as per original spare parts




















































Sequential Order	Rotational Order
1-2	1
3-4	3
	2
	4



Sequential Order	Rotational Order
1-2	1
3-4	5
5-6	3
7-8	7
	2
	6
	4
	8

Sequential Order	Rotational Order
1-2	1
3-4	5
5-6	9
7-8	3
9-10	7
11-12	11
	2
	6
	10
	4
	8
	12

Sequential Order	Rotational Order
1-2	1
3-4	9
5-6	5
7-8	13
9-10	3
11-12	11
13-14	7
15-16	15
	2
	10
	6
	14
	4
	12
	8
	16

	Setting	Units	Lower limit	Upper limit	Default	Setting
	<b>Alarm settings</b>					
	<b>Clean steam pressure band alarm</b>					
	High band	%	1.0	10.0	10.0	
	Low band	%	1.0	10.0	10.0	
	Alert time	sec	1	30	10	
	Alarm time	sec	30	180	30	
	<b>Water level band alarm</b>					
	High band	%	1.0	10.0	10.0	
	Low band	%	1.0	10.0	10.0	
	Alert time	sec	1	30	10	
	Alarm time	sec	30	180	30	
	<b>Clean steam control capacity alarm</b>					
	Alert time	sec	1	60	30	
	Alarm time	sec	1	60	60	
	<b>Water level control capacity alarm</b>					
	Alert time	sec	1	60	30	
	Alarm time	sec	1	60	60	
	<b>TDS alarm</b>					
	TDS high time	sec	0	600	600	
	Hysteresis time	sec	0	600	600	
	<b>Water level band alarm</b>					
	Trap fail open temperature difference	°C			15.0	
	Trap fail closed temperature	°C			15.0	
	Maximum water level valve opening	sec	0.0	20.0	5.0	
	Maximum clean steam valve opening	sec	0.0	20.0	10.0	
	<b>Process settings</b>					
	<b>Main process</b>					
	Clean steam pressure	bar	1.0	6.0	1.0	
	Water level	%	60	80	70	
	Ramp up time	min	2	10	5	
	Ramp down time	min	2	10	5	
	Timed shut-down	time	00:00	23:59	disabled	
	<b>Clean Steam PID</b>					
	Proportional gain	-	1.0		2.0	
	Integral gain	-	0.0		1.0	
	Derivative gain	-	0.0		0.0	

	Setting	Units	Lower limit	Upper limit	Default	Setting
	<b>Water level PID</b>					
	Proportional gain	-	1.0		10.0	
	Integral gain	-	0.0		45.0	
	Derivative gain	-	0.0		0.0	
	Pump pressure	Δbar	0.5	2.0	1.0	
	<b>TDS (Interval only)</b>					
	Interval time	sec	5.00		28.00	
	Duration time	sec	0.00		2.00	
	<b>TDS (CP10)</b>					
	Interval time	sec	5.00		28.00	
	Duration time	sec	0.00		2.00	
	TDS setpoint	μS	10.0		35.0	
	Hysteresis band	μS	0.001	20.000	0.100	
	<b>TDS (CP32)</b>					
	Interval time	sec	5.00		28.00	
	Duration time	sec	0.00		2.00	
	TDS setpoint	μS	10.0		35.0	
	Hysteresis band	μS	0.001	20.000	0.100	
	<b>Forward Controls</b>					
	High Demand drop	%	5.00	20.00	10.00	
	Level SP rise	%			10	
	Low Demand rate		0.00	1.00	0.10	
	Pressure SP drop	%			10	
	Demand duration	sec	1	10	5	
	Demand enable time	sec	1	60	10	
	<b>Integrity test</b>					
	Integrity test duration	sec			60	
	Pressure drop limit	%	-100	-1	-2	
	Pressure rise limit	%	100	1	2	
	<b>Performance Monitoring</b>					
	Flow stable band	%			10.00	
	Flow stable time	sec			5	
	Performance ratio fault tolerance	%			0.1	
	Performance ratio sample limit time	hrs			100	
	Sample time pulse	sec			1	

	Setting	Units	Lower limit	Upper limit	Default	Setting
	<b>4-20mA</b>					
	FA01 4mA	L/min			48.80	
	FA01 20mA	L/min			1450.0	
	PA01 4mA	bar			0.00	
	PA01 20mA	bar			10.0	
	PA21 4mA	bar			0.00	
	PA21 20mA	bar			10.0	
	PA31 4mA	bar			0.00	
	PA31 20mA	bar			10.0	
	CA11 4mA	µS			0.0	
	CA11 20mA	µS			100.0	
	LA11 4mA (Viscorol)	%			0.0	
	LA11 20mA (Viscorol)	%			100.0	
	LA11 4mA (LP20)	%			16.7	
	LA11 20mA (LP20)	%			83.3	
	FA01 Feedwater flow smoothing				Enable	
	FA01 smothing interval	0.2sec			2	
	FA01 smothing samples				10	
	LA11 Water level smoothing				Disable	
	LA11 smothing interval	0.2sec			1	
	LA11 smothing samples				2	
	<b>Configuration</b>					
	Water setpoint delta select				Enable	
	Warmup pressure check				Enable	
	VB31 warm	%			10.0	
	Pressure SP minimum	bar	0.0	10.0	1.0	
	Pressure SP maximum	bar	0.0	10.0	6.0	
	Atmospheric Pressure	barA			1.013	

# 11. Troubleshooting

## 11.1 Alarms

Diagnostics critical to the equipment or the process that require intervention to correct or monitor.

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
3	ALA_TEST_LEAK	Cold leak test alarm	Leak pipe joints	Ceased production of clean steam	Emergency stop displayed	Leak in pipe joints	-	-	-	-	-	-	-	-	Inspect pipe joints
			Leak in steam control valve			Leak in steam control valve	VA31	Steam control valve	Anaolgue input	3	1	-	Inspect steam control valve		
			Leaks in Integrity test valves			Leak in isolation valves	-	-	-	-	-	-	Inspect isolation valves		
4	ALARM_SERV_STOP	Temperature or pressure alarm in service sequence	Hot pipes	Temperature or pressure detected	System isolation not complete	-	-	-	-	-	7	COND_TEMP_HI	Condensate temperature hot	Inspect isolation valves	
											11	FEED_PRES_HI	Feedwater pressurised		
											12	FEED_TEMP_HI	Feedwater temperature hot		
											25	PRI_PRES_HI	Primary side pressurised		
											27	PRI_TEMP_HI	Primary side temperature hot		
											32	SEC_PRES_HI	Secondary side pressurised		
											33	SEC_TEMP_HI	Clean steam temperature hot		
											62	WASTE_TEMP_HI	Waste steam temperature hot		
64	WASTE_TEMP_HI	Water in temperature hot													
5	CA11_ANLG_ALA_OPEN	Water conductivity Analog input alarm circuit open	Cables removed from sensor	Flashing conductivity readings	-	-	-	-	-	1	1	Operator error		Replace cable	
												Refer to technical documentation		Replace sensor	
												Refer to technical documentation		Replace controller	

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
6	CA11_ANLG_ALA_SHRT	Water conductivity Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	CA11	Conductivity sensor	Analogue input	1	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
9	FA01_ANLG_ALA_OPEN	Feedwater flow rate Analog input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	FA01	Flowmeter	Analogue input	0	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
10	FA01_ANLG_ALA_SHRT	Feedwater flow rate temperature Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	FA01	Flowmeter	Analogue input	0	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
13	LA11_ANLG_ALA_OPEN	Panel temperature analogue input alarm circuit open	Cables removed from sensor	Ceased production of clean steam	Emergency stop displayed on HMI/ Flashing conductivity readings	Wire removed from sensor	LA11	Level sensor	Analogue input	1	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
						Sensor not calibrated						Sensor transmitting less than 3.8mA			Check HMI for mA reading, lower sensor until lowest point on scale reads 4mA
14	LA11_ANLG_ALA_SHRT	Panel temperature analogue input alarm short circuit	Pinched cable from sensor	Ceased production of clean steam	Emergency stop displayed on HMI/ Flashing conductivity readings	Wire pinched or kinked	LA11	Level sensor	Analogue input	1	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
						Sensor not calibrated						Sensor transmitting more than 20mA			Check HMI for mA reading, (when the generator is empty) lower sensor until lowest point on scale reads 4mA
16	PA01_ANLG_ALA_OPEN	Panel temperature analogue input alarm circuit open	Cables removed from sensor	Ceased production of clean steam	Emergency stop displayed on HMI/ Flashing conductivity readings	Wire removed from sensor	PA01	Pressure sensor	Analogue input	0	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
17	PA01_ANLG_ALA_SHRT	Panel temperature analogue input alarm short circuit	Pinched cable from sensor	Ceased production of clean steam	Emergency stop displayed on HMI/ Flashing conductivity readings	Wire pinched or kinked	PA01	Pressure sensor	Analogue input	0	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
18	PA21_ANLG_ALA_OPEN	Panel temperature analogue input alarm circuit open	Cables removed from sensor	Ceased production of clean steam	Emergency stop displayed on HMI/ Flashing conductivity readings	Wire removed from sensor	PA21	Pressure sensor	Analogue input	2	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
19	PA21_ANLG_ALA_SHRT	Panel temperature analogue input alarm short circuit	Pinched cable from sensor	Ceased production of clean steam	Emergency stop displayed on HMI/ Flashing conductivity readings	Wire pinched or kinked	PA21	Pressure sensor	Analogue input	2	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
20	PA31_ANLG_ALA_OPEN	Supply steam in pressure Analog input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	PA31	Pressure sensor	Analogue input	3	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
21	PA31_ANLG_ALA_SHRT	Supply steam in pressure Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	PA31	Pressure sensor	Analogue input	3	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
22	PRI_BAND_HI_ALARM	Primary band HIGH alarm	-	Emergency stop sequence-Ceased production of clean steam	Emergency stop displayed on HMI	Reduced primary pressure	-	-	-	-	-	Setpoint not achieved			Re-tune system
															Leaking control valve
23	PRI_BAND_LOW_ALARM	Primary band LOW alarm	Control valve failed closed	Emergency stop sequence-Ceased production of clean steam	Emergency stop displayed on HMI	Customer steam supply	-	-	-	-	-	Codensate blockage			Tune PID
												Insufficient customer steam supply/ Quality of inlet steam			Fix Inlet steam supply
24	PRI_CAP_ALARM	Primary control capacity alarm	Valve over 99% open	Target clean steam pressure not achieved	Alarm displayed on HMI	Steam demand exceeds CSG capacity.	-	-	-	-	-	Insufficient capacity			Review IMI to check capacities

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
26	PRI_PRES_LOW	Primary pressure low alarm	Valve 100% open	Emergency stop sequence-Ceased production of clean steam	Emergency stop displayed on HMI	Primary pressure PA31 lower than setpoint for clean steam pressure	PA31	Pressure sensor	-	-	-	Insufficient customer steam supply	Increase supply of inlet steam		
28	SEC_BAND_HI_ALARM	Secondary band HIGH alarm	-	-	Alarm displayed on HMI	Leaking within valve	VA01	Water control valve	Analogue input	0	1	Water control valve stuck open	Inspect water control valve to identify cause		
						PID Settings						Poor PID Settings	Adjust PID settings		
29	SEC_BAND_LOW_ALARM	Secondary band LOW alarm	No noise/ pump not spinning	No feedwater pressure	Water pump failure alarm	Water supply not sufficient	MB01 MD01	Pump	Analogue output Digital input	0	1	-	Check water supply (Pressure and ensure no debris-Check strainers/ Filters)		
						Air lock in water pump						-	Check air bleed		
						Power loss to pump						-	Check power status		
						Pump mechanical/ electrical failure						Pump failure	Refer to pump IMI		
			Valve closed when not instructed	-	Water level low alarm Valve feedback alarm (OPT)	For more information see alarm 60	VB01	Supply water control valve	Analogue output	0	1	For more information see Alarm 60	For more Information see alarm 60		
			Reduced water level on visual boiler sight glass												
			Boiler water being dumped to drain, potential for flash steam	-	Water level low alarm Valve feedback alarm (OPT)	Valve failure	VE11	Drain valve	Digital output	1	1	Visual inspection	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
			Excess Steam coming from drain Water level indicator low Sound from valve									-	Potential reduced CSG capacity More water consumption	-	VE12
									Debris in pipeline	Check strainer screen on water inlet. Check for debris origin.					
											TDS settings too Low	TDS valve stuck open	Visit TDS Blowdown section in IMI for details. Check input water conductivity.		
			Possible reduced pressure on pressure dial	-	-	Inlet water supply	-	-	-	-	-	Inlet water supply failure	Check inlet water supply for any blockages		
30	SEC_CAP_ALARM	Secondary control capacity alarm	Valve over 99% open	Target clean steam pressure not achieved	Alarm on HMI	Steam demand exceeds CSG capacity	-	-	-	-	-	Insufficient capacity	Review IMI to check capacities		

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
31	SEC_LVL_LOW	Secondary side boiler water level low	Level indicator low	Emergency stop sequence-Ceased production of clean steam	Low water level alarm displayed, Emergency stop displayed on HMI	Water level lower than setpoint	-	-	-	-	-				
34	TA01_ANLG_ALA_OPEN	Feedwater temperature Analog input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	TA01	Temperature sensor	Analogue input	0	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
35	TA01_ANLG_ALA_SHRT	Feedwater temperature Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	TA01	Temperature sensor	Analogue input	0	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
36	TA0X_ANLG_ALA_OPEN	Panel temperature analogue input alarm circuit open	Cables removed from sensor	Emergency stop sequence-Ceased production of clean steam	Emergency Stop displayed on HMI/Flashing conductivity readings	Wire removed from sensor	TAX1	Temperature of panel	Analogue input	0	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
37	TA0X_ANLG_ALA_SHRT	Panel temperature analogue input alarm short circuit	Pinched cable from sensor	Emergency stop sequence-Ceased production of clean steam	Emergency Stop displayed on HMI/Flashing conductivity readings	Wire pinched or kinked	TAX1	Temperature of panel	Analogue input	0	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
38	TA0X_HIGH_ALARM	Panel temperature limit alarm		Emergency stop sequence-Ceased production of clean steam	Emergency stop displayed with high panel temperature alarm	High panel temperature	TAX1	Temperature of panel	Analogue Input	X	1	High ambient temperature		Reduce environment temperature	
39	TA11_ANLG_ALA_OPEN	Water in temperature Analog input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	TA11	Temperature sensor	Analogue input	1	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
40	TA11_ANLG_ALA_SHRT	Water in temperature Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	TA11	Temperature sensor	Analogue input	1	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
41	TA21_ANLG_ALA_OPEN	Clean steam temperature Analog input alarm circuit open	Cables removed from sensor	Emergency stop sequence-Ceased production of clean steam	Emergency Stop displayed on HMI/Flashing conductivity readings	Wire removed from sensor	TA21	Temperature sensor	Analogue input	2	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
42	TA21_ANLG_ALA_SHRT	Clean steam temperature Analog input alarm short circuit	Pinched cable from sensor	Emergency stop sequence-Ceased production of clean steam	Emergency Stop displayed on HMI/Flashing conductivity readings	Wire pinched or kinked	TA21	Temperature sensor	Analogue input	2	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
43	TA31_ANLG_ALA_OPEN	Supply steam temperature Analog input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	TA31	Temperature sensor	Analogue input	3	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
44	TA31_ANLG_ALA_SHRT	Supply steam temperature Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	TA31	Temperature sensor	Analogue input	3	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller
45	TA41_ANLG_ALA_OPEN	Supply waste temperature Analog input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	TA41	Temperature sensor	Analogue input	4	1	Operator error			Replace cable
						Sensor failure						Refer to technical documentation			Replace sensor
						BC3250 controller failure						Refer to technical documentation			Replace controller

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
46	TA41_ANLG_ALA_SHRT	Supply waste temperature Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	TA41	Temperature sensor	Analogue input	4	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
47	TA51_ANLG_ALA_OPEN	Condensate out temperature Analog input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	TA51	Temperature sensor	Analogue input	5	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
48	TA51_ANLG_ALA_SHRT	Condensate out temperature Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	TA51	Temperature sensor	Analogue input	5	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
49	TA52_ANLG_ALA_OPEN	Drain temperature analogue input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	TA52	Temperature sensor	Analogue input	5	2	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
50	TA52_ANLG_ALA_SHRT	Drain temperature analogue input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	TA52	Temperature sensor	Analogue input	5	2	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
51	TDS_HI	TDS failure	-	High levels of conductivity	TDS alarm displayed	TDS set point exceeded	VE12	TDS valve	Digital output	1	2	TDS set point exceeded		Take action to reduce TDS, if necessary adjust setpoint Visit TDS blowdown section in IMI for details	
			-			Invalid time duration entry						Input error on HMI			
52	TDS_HYS_FAIL	TDS hysteresis fault	Continuous Blowdown	-	TDS hysteresis alarm displayed	TDS hysteresis setpoint not achieved	VE12	TDS valve	Digital output	1	2	Input error on HMI		Adjust setpoint whilst referring to IMI	
												Partially blocked valve		Inspect blocked valve	
												Restrictions in blowdown		Inspect any blockages in blowdown	

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
56	VA01_ANLG_ALA_OPEN	Water level control valve feedback Analog input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	VA01	Feedwater control valve	Analogue input	0	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
57	VA01_ANLG_ALA_SHRT	Water level control valve feedback Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	VA01	Feedwater control valve	Analogue input	0	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
58	VA31_ANLG_ALA_OPEN	Supply steam in control valve feedback Analog input alarm circuit open	Cables removed from sensor	-	Flashing conductivity readings	Wire removed from sensor	VA31	Plant steam control valve	Analogue input	3	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	
59	VA31_ANLG_ALA_SHRT	Supply steam in control valve feedback Analog input alarm short circuit	Pinched cable from sensor	-	Flashing conductivity readings	Wire pinched or kinked	VA31	Plant steam control valve	Analogue input	3	1	Operator error		Replace cable	
						Sensor failure						Refer to technical documentation		Replace sensor	
						BC3250 controller failure						Refer to technical documentation		Replace controller	

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
60	VB01_FBK	Feedwater control feedback error	Valve not open when instructed.	-	Valve feedback alarm (OPT), Water level failure alarm, Water level high alarm	VA01	Feedwater control valve	Analogue input	0	1	Leaking seat/ plug	Wear of seat	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
											Positioner failure	Debris in pipeline	Check strainer screen on water inlet. Check for debris origin.		
											Positioner calibration faulty	Mismatch between positioner and PLC	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
											Actuator failure	Mismatch between positioner and actual stem indicator position and PLC			
											Mechanically failed shut	Mismatch between positioner and actual stem indicator position and PLC			
											Positioner failure	Mismatch between positioner and actual stem indicator position and PLC			
			Actuator failure	Mismatch between positioner and actual stem indicator position and PLC											
			Valve failure	Gailing of stem											
			Valve closed when ot instructed.	Potential reduced CSG capacity. More water consumption	Water Level Low alarm, Valve feedback alarm (OPT)						Positioner failure	Mismatch between positioner and PLC			
											Actuator failure	Mismatch between positioner and actual stem indicator position and PLC			
											Gailing Valve	Gailing/ Wear of stem			
					Valve feedback alarm (OPT), Water level failure alarm, Water level high alarm						Positioner failure	Mismatch between positioner and PLC			

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action	
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION		
61	VB31_FBK	Steam in control feedback error	Valve not open when instructed.	-	Valve feedback alarm (OPT), Water level failure alarm, Water level high alarm	Leaking seat/ plug	VA01	Feedwater control valve	Analogue input	0	1	Wear of seat			Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
						Positioner failure						Debris in pipeline			Check strainer screen on water inlet. Check for debris origin.	
						Positioner calibration faulty						Mismatch between positioner and PLC			Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
						Actuator failure						Mismatch between positioner and actual stem indicator position and PLC				
						Mechanically failed shut						mismatch between positioner and actual stem indicator position and PLC				
			Valve closed when not instructed	Potential reduced CSG capacity. More water consumption	Water Level Low alarm. Valve feedback alarm (OPT)							Valve failure	Gailing of stem			
												Positioner failure	Mismatch between positioner and PLC			
			Actuator failure	Mismatch between positioner and actual stem indicator position and PLC												
			Gauling valve		Valve feedback alarm (OPT), Water level failure alarm, Water level high alarm	Valve failure						Gailing/ Wear of stem				
						Positioner failure										
63	WATER_PUMP_FAIL	Water pump failure	No Sound from water pump	Reduced output of clean steam	Alarm displayed on HMI	Power loss to pump	MB01 MD01	Pump	Analogue output Digital input	0	1	-			Check power status	
						Water supply not sufficient						Insufficient water head pressure			Check water supply (Ensure no debris, checking strainers and filters along with the pressure)	
						Air lock in water pump						Insufficient bleeding			Check air bleed	
						Pump mechanical/ electrical failure						-			Refer to pump IMI-Suspect pump internal failure	
68	WATER_LVL_HI	Water level high alarm	Water Level exceeds 90%	Inaccurate control of water control valve	Alarm displayed on HMI	Water level exceeds 90%	VA01	Feedwater control valve	Analogue input	0	1	65	WATER_VLV_FAIL	Water control valve failure	Inaccurate control of water control valve	
				Water control valve failed open								65	WATER_VLV_FAIL	Water control valve failure	Water control valve failed open	
69	WATER_LVL_ALARM	Water level failure	TDS Valve opening outside of TDS control	-	Alarm displayed on HMI	Repeated high water level alarm on HMI	-	-	-	-	-	See Alarm 68 for more information			See Alarm 65 for more Information	
70	AIR_PRESS_FAIL	Air supply pressure fail	No valve movement	-	Alarm displayed on HMI	Insufficient Compressed Air	PDX1	Air supply	Digital input	0	1	-			Restore air supply	

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
71	VE31_FAIL_OPEN	Plant isolation valve fail open	-	Start-up/ Shutdown sequence would halt	Alarm displayed on HMI	Leaking seat	VE31	Steam isolation valve	Digital output	3	1	Wear of seat	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
			Actuator Indicator in incorrect Position			Actuator failure	VE31	Steam isolation valve	Digital output	3	1	Debris in pipeline	Check strainer screen on water inlet. Check for debris origin.		
												Insufficient customer air supply	Check customers air supply line		
72	VE31_FAIL_CLOSE	Plant isolation valve fail closed	Indicator displays closed when instructed to open	CSG does not start/ Loss of clean steam supply	Alarm displayed on HMI	Valve does not leave closed position when instructed	VE31	Steam isolation valve	Digital output	3	1	Mismatch between positioner and actual stem indicator position and PLC	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
73	VE31_FAIL_STICK	Plant isolation valve fail stuck	Actuator indicator shows neither on/off	Start-up/ Shutdown sequence would halt	Alarm displayed on HMI	Leaking seat	VE31	Steam isolation valve	Digital output	3	1	Wear of seat	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
						Actuator failure						Debris in pipeline	Check strainer screen on water inlet. Check for debris origin.		
												Insufficient customer air supply	Check customers air supply line		
74	VE31_FAIL_SPEED	Inlet Plant valve fail opening speed	Possible waterhammer in primary side	-	Alarm displayed on HMI	Unrestricted exhaust flow from actuator	VE31	Steam isolation valve	Digital output	3	1	Exhaust restrictor set incorrectly	Reset/ Replace exhaust restrictor		
75	VE21_FAIL_OPEN	Outlet isolation valve fail open	-	Start-up/ Shutdown sequence would halt	Alarm displayed on HMI	Leaking seat	VE21	Steam isolation valve	Digital output	2	1	Wear of seat	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
			Actuator Indicator in incorrect position			Actuator failure						Debris in pipeline	Check strainer screen on water inlet. Check for debris origin.		
												Insufficient customer air supply	Check customers air supply line		
76	VE21_FAIL_CLOSE	Outlet isolation valve fail closed	Indicator displays closed when instructed to open	CSG does not start/ Loss of clean steam supply	Alarm displayed on HMI	Valve does not leave closed position when instructed	VE21	Isolation valve	Digital output	2	1	Mismatch between positioner and actual stem indicator position and PLC	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
77	VE21_FAIL_STICK	Outlet isolation valve fail stuck	Actuator indicator shows neither on/off	Start-up/ Shutdown sequence would halt	Alarm displayed on HMI	Leaking seat	VE21	isolation valve	Digital output	2	1	Wear of seat	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
						Actuator failure						Debris in pipeline	Check strainer screen on water inlet. Check for debris origin.		
													Insufficient customer air supply	Check customers air supply line	
78	VE21_FAIL_SPEED	Outlet isolation valve fail opening speed	Waterhammer	Sudden/ rapid pressure loss Risk of carryover	Alarm displayed on HMI	Unrestricted exhaust flow from actuator	VE21	isolation valve	Digital output	2	1	Exhaust restrictor set incorrectly	Reset/ Replace exhaust restrictor		

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action	
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION		
81	PRI_BAND_HI_ALERT	Primary band high alert	-	High clean stem pressure	Alert displayed on HMI	Failed open control valve							See alarm 71 for more information			See Alarm 71 for more Information
						Leaking control valve							-	Identify leak in control valve		
						Leak in heat exchanger							-	Identify leak in heat exchanger		
						PID settings						Incorrect PID settings	Adjust PID setting if necessary			
82	PRI_BAND_LOW_ALERT	Primary band low alert	Control valve closed for a given amount of time	Low clean steam pressure	Alert displayed on HMI	Valve positioning incorrect	VA31	Steam control valve	Analogue input	3	1		-	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
						PID settings							Incorrect PID settings	Adjust PID setting if necessary		
						Customer supply steam	-	-	-	-	-		-	Fix inlet steam supply		
						Restricted condensate flow							Debris in pipeline	Remove debris from pipeline		
83	PRI_CAP_ALERT	Primary control capacity alert	Valve over 99% open for a given amount of time	-	Alert displayed on HMI	Plant steam	VA31	Plant steam control valve	Analogue input	3	1		Plant steam Insufficient	Fix Plant steam		
						Capacity incorrect							Capacity incorrect	See IMI for correct capacities.		
						Restricted condensate flow	-	-	-	-	-		Debris in pipeline	Inspect pipeline and remove any debris		
84	SEC_BAND_HI_ALERT	Secondary band high alert	-	Possible carryover	Alert displayed on HMI	PID settings							Inspect PID settings	Adjust PID settings if necessary		
						Leaking valve	-	-	-	-	-		-	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
85	SEC_BAND_LOW_ALERT	Secondary band low alert	-	-	Alert displayed on HMI	Positioner failure	-	-	-	-	-		-	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
						PID settings							Inspect PID settings	Adjust PID settings if necessary		
86	SEC_CAP_ALERT	Secondary control capacity alert	-	-	Alert displayed on HMI	Insufficient water supply	-	-	-	-	-		Debris in pipeline	Remove any debris from pipeline.		
87	VE51_FAIL_SPEED	Condensate isolation valve fail opening speed	Waterhammer	Sudden/ rapid pressure loss Risk of carryover	Alarm displayed on HMI	Unrestricted exhaust flow from actuator	VE51	isolation valve	Digital output	2	1		Exhaust restrictor set incorrectly	Reset/ Replace exhaust restrictor		

11.1 Alarms continued on next page

Alarm number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
88	TEMP_LIM	Saturated pressure temperature limit	-	Emergency Stop Sequence- Ceased production of clean steam	Emergency stop displayed on HMI	Clean steam thermistat tripped	TD21	Temperature switch	Digital input	2	1	Clean steam temperature exceeds set limit	Investigate clean steam temperature source		
						Low water level limit exceeded	LD11	Level switch	Digital input	1	1	Clean steam temperature switch failure	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
												Water level below allowanle limit	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
												Water low level switch failure			
89	HMI_SYNC_ALARM	HMI Communications Fault	HMI Unresponsive	Optional: Emergency Stop Sequence- Ceased production of clean steam	HMI connection banner	Communication between PLC and HMI has been lost	-	HMI screen	-	-	-	HMI Failure	Replace HMI		
												Connection fault with ethernet cable	Check ethernet ports for connection and communication lights		
90	ALA_TEST_LEAK_NEG	Integrity test leak alarm	Leak pipe joints	Ceased production of clean steam	Alarm displayed on HMI	Leak in pipe joints	-	-	-	-	-	-	Inspect pipe joints		
			Leak in steam control valve			Leak in steam control valve	VA31	Steam control valve	Anaolgue input	3	1	-	Inspect steam control valve		
			Leaks in Integrity test valves			Leak in isolation valves	-	-	-	-	-	-	Inspect isolation valves		
91	ALA_TEST_POS_MAX	Integrity test count alarm	-	Ceased production of clean steam	Alarm displayed on HMI	Maximum number of integrity tests reached	-	-	-	-	-	Air pressure rises during integrity test requires customer decision before clean steam production can begin	Use on-screen pop-up screen		
93	ESTOP_PB	Emergency stop button pressed	E-stop button locked in	Ceased production of clean steam	Emergency stop displayed on HMI	-	-	-	-	-	-	User operated	Release e-stop button and press reset button		

11.1 Alarms continued on next page

## 7.2 Alerts

Diagnostics provided to guide users to improve performance of the equipment or quality of the process.

Alert number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
1	ALA_PERF_CACL	Heat exchanger scaling alarm	-	Begin to lose flow capacity	More primary steam required	Scale formation on heating element	-	-	-	-	-	-	Poor water quality/water hardness	Remove and clean heating elements Improve water quality	
2	ALA_PERF_LEAK	Supply steam leaking through to clean side alarm	-	-	Over pressure during low flow conditions	Leaking from primary to secondary side	-	-	-	-	-	-	Manufacturing fault Fatigue	Replace heating element Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
7	COND_TEMP_HI	Condensate temperature hot	Temperature exceeds 40 °C/104 °F	-	High condensate temperature alarm	System isolation not complete	TA41	Temperature sensor	Analogue input	4	1	-	Operator error	Close isolation valve VM51	
11	FEED_PRES_HI	Feedwater pressurised	Pressure exceeds 0.1 bar g/ 1.45 psi g	-	Warning displayed Emergency stop	Service sequence	-	-	-	-	-	-	Insufficient isolation during servicing	Work and check isolation valves	
12	FEED_TEMP_HI	Feedwater temperature hot	Temperature exceeds 40 °C/104 °F	-	Warning displayed Emergency stop	Service sequence	-	-	-	-	-	-	Insufficient isolation during servicing	Work and check isolation valves	
25	PRI_PRES_HI	Primary side pressurised	Pressure exceeds 0.1 bar g/ 1.45 psi g	-	Emergency stop displayed on HMI	Service sequence	-	-	-	-	-	-	Incorrectly isolated valves	Check isolation valves	
27	PRI_TEMP_HI	Primary side temperature hot	Temperature exceeds 40 °C/104 °F	-	-	-	-	-	-	-	-	-	-	-	
32	SEC_PRES_HI	Secondary side pressurised	Pressure exceeds 0.1 bar g/ 1.45 psi g	-	Emergency Stop displayed on HMI	Service sequence	-	-	-	-	-	-	Isolation valves in service sequence	Check isolation valves	
33	SEC_TEMP_HI	Clean steam temperature hot	Temperature exceeds 40 °C/104 °F	-	-	Temperature exceeds 40 °C/104 °F	-	-	-	-	-	-	-	-	
62	WASTE_TEMP_HI	Waste steam temperature hot	Temperature exceeds 40 °C/104 °F	Service sequence halted	-	Service sequence	-	-	-	-	-	-	Insufficient isolation during servicing	Work and check isolation valves	
64	WATER_TEMP_HI	Water in temperature hot	Temperature exceeds 40 °C/104 °F	Service sequence halted	Alarm displayed on HMI	Service sequence	-	-	-	-	-	-	Insufficient isolation during servicing	Work and check isolation valves	

11.2 Alerts continued on next page

Alert number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
67	INITIALISE	PLC Start-up from power cycle	-	No Clean Steam Produced/CSG not operational	No display on HMI or partial display	Faulty PLC	-	-	-	-	-	-	PLC failure	Contact SXS engineer	
92	DRAIN_TEMP_HI	Drain temperature hot	Temperature exceeds 40 °C / 104 °F	Service sequence halted	Alarm displayed on HMI	Service sequence	TA52	Temperature sensor	Anaolgue input	5	2	Insufficient isolation during servicing	Work and check isolation valves		
95	PRE_HP_TA11_LOW	Preheater temperature low	Temperature falls below TA21 - 2.5°	Ceased production of clean steam	Alarm displayed on HMI	Preheater pressure too low	TA11 and TA21	Temperature Sensor	Analogue input	1 and 2		Check preheater HE02 for scale and re-set VU33. Alarm could also be triggered due to poor PID tuning.	Reset VU33 and retune PID settings		
96	PRE_HP_TA11_HI	Preheater temperature high	Temperature raises above TA21 + 2.5°	Ceased production of clean steam	Alarm displayed on HMI	Overpressure in the preheater	TA11 and TA21	Temperature Sensor	Analogue input	1 and 2		Mal-adjusted VU33 or primary side overpressure or poor PID tuning	Perform inspection on VU33 and primary steam control valve		
97	PRI_BAND_HI_ALERT	Primary band high alert	-	High clean stem pressure	Alert displayed on HMI	Failed open control valve						See alarm 71 for more information	See Alarm 71 for more Information		
						Leaking control valve						-	Identify leak in control valve		
						Leak in heat exchanger						-	Identify leak in heat exchanger		
						PID settings						Incorrect PID settings	Adjust PID setting if necessary		
98	PRI_BAND_LOW_ALERT	Primary band low alert	Control valve closed for a given amount of time	Low clean steam pressure	Alert displayed on HMI	Valve positioning incorrect	VA31	Steam control valve	Analogue input	3	1	-	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.		
						PID settings						Incorrect PID settings	Adjust PID setting if necessary		
						Customer supply steam	-	-	-	-	-	-	Fix inlet steam supply		
						Restricted condensate flow						Debris in pipeline	Remove debris from pipeline		
99	PRI_CAP_ALERT	Primary control capacity alert	Valve over 99% open for a given amount of time	-	Alert displayed on HMI	Plant steam	VA31	Plant steam control valve	Analogue input	3	1	Plant steam Insufficient	Fix Plant steam		
						Capacity incorrect						Capacity incorrect	See IMI for corrcet capacities.		
						Restricted condensate flow	-	-	-	-	-	Debris in pipeline	Inspect pipeline and remove any debris		

11.2 Alerts continued on next page

Alert number	Alarm PLC tag	Alarm description	Identifier			Fault	Component					Cause			Action
			Physical	Process	System		TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
100	SEC_BAND_HI_ALERT	Secondary band high alert	-	Possible carryover	Alert displayed on HMI	PID settings	-	-	-	-	-	Inspect PID settings			Adjust PID settings if necessary
						Leaking valve						-			Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
101	SEC_BAND_LOW_ALERT	Secondary band low alert	-	-	Alert displayed on HMI	Positioner failure	-	-	-	-	-	-			Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
						PID settings						Inspect PID settings			Adjust PID settings if necessary
102	SEC_CAP_ALERT	Secondary control capacity alert	-	-	Alert displayed on HMI	Insuffiecnt water supply	-	-	-	-	-	Debris in pipeline			Remove any debris from pipeline.

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## **Service**

For technical assistance contact our nearest Office or Agency or contact directly:

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## **Warranty**

Ascertained partial or complete non-compliance with these regulations will result in forfeiture of the related warranty.