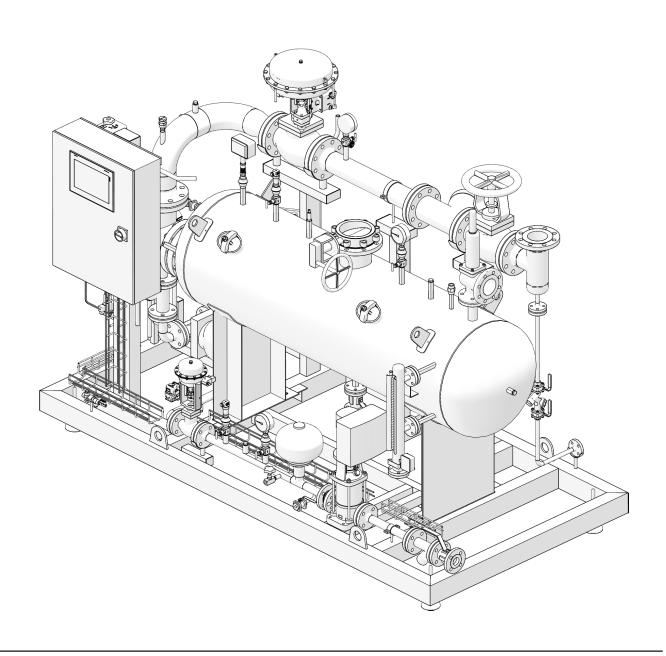


# **CSG-FB** Clean steam generation system for Food & Beverage Installation and Maintenance Instructions



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## 1. Safety information

In addition to putting your personnel at risk of death or serious harm, failure to comply with the instructions, recommendations and guidance set out in this document may jeopardise your warranty rights. Further, use of the product(s) otherwise than in accordance with this document will be undertaken entirely at your own risk. To the fullest extent legally permitted, Spirax Sarco excludes all responsibility and liability for any and all loss or damage caused in the event that the practices and procedures detailed in this document have not been followed.

Safe operation of these products can be guaranteed only if they are properly installed, commissioned and maintained by a qualified person (see Section 1.11) in compliance with the related operating instructions. General installation and safety instructions for pipeline and plant construction and also the proper use of tools and safety equipment must also be complied with.

### **General safety notes**

This manual is intended to cover the installation, start-up and maintenance procedures of the CSG-FB indirect clean steam generator and must be read in conjunction with the installation and maintenance manuals (IM) of the single components of the unit and related additional safety notes.

### Precautions when lifting the unit

The CSG-FB indirect clean steam generator must be lifted from the base depending on the size, adopting a suitable forklift or transpallet for 020 and 050 sizes and using the lifting eye bolts installed on the base frame for 110 and 160 sizes.



Do not lift the CSG-FB indirect clean steam generator by any other part except from the base.

Note: always leave sufficient space around the system for future maintenance operations.

# Caution or Warning

### Warnings

- 1. The unit is designed and constructed to withstand the intensity of work in ordinary use.
- 2. Use of the product for any other purpose, or failure to install the product in compliance with these Installation and Maintenance Instructions, may damage the product and also cause serious injuries to operating personnel.
- 3. Before carrying out any installation and maintenance procedure, always check that all primary steam, condensate and water return lines on the secondary have been isolated.
- 4. Make sure that residual pressure in the system and in pipework has been vented to atmospheric level.
- 5. To avoid the risk of burns, allow parts to cool before carrying out any type of operation.
- 6. Always wear suitable protective clothing before carrying out any installation or maintenance activity.
- 7. This product is intended to be connected into a system that can operate an EC1935 compliant process. To minimise the risk of non-intentionally added substances in the system, it is essential that an appropriate CIP (cleaning in place) cycle is carried out by the end user prior to first use in a food contact application. A list of the materials that could come directly or indirectly into contact with foodstuffs can be found in the Declaration of Compliance available for this product.

### 1.1 Intended use

Referring to the installation and maintenance instructions and the nameplate of the unit and the Technical Specifications, check that the product is suitable for intended use/application.

EMEA - The CSG-FB indirect clean steam generator complies with the requirements of the EU Pressure Equipment Directive/ UK Pressure Equipment (Safety) Regulations and is **( f** marked.

America's - The CSG-FB indirect clean steam generator complies with the requirements of the ASME Pressure vessel code and ASME U Stamp upon request.

Asia Pacific - The CSG-FB indirect clean steam generator complies with the requirements of the EU Pressure Equipment Directive/UK Pressure Equipment (Safety) Regulations Conformance to KGS / MOM and DOSH is available upon request.

- The product has been specifically designed for use on steam and water belonging to Group 2 of the above-mentioned Pressure Equipment Directive.
- ii) Check suitability of material, pressure and temperature and related maximum and minimum values. If the maximum operating limits of the product are lower than those of the system in which it to be inserted, or if malfunction of the product could generate dangerous overpressure or overtemperature, always insert a safety device in the system to prevent exceeding of such limits.
- iii) Determine the correct installation position and direction of flow of fluids.
- iv) The product is not designed to withstand external stresses induced by the system in which it is fitted. The installer is responsible for taking into account such stresses and for adopting adequate precautions to reduce these to a minimum.
- v) Prior to installation, remove protective covers from all connections and and also protective film and packaging elements.

# 1.2 EU Pressure Equipment Directive/UK Pressure Equipment (Safety) Regulations classification

The clean steam generators CSG-FB series are classified as assembly according the EU Pressure Equipment Directive/ UK Pressure Equipment (Safety) Regulations:

Product	Fluid Group	Category
CSG-FB-020	2	Ш
CSG-FB-050	2	Ш
CSG-FB-110	2	IV
CSG-FB-160	2	IV

For the category of bespoke units, refer to the "EC Declaration of Conformity" supplied with the product. Other component parts of the assembly comply with the relevant European Directives, where necessary. Please refer to specific component literature for further details.

### 1.3 Access

Ensure safe access and, if necessary, a safe working platform (suitably guarded) before attempting any work on the product. Arrange suitable lifting gear if required.

### 1.4 Lighting

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Ensure adequate lighting, particularly where detailed or intricate work is required.

### 1.5 Hazardous liquids or gases in the pipeline

Take into account what is currently in the pipeline or what may have been in the pipeline at some previous time. Consider: flammable materials, substances hazardous to health, extreme temperatures.

CSG-FB Clean steam generation system for Food & Beverage

### 1.6 Hazardous environment around the product

Consider: areas with a risk of explosion, lack of oxygen (e.g. tanks, pits), dangerous gases, extreme temperatures, hot surfaces, fire hazards (e.g. during welding), excessive noise, moving machinery.

The place of installation of the assembly must be equipped with the fire-prevention devices required by current regulations.

### 1.7 The system

Consider the effect of the work to be carried out on the entire system. Consider whether the action proposed (e.g. closing of isolating valves, electrical isolation) may put any other part of the system or personnel at risk.

Hazards may include isolation of vents or protective devices or the rendering ineffective of controls or alarms. Ensure isolating valves are opened and closed gradually to avoid shocks to the system.



### 1.8 Pressure systems

Ensure that any pressure is isolated and safely vented to atmospheric pressure.

Consider double isolation (double block and bleed) and locking or labelling of closed valves. Do not assume that the system has depressurised even when the pressure gauge indicates zero.

### 1.9 Temperature

Allow time for temperature to normalise after isolation to avoid the risk of burns and consider whether protective clothing (including safety glasses) is required.

### 1.10 Tools and consumables

Before starting work, make sure you have suitable tools and/or consumables on hand. Use only genuine Spirax Sarco replacement parts.

### 1.11 Protective clothing

Consider whether you and/or others require protective clothing to protect against hazards, such as chemicals, high/low temperatures, radiation, noise, falling objects and danger to eyes and face.

### 1.12 Permits to work

All work must be carried out or supervised by a suitably competent person. Installation and operating personnel should be trained in correct use of the product according to the Installation and Maintenance Instructions. Any formal work permit system adopted must be complied with. Where no such system is applied, a person responsible should be informed of progress of the work and, where necessary, an assistant with primary responsibility for safety should be appointed. Post "warning signs" if necessary.

### 1.13 Handling

Manual handling of large and /or heavy products may involve a risk of injury. Lifting, pushing, pulling, carrying or supporting a load by bodily force may cause injury, particularly to the back. You are advised to assess the risks, taking into account the task, the individual, the load and the working environment and use appropriate handling methods according to the circumstances of the work to be carried out.

Note: if it is necessary to use slings for lifting, it is good practice to fit these around the plate of the base unit to avoid damage to the unit.

### 1.14 Storage

Note: If the Clean Steam Generator cannot be installed and put into operation immediately upon receipt at the jobsite, certain precautions are necessary to prevent deterioration during storage.

Responsibility for integrity of the heat exchangers must be assumed by the user. Spirax Sarco will not be responsible for damage, corrosion or other deterioration of heat exchanger equipment during transit and storage. Good storage practices are important, considering the high costs of repair or replacement, and the possible delays for items which require long lead times for manufacture. The followings suggested practices are provided solely as a convenience to the user, who shall make his own decision on whether to use all or any of them.

- On receipt of the CSG-FB Steam Generation System, inspect for shipping damage to all protective covers. If damage
  is evident, inspect for possible contamination and replace protective covers as required. If damage is extensive, notify
  the carrier immediately and Spirax Sarco.
- If the CSG-FB is not to be placed in immediate service, take precautions to prevent rusting or contamination.
- Store under cover in a heated area, if possible. The ideal storage environment for CSG-FB and accessories is indoors, above grade, in a dry, low humidity atmosphere which is sealed to prevent entry of blowing dust, rain or snow. Maintain temperatures between 20 °C and 50 °C (68 °F and 122 °F) and humidity at 40% relative humidity or lower.

Note: Ambient temperature of the place where the unit will be installed must be above 0 °C (32 °F) and below 40 °C (104 °F).

### 1.15 Freezing

Precautions must be taken to protect products that are not self-draining against frost damage in environments where they may be exposed to temperatures below freezing point.

### 1.16 Disposal

As the product may contain PTFE and Viton, particular precautions must be adopted to avoid potential risks for health caused by decomposition or combustion of such materials. Unless otherwise indicated in the installation and maintenance instructions with regard to the materials of the seals, this product can be recycled and it is considered that no environmental risk exists deriving from disposal thereof provided that suitable precautions are adopted. However, its components can be checked to verify the possibility of safe disposal.

### PTFE:

- This material can be disposed of only using approved systems and never in incinerators.
- PTFE waste to be disposed of must be stocked in separate containers and must never be mixed with other waste.

Please visit the Spirax Sarco product compliance web pages

https://www.spiraxsarco.com/product-compliance

for up to date information on any substances of concern that may be contained within this product. Where no additional information is provided on the Spirax Sarco product compliance web page, this product may be safely recycled and/or disposed providing due care is taken. Always check your local recycling and disposal regulations.

### Viton:

- VITON waste can be sent directly to landfills when permitted and accepted by local and national regulations.
- VITON components may also be incinerated but a scrubber must be used to remove the hydrogen fluoride developed by the product, carrying out this procedure in accordance with local and national regulations.
   The components are insoluble in aquatic media.

### **Electrical:**

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Unless otherwise stated, the electrical components within this product are recyclable and no ecological hazard is anticipated with its disposal providing due care is taken. The product should be recycled in line with local legislation.

### 1.17 Return of products

Customers and stockists are reminded that, under EC Health, Safety and Environment Law, when returning products to Spirax Sarco, they must provide information regarding any hazards and precautions to be taken due to contamination residues or mechanical damage which may represent a risk to health, safety or the environmental. This information must be provided in writing, including Health and Safety datasheets relating to any substances identified as hazardous or potentially hazardous.

CSG-FB Clean steam generation system for Food & Beverage

## 2. General product information

### 2.1 Description

The CSG-FB indirect clean steam generator consists of a complete, safe and functional system package, ready for installation and able to produce up to 200/500/1100/1600 kg/h of clean steam (at normal operating conditions) using industrial steam as a primary energy source.

The CSG-FB series of indirect clean steam generators are designed to produce clean steam for direct injection processes within the food & beverage industry sector, where steam is considered as an ingredient.

The heat exchange is indirect, for which there is no contamination between the primary steam and the 'clean' steam produced.

### Models and applications

	CSG-FB-020 for a nominal production of 200 kg/h*	(441 lbs/hr)
Size	CSG-FB-050 for a nominal production of 500 kg/h*	(1102 lbs/hr)
3126	CSG-FB-110 for a nominal production of 1100 kg/h*	(2425 lbs/hr)
	CSG-FB-160 for a nominal production of 1600 kg/h*	(3527 lbs/hr)

Applications Sterilisation of containers, generic use of clean steam.

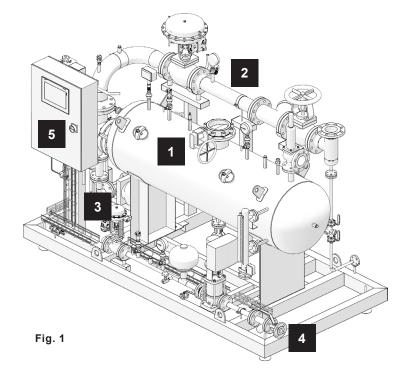
### 2.2 Identification of the product

The product is identified by the nameplate fastened to the frame.

### The CSG-FB unit, (Figure 1), comprises the following main parts:

- 1 Steam generator and instrumentation/accessories, protection and safety devices
- 2 Primary steam control
- 3 Condensate removal
- 4 Feedwater inlet
- 5 Electrical control panel

For a detailed list of equipment and specifications, refer to the P&ID and documentation provided.



### Notes:

- 1. For further information concerning individual components refer to the specific technical documentation of each product.
- 2. Further technical information regarding the CSG-FB indirect clean steam generator can be found in TI-P664-01.

<sup>\*</sup> Nominal steam production at reference operating conditions: primary plant steam at 10 bar g (145 psi g), production at 5 bar g (73 psi g), feedwater at 20 °C (68 °F).

### **Example of nameplate:**

- "CE" marking and Id. of notified body
   Unit PED category
- 2. Unit model
- 3. Product Nomenclature Series
  - Size
  - Configuration
  - Options
- 4. Unit serial No.:

- YY: year
- XXXXXX: identification number (6 or 9 digits)
- = ZZ: unit progressive number
- Year of construction
- 5. Electric and air supply specifications (where required)
- 6. Fluid group (PED), design conditions and circuit hydro test pressure

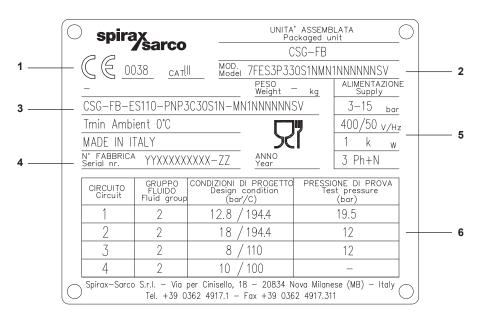


Fig. 2 Note: the pressure values in the nameplate are expressed in 'bar g'.



Note: the pressure values in the nameplate are expressed in 'psi g'.

Fig. 2.1 - Americas' nameplate

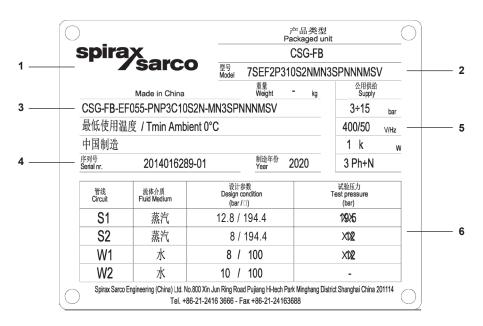


Fig. 2.2 - Asia Pacific nameplate

**2.3 Product nomenclature and selection guide**The product nomenclature is based on the characteristics of the main elements and options, identified as follows:

Basic configuration								
	E	EN						
Parton and	A	ASME						
Design code	G	GB						
	J	JBA						
Shell type	S	Flanged openable-shell and tube, flanged openable without integrated deaerator						
	020	Up to 200 kg/h (441 lbs/hr) (at the reference operating conditions)						
Unit aims	050	Up to 500 kg/h (1102 lbs/hr)						
Unit size	110	Up to 1100 kg/h (2425 lbs/hr)						
	160	Up to 1600 kg/h (3527 lbs/hr)						
Valve actuation tune	PN	Pneumatic (fail-safe)						
Valve actuation type	EL	Electric (fail-safe)						
	P1	ABB AC500 series + 7" display						
Control	P2	Allen-Bradley CompactLogix 1700 series + 7" display						
Control	P3	Siemens S7.1200 series + 7" display						
	P4	Selective Control Panel (with PLC ABB AC500 series + 7" display)						
	C0	None						
	C1	BACnet IP						
	C2	Profinet						
	C3	Modbus TCP/IP						
Communication interface	C4	BACnet MSTP						
	C5	Profibus						
	C6	Modbus RTU						
	C7	BACnet (BTL cert.) IP						
	C8	BACnet (BTL cert.) MSTP						
	0	Base and cabinet made of carbon steel, painted						
	1	Open frame and cabinet made of carbon steel, painted						
	2	Frame w. side panels and cabinet made of carb. steel, painted						
Unit frame/Electrical cabinet	3	Base and cabinet made of stainless steel (304) *						
	4	Open frame and cabinet made of stainless steel (304) *						
	5	Frame with side panels and cabinet made of stainless steel (304) *						
	7	Seismic, Base and cabinet made of carb. steel, painted						

<sup>\*</sup> This option/configuration is not allowed with P4 control (Selective Control Panel)

Product nomenclature and selection guide continues on next page

### 2.3 Product nomenclature and selection guide (continued)

Basic configuration				
Control Panel location	S	Side		
	1	Steam generator body only		
In avalation	2	Steam generator and hot piping		
Insulation	3	Insulation to EnEV specification		
	0	Not insulated		
	N	None (only plates with anchor holes are provided)		
Handling wheels and feet	F	Adjustable feet		
	W	Pivoting wheels, lockable, with feet		
Plant steam inlet shut-off valve	М	Manual stop valve		
Plant Steam inlet Shut-off Valve	AE	Automatic electric isolation valve*		
Plant steam line transing	N	None		
Plant steam line trapping	Т	Plant steam line trapping station		
TDS control ovetem	1	Timed TDS blowdown		
TDS control system	2	TDS control with external probe (discontinuous metering) *		
Sampling cooler	N	None		
Sampling cooler	S	Sample-cooler and sampling valve		
Feedwater pressurisation system	N	None (water P > clean steam P + 0,5 bar g)		
reedwater pressurisation system	Р	Pump with VFD *		
Independent downstream plant	N	None		
protection	Т	Temperature limiter *		
Feedwater pre-heating	N	None		
reedwater pre-neating	PR	Feedwater pre-heating by heat recovery from primary condensate		
	N	None		
Intelligent diagnostics	<u>I1</u>	System diagnostics *		
intelligent diagnostics	13	Integrity test *		
	14	System diagnostics + Integrity test *		
	N	None		
Clean steam outlet shut-off valve	М	Manual stop valve		
	AE	Automatic electric isolation valve*		

<sup>\*</sup> This option/configuration is not allowed with P4 control (Selective Control Panel)

Product nomenclature and selection guide continues on next page

### 2.3 Product nomenclature and selection guide

Basic configuration						
	S	EU PED test and CE marking of the assembly				
	U	ASME U stamp				
	М	MOM compliance				
Test and certifications	K	KGS compliance				
rest and certifications	D	DOSH compliance				
	GC	GB standard in Chinese language				
	GE	GB standard in English language				
	SF	None (as assembly)				
Level indicator	V	Viscorol (Magnetic Level Indicator)				

**Product nomenclature example** CSG-FB E S 020-PN P3 C1-1 S 2 F-AE T-2 S P T N I1-AE S V

Not all configurations are available in every country. Please contact your local Spirax Sarco representative for more details.

### 2.4 Design conditions

Duimanu aida	Design pressure		12.8 bar g	(187 psi g)	
Primary side	Design temperature		194.4 °C	(382 °F)	
	Design pressure  Design temperature		8 bar g	(116 psi g)	
Secondary side			194.4 °C	(382 °F)	The complete condition of the design of the
	Safety valve set pressure		7 bar g	(101.5 psi g)	supplied units are reported on the P&ID.
	Design pressure		8 bar g	(116 psi g)	
Feedwater	Design	without pump	110 °C	(220 °F)	
	temperature	with pump	110 C	(230 °F)	

### 2.5 Operating limits

	Without pump	With pump			
Production	Clean saturated steam, up to 6 bar g/165.0 °C (Clean saturated steam, up to 97 psi g/206 °F)				
Primary side	Plant steam, up to 12 bar g/191.7 °C (Plant steam, up to 174 psi g/345 °F)				
	P min. ≥ P clean steam + 0.5 bar g (P min. ≥ P clean steam + 7.2 psi g)	Minimum Supply Pressure (see below)			
Feedwater	P max 8 bar g/T max 110 °C (P max 116 psi g/T max 230 °F)	P max 8 bar g/T max 100 °C (P max 116 psi g/T max 212 °F)			

Minimum pressure of the feedwater at the inlet flange of the units equipped with pump, to avoid cavitation (NPSHR) = P' min. + dP dP: pressure drop along the water feed pipework, at maximum flow-rate.

P' min. depending on the water temperature:

<b>T</b>	°C	≤ 85	90	95	100	
1	( °F)	(185)	(194)	(203)	(212)	- (*\ Under water bood
Di min	bar g	0*	0.05	0.20	0.35	· (*) Under water head
P' min.	(psi g)	(0)	(0.72)	(2.90)	(5.07)	-

Minimum ambient temperature: 0 °C (32 °F). Maximum ambient temperature: 40 °C (104 °F)

Unit designed for indoor installation, protect from freezing.

To ensure the correct operation of the clean steam generator, the inlet feed water should have the following characteristics. An excess on these values can compromise the lifetime, maintenance and efficiency of the steam generator.

pH  $5.5 \div 7.5$  (at 20 °C) Hardness  $\leq 0.02$  mmol/l

(5.5 ÷ 7.5 (at 68 °F))

**Chloride** Please refer to table below **Conductivity**  $\leq 20 \mu \text{S/cm}$ 

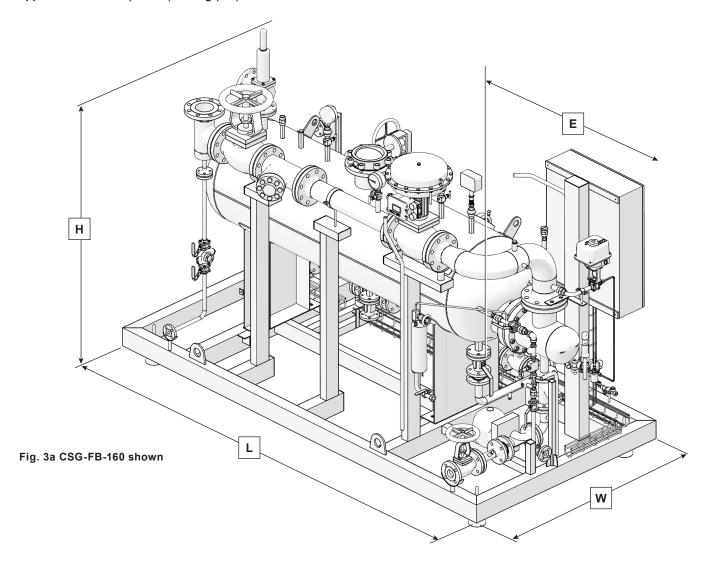
Chlorides concentration limit in inlet feed water							
Blowdown set Inlet feed water pH							
	pH = 5,5	pH = 6,5	pH = 7,5				
5%	≤ 0,5 mg/l	≤ 1 mg/l	≤ 3 mg/l				
10%	≤ 1 mg/l	≤ 2 mg/l	≤ 6 mg/l				

<sup>\*</sup> All the other characteristics and values of feed water are up to end user of the plant.

In addition to the above, for monitored TDS blowdown, a maintained concentration below a maximum of 100uS/cm is required during operation.

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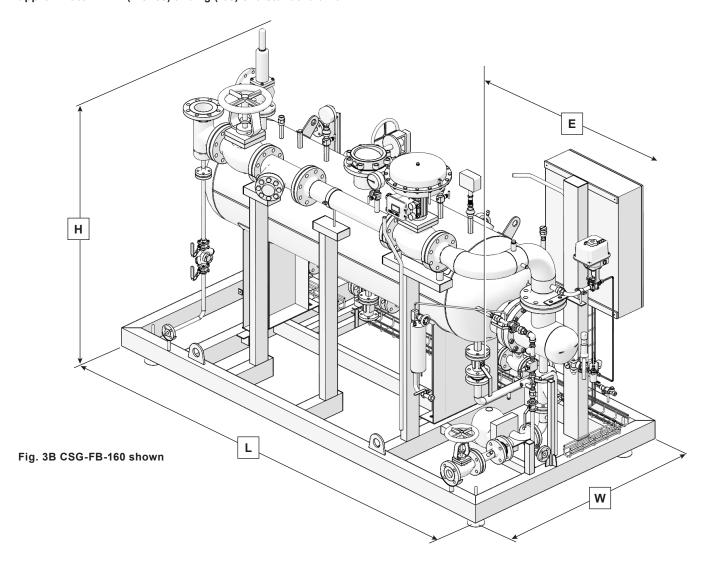
2.6 Dimensions and weights approximate in mm (inches) and kg (lbs) of a standard unit



			imensions m (inches)	Weights kg (lbs)			
	L Length	W Width	H Height	E Clearance for tube bundle extraction	Empty	In operation	Maximum
CSG-FB 020	2000	850	1840	1250	550	650	800
	(79)	(33)	(72)	(49)	(1213)	(1433)	(1764)
CSG-FB 050	2350	850	1840	1300	850	1050	1250
	(93)	(33)	(72)	(51)	(1874)	(2315)	(2756)
CSG-FB 110	2450	1450	2060	1600	1100	1450	1700
	(96)	(57)	(81)	(63)	(2425)	(3197)	(3748)
CSG-FB 160	2950	1450	2060	2000	1550	2050	2450
	(116)	(57)	(81)	(78)	(3417)	(4519)	(5401)

For detailed dimensions of the unit, size and position of the connections, clearance for the tube bundle extraction, weights and other constructive information, refer to the specific general arrangement drawing of the product.

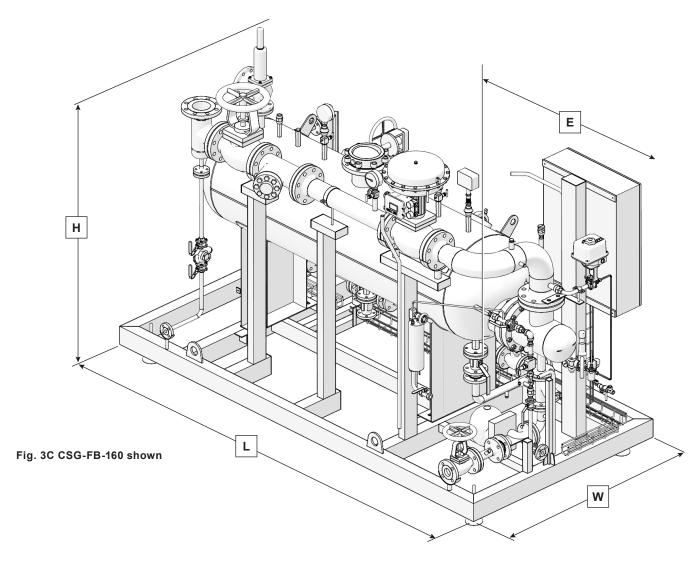
# 2.7 Dimensions and weights with pre-heater approximate in mm (inches) and kg (lbs) of a standard unit



		_	imensions m (inches)	Weights kg (lbs)			
	L Length	W Width	H Height	E Clearance for tube bundle extraction	Empty	In operation	Maximum
CSG-FB 020	2000	850	1840	1250	600	670	850
	(79)	(33)	(72)	(49)	(1323)	(1477)	(1874)
CSG-FB 050	2350	850	1840	1300	870	1070	1270
	(93)	(33)	(72)	(51)	(1918)	(2359)	(2799)
CSG-FB 110	2450	1450	2060	1600	1100	1450	1700
	(96)	(57)	(81)	(63)	(2425)	(3197)	(3748)
CSG-FB 160	2950	1450	2060	2000	1550	2050	2450
	(116)	(57)	(81)	(78)	(3417)	(4519)	(5401)

For detailed dimensions of the unit, size and position of the connections, clearance for the tube bundle extraction, weights and other constructive information, refer to the specific general arrangement drawing of the product.

# 2.8 Dimensions and weights of the units with EnEV option - insulation 100 mm approximate in mm (inches) and kg (lbs)



			mensions m (inches)	Weights kg (lbs)			
	L Length	W Width	H Height	E Clearance for tube bundle extraction	Empty	In operation	Maximum
CSG-FB 020	2100	950	1950	1250	700	800	950
	(83)	(37)	(77)	(49)	(1543)	(1764)	(2094)
CSG-FB 050	2500	1100	2000	1300	1000	1200	1400
	(98)	(43)	(79)	(51)	(2205)	(2646)	(3086)
CSG-FB 110	2550	1450	2250	1600	1300	1600	1850
	(100)	(57)	(89)	(63)	(2866)	(3527)	(4079)
CSG-FB 160	3100	1500	2250	2000	1650	2200	2550
	(122)	(59)	(89)	(79)	(3638)	(4850)	(5622)

### 3. Installation

### 3.1 Installation site

The correct installation of the CSG is required to ensure the safety of the package and to realise the full performance (clean steam flowrate, pressure, dryness). Therefore, it's important to consider the entire installation (see section 3.4 - Process pipework and vents).

The CSG-FB unit is designed for installation indoors with a minimum ambient temperature of 0 °C (32 °F). Installation outdoors is permitted provided that the unit is suitably protected against adverse weather conditions and freezing.

The unit is not suitable for installation in potentially hazardous zones classified as ATEX. Specific solutions can be provided on request.

### 3.2 Handling

020/050 sizes: The CSG-FB unit must be lifted from the base using suitable forklift or transpallet.

Do not use any eyebolts of equipment on board the unit.

If fitted with wheels for handling (option), the unit must be moved in safe conditions and then secured in position

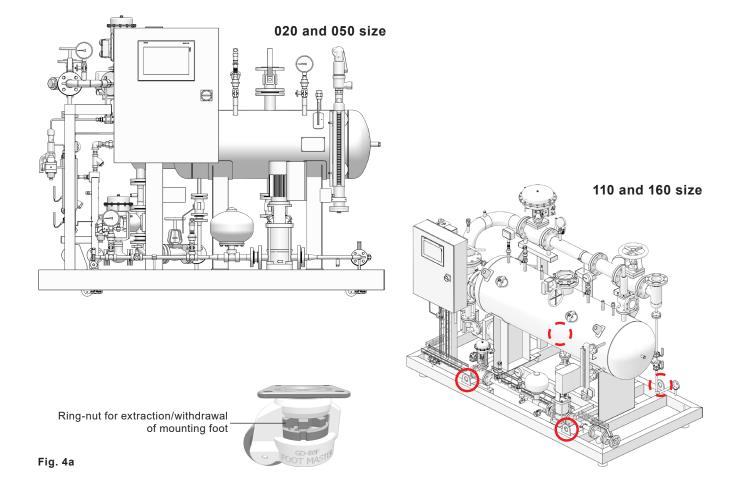
using the integrated mounting feet.

110/160 sizes: The CSG-FB unit must be lifted from the lifting eyebolts mounted on the base of the unit.



Do not lift the unit by other parts or in any manner other than as indicated above.

During lifting, take into account the high centre of gravity of the unit and adopt all the necessary precautions to avoid accidental tipping over of the unit.



### 3.3 Positioning and fastening

The unit must be positioned on a completely flat, horizontal surface able to support its entire weight at full load. A level surface is important as the water level is used in the control system. For access to the unit, provide at least one metre of clearance around, and 0.5 m (1.64 ft) above. A space for tube bundle removal has to be considered.

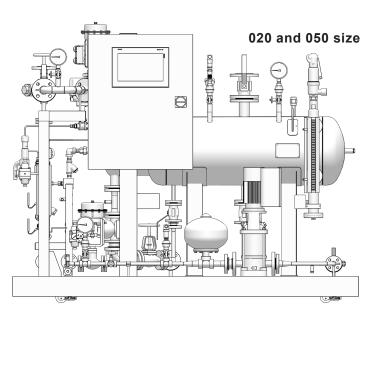
### 3.4 Process pipework and vents

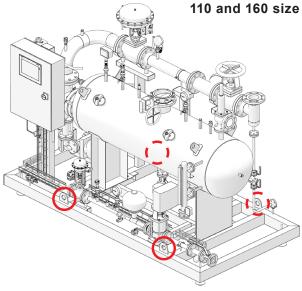
Each unit is provided complete with drawings indicating the position and specifications of connections to be made according to configuration and options ordered.

The main connections of the unit are as follows:

UNI-EN 1092-1 PN16/25/40 connection flanges ASME/ANSI B16.5 connection flanges

For other pipework, according to options installed, refer to the dimensional (or G.A.) drawing of the unit provided.





Ring-nut for extraction/withdrawal of mounting foot

Fig. 4b

### Connections

		Metric					Imp	erial	
		020	050	110	160	020	050	110	160
A	Plant steam inlet connection	DN32 PN16	DN50 PN16	DN80 PN16	DN100 PN16	1¼" ANSI 150	2" ANSI 150	3" ANSI 150	4" ANSI 150
С	Clean steam outlet connection	DN50 PN40	DN80 PN40	DN125 PN16	DN150 PN16	2" ANSI 300	3" ANSI 300	5" ANSI 300	6" ANSI 300
D	Feedwater inlet connection	DN15 PN40	DN20 PN40	DN25 PN40	DN32 PN40	½" ANSI 300	<sup>3</sup> ⁄ <sub>4</sub> " ANSI 300	1" ANSI 300	1¼" ANSI 300
E	Safety valve discharge	1" G-f	DN50 PN16	DN80 PN16	DN80 PN16	1" NPT	1¼" NPT*	3" NPT	3" NPT
G	Plant steam condensate drain connection	DN15 PN40	DN15 PN40	DN15 PN40	DN15 PN40	½" ANSI 150	½" ANSI 150	½" ANSI 150	½" ANSI 150
					Options				

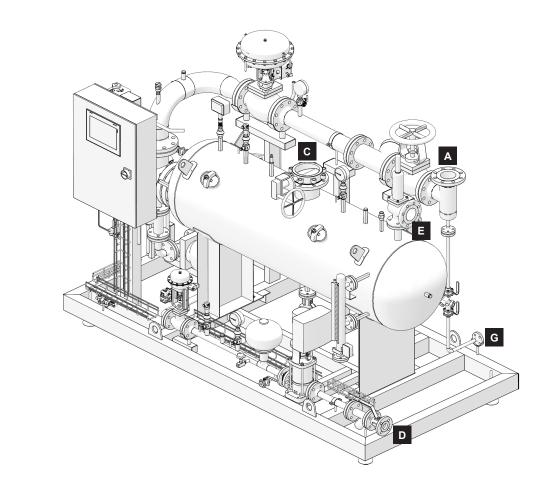


Fig. 5

### Connections continued on next page

### Connections (continued)

	•	Metric			Imperial				
	•	020	050	110	160	020	050	110	160
В	Condensate outlet connection	DN25 PN40	DN25 PN40	DN40 PN40	DN40 PN40	1" ANSI 300	1" ANSI 300	1½" ANSI 300	1½" ANSI 300
F	Drain connection	DN25 PN40	DN25 PN40	DN25 PN40	DN25 PN40	1" ANSI 300	<sup>3</sup> ⁄ <sub>4</sub> " ANSI 300	1" ANSI 300	1" ANSI 300
н	TDS Blowdown connection	DN15 PN40	DN15 PN40	DN15 PN40	DN15 PN40	½" ANSI 150	½" ANSI 150	½" ANSI 150	½" ANSI 150
1	Sampling system (cooling water in/out - sample out)	½" BSP - 6 mm	½" BSP	½" BSP	½" BSP	½" BSP			
					Options				

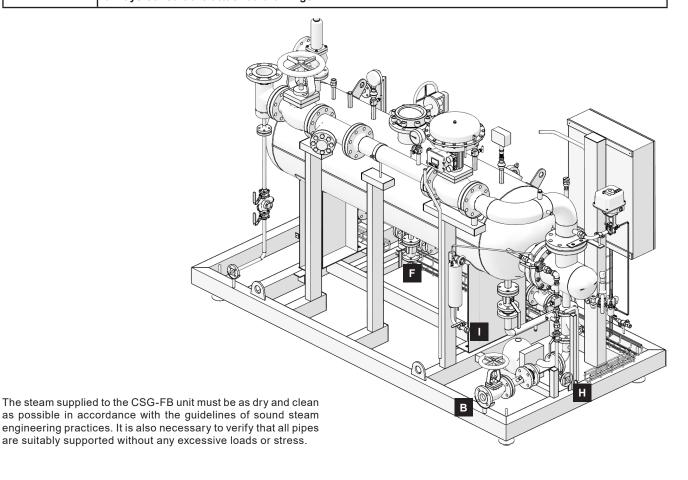


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Before making any connection, check that all pipework is clean and free of foreign material or scale that may adversely affect functioning and/or the performance of the unit.

The steam supplied must always be maintained within design operating pressure and temperature limits. The unit shall not work above the design pressures and temperatures indicated on the name plate on the package.

The drawings provided in this manual are for guidance purposes only. For connections of the unit, always consult the attached drawings.



### 3.4.1 Feedwater inlet

The first step of the installation procedure consists in connecting the unit to the cold feedwater line. The manual isolating valve on the feedwater control line of the unit must remain closed until installation has been completed. The precise position of the feedwater inlet connections, the pipe diameter and size of the attachment flange can be deduced from the drawings provided with the unit.

The feedwater system must be able to supply the correct volume of water to the package whilst meeting the design criteria (see 2.5 Operating limits - temperature, supply pressure, feedwater quality).

#### 3.4.2 Clean steam outlet

The next step in the installation procedure is to connect the clean steam outlet of the generator to the clean steam distribution network of the plant. The precise position of the clean steam outlet, the pipe diameter and size of the attachment flange can be deduced from the drawings provided with the unit. A manual isolating valve (if option is not selected) should be installed downstream of the unit on the clean steam line to permit isolation of the generator. This valve must remain closed until installation has been completed.

Note: In the case of units installed in parallel with another generator(s) (common clean steam distribution line), a check valve must be installed on the steam outlet of each generator.

### 3.4.3 Primary energy source (industrial steam)

Connect the inlet of the primary fluid of the unit to the technological steam distribution network of the plant. The manual (if fitted) isolating valve installed on the primary fluid control line must be closed and remain closed during installation. The precise position of the primary fluid connection, the pipe diameter and size of the attachment flange can be deduced from the drawings provided with the unit. If there is a risk of overpressure to the package, it is good practice for the customer to install a safety relief valve upstream of the package. This may impact the supply pressure that can be supplied to the package and therefore may also have an impact on the clean

If the plant steam supply pressure drops this will impact on the clean steam performance (pressure/dryness/flowrate).



Potential risk of injury and/or fatality

### 3.4.4 Condensate removal

steam generator's performance (kg/h).

Transfer of heat from the primary steam to the produced clean steam generates condensate. The condensate removal from the unit must therefore be connected to the condensate return line of the plant. The manual isolating valve installed on the condensate removal line of the unit must be closed and remain closed during installation. The precise position of the condensate removal connection and size of the attachment flange can be deduced from the drawings provided with the unit.

The condensate trap on the system has been sized considering the upstream pressure. The condensate system (pipework, condensate tank and pumps) downstream of this trap should be designed and sized independently, with consideration given to the downstream pressure and the amount of flash steam that may be produced from the clean steam generator. See TI-GM-11 Condensate Pipe Sizing for more information.

### 3.4.5 Piping the pressure relief valve to vent and drain

As required by current regulations, CSG-FB unit generators are equipped with a pressure relief valve to protect against the risk of overpressure. Venting of the pressure relief valve (steam) shall be directed towards a safe area to avoid injuries or damage. In most applications, the pressure safety valves should be vented to atmosphere (generally through the roof). The piping used in the vent system shall be of adequate size to handle the capacity of the pressure safety valve. The vent piping system shall be suitably drained to prevent formation of condensate inside this. **The vent pipe of the pressure relief valve shall not be intercepted in any way or even partially obstructed.** For further information and prescriptions regarding connection of the vent piping of the pressure safety valve, refer to the related use and maintenance manual. Venting of the pressure relief valve shall comply with current legislation. The purchaser/installer is responsible for such conformity.

### 3.4.6 Drainage of the generator

The CSG-FB steam generators are equipped with a drain/bottom blowdown line with manual valve installed on the lower part of the vessel. The blowdown from this valve is at the same pressure and temperature of the generated steam and can cause severe injury or death if not properly piped. In accordance with local regulations or standards, it is recommended that the blowdown lines be connected to a blowdown vessel or condensate cooler before being discharged to drain.

The precise position of the drainage of the generator connection and also pipe diameter and size of the attachment flange can be taken from the drawings supplied with the unit.

The drains of the generator cannot be placed back in the circuit return condensate or feedwater.

### 3.4.7 Other blowdown, venting, drainage facilities (where required)

The CSG-FB can be equipped with optional systems for blowdown, drainage and venting, such as for example a TDS control system, primary steam drainage line. In accordance with current legislation, blowdown from the TDS control system should be connected to a blowdown vessel or condensate cooler before being discharged to drain. TDS blowdown shall not be connected to the condensate return line. Primary steam blowdown can be connected to the condensate return line of the plant.

Any purge/drain should not be recovered reintegrating the line/water storage tank of feedwater.

The sample cooler option is strongly recommended, especially when the timed TDS option is selected, to assist calibration of the blowdown conductivity.

### 3.4.8 Commissioning infrastructure

It is useful to be able to vent to atmosphere during commissioning as this helps to set PID settings and to prove the package performance. If possible, include a vent to atmosphere to facilitate this. A valve on this line is useful to simulate process demands.

### 3.4.9 Cleanliness

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This product is intended to be connected into a system that can operate an EC1935 compliant process.

Take care to not introduce any contaminants during installation. When making connections to the clean steam side, keep covers on the connections until the connection is ready to be made. During installation, use only products that meet EC1935 requirements, for example gaskets with EC1935 compliance. A list of the materials that could come directly or indirectly into contact with foodstuffs can be found in the Declaration of Compliance available for this product.

### 3.5 Connection of the power supply

For voltage connections, consult the wiring diagram provided for the unit.



Possible injury or death

Before connecting the power supply, check that the main power switch and system start selector are off (0 position).

Where indicated in the wiring diagram, single phase or 3 phase power supplies are to be connected directly to the main isolation switch. Earth points are provided and must always be connected. Power supplies and earth connections must pass through the appropriate number of cable glands to maintain the IP rating for the electrical panel.

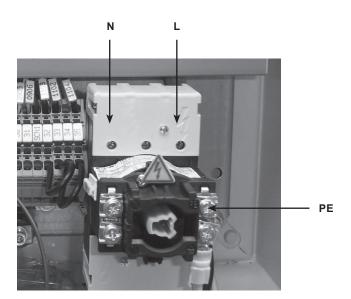


Fig. 6
Version with single-phase power supply

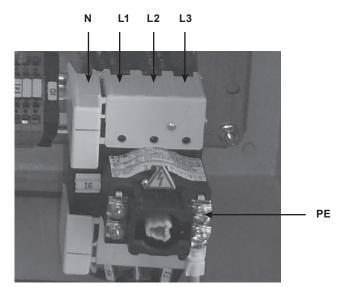


Fig. 7
Version with three-phase + N power supply

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All electrical connections must be made by qualified electricians.

The user is responsible for the suitability of electrical connections outside the unit and for their conformity with current legislation.

Before drilling holes in the cabinet of the control panel to connect the power cables and any interface with an external system, open the door very carefully and check that there are no obstacles inside the cabinet. Ensure that there is no contact between electrical cables inside the panel with drilling residues or with metal.



Signal cables must not be laid together with power cables outside the unit to avoid disturbances and interference during operation. Failure to comply may cause also irreparable damage to the equipment.

The user must install a device between the power supply and control panel able to cut off the power if necessary. It is important to check compatibility of the mains supply with that required by the control panel, verifying correspondence with voltage and frequency data indicated on the nameplate.

Unused wires in conduit must be grounded at both ends to avoid a possible shock hazard caused by induced voltages.

The user is responsible for power connections outside the unit and their compliance with current legislation.

### 3.6 Connection of air supply (where necessary)

If pneumatic actuators or integrity test options are selected, the compressed air must be as dry and clean as possible in accordance with the guidelines of sound engineering practice.

Connect the compressed air supply (minimum 5 bar g-maximum 7 bar g (72.5 psi g-101.5 psi g)) to the pressure regulators fitted on the valves (CV1 and CV2).

So, before starting, adjust the downstream pressure reducers at least 1 bar g above the spring range of pneumatic actuators (if any):

Actuator spring ranges	Primary steam control valve CV1 with electro-pneumatic positioner (smart positioner as option)	Feedwater control valve CV2 with I/P converter (smart positioner as option)
020	2 – 4 bar g (29-58 psi g)	0.4 – 1.2 bar g (5.8-17.4 psi g)
050	1 – 2 bar g (14.5-29 psi g)	0.4 – 1.2 bar g (5.8-17.4 psi g)
110	2 – 4 bar g (29-58 psi g)	1 – 2 bar g (14.5-29 psi g)
160	2.5 – 3.5 bar g (36.2-50.7 psi g)	1 – 2 bar g (14.5-29 psi g)

### 3.7 Electrical specifications

For detailed electrical information, consult the wiring diagram supplied with the unit.

Туре	Rated power	Suggested supply protection
Single Phase 1 x 90-132 V AC or 1 x 180-264 V AC (no pump)	0.5 kW	8A, C Curve MCB
3 Phase, 200-230 Vac with pump	5 kW	20A, C Curve MCB
3 Phase, 380-460 Vac with pump	5 kW	16A, C Curve MCB

<sup>\*</sup> Note: A single leg is taken from the three phase supply to power the PSU, ensure the single leg will have a voltage in the range required for single phase.

### 3.8 Digital inputs/outputs (on all versions)

For wiring, consult wiring diagram provided with the unit.

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The control system for the CSG-FB can provide signals to the customer to enable monitoring of the processes. This is facilitated by the use of industrial communications. The communications protocols are included in the nomenclature and are listed below.

## 4. Commissioning

For correct commissioning, we recommend the service and support of a Spirax Sarco engineer. Please contact your local Spirax Sarco representative for more details.

### 4.1 Pre-commissioning inspection (initial start-up)

- Most of the new installations during the construction of pipelines and the installation of the system, may inadvertently collect dirt
  particles inside the pipes. It is essential to carefully remove any residual impurities and dirt in them before starting the commissioning.
  Upon receipt of CSG-FB begin the SAT check (Site Acceptance Test) by completing 6.1.1 Document Review.
- Check that all the manual isolating valves (on primary stream, on condensate blowdown, on clean steam intake and on feedwater)
  are closed
- Clean the filters upstream of the regulation valves.
- Check that the bottom drain valve VM11 (or VE11) of the unit is closed.
- Make sure that the unit power supply is disconnected.
- Check that primary steam and feedwater design conditions do not exceed the rated values of the unit.
- Check that the design conditions of the downstream system, clean steam side, are not lower than the rated data of the unit or in
  any case not lower than the calibration pressure of the safety valve installed on the unit, secondary side.
- Check that the feedwater line is properly pressurised and has been vented.
- Check that the supply steam (primary) line is properly pressurised and has been drained/ vented.
- Check that the clean steam line has been drained/vented.
- Check that the air supply line, if any, complies with system requirements.
- Check that the power supply complies with the system requirements.
- Make a double check to verify that all connections to steam, condensate and water lines have been made correctly.
- Check that the bolts of the flanged attachments are correctly torqued.
- Check that all the electrical connections outside the unit, are verifying compliance with the wiring diagram (see wiring diagram supplied with the unit).
- Check the air supply of the filters/reducers of the valves (actuated pneumatically where established) and that it complies with the system requirements.
- Check that the base has been properly electrically grounded.
- Cut the cable ties on the safety valve, remove and store the attached documentation.
- Remove the viscorol float from the bag, reinsert the float with the arrow pointing upwards.
- Check safety valve has been plumbed to a safe location, and that pipes are of a suitable size.
- Perform a walk-the-plant to ensure the wider installation is safe.
- Check for sufficient insulation on steam pipes around the control panel and any wiring.
- Using the P&ID, ensure all components are present.
- Check the details of all the sensors.
- Check all subsystems to the package are installed correctly, eg condensate cooler.
- Continue the SAT test by completing up to and including 6.1.5 Pneumatic component check.

### 4.1.2 Cleaning cycles

The clean steam generator is supplied after a pickling and passivation cycle., however, during the construction of pipelines and the installation of the system may inadvertently collect dirt particles inside the pipes. To account for this, there are two cleaning cycles to be completed as part of the commissioning process. The first cleaning cycle will flush the feedwater line and the generator, and a second purge cycle is performed once the system is at operating pressure.

The first cycle is performed by partially filling the generator, isolating the feedwater supply and then opening the bottom drain to fully drain the generator. See 4.2 On-site commissioning procedure for when to perform this cleaning cycle.

The second cleaning cycle:

Before the first use a purge cycle must be performed. This takes place after a CIP (cleaning in place) or other procedure that is performed by following the process in the below table that shows the time each cycle should last for in order to sufficiently flush the CSG. The point at which to perform the purge cycle is given in the commissioning procedure.

Clean steam pressure (bar g)	No. of 30s open, 30s off intervals (full minutes for test)
1	16
2	11
3	9
4	8

Clean steam pressure (bar g)	No. of 30s open, 30s off intervals (full minutes for test)
5	7
6	6
7	6
8	6

### 4.2 On-site commissioning procedure

The CSG-FB control system has an integrated commissioning sequence designed to guide the user through configuring, starting and tuning the systems PID settings from factory.

It is assumed at this point that all required pipe connections and services have been connected. To begin the commissioning sequence, all connected services must be available and all critical alarms must be cleared.

Have the package nomenclature ready as it is needed during commissioning.

- 1. Using the Bolt torque table, ensure that all fittings and flanges are tightened to their correct settings. Ideally, these should be identified with a marking compound to allow checks before proceeding.
- 2. Close all manually operated steam isolation valves and provide steam to that part in the line. If automated isolation valves have been fitted, open all manually operated steam isolation valves.
- Open all manually operated condensate valves from the customer's connection.
   Note: To reduce water hammer during start-up, it can be useful to crack the condensate valve open slightly to allow the system to warm up before opening the valve fully once the package is up to operating temperature.
- 4. Open any manually operated valves downstream of the TDS valve VE12.
- 5. If Integrity test option is fitted, open any manually operated valves connected the Drain Valve VE11.
- 6. Open any manually operated valves upstream water inlet to the CSG-FB.
  - Bleed the pump and prime the feedwater line.
  - Open any ports for gauges and sensors.
  - Open the clean steam manual isolation valve (if fitted).
- 7. Ensure that all trip switches inside the control panel are set to on.
- 8. Switch the control panel isolator to the On position.
- 9. Check that all pneumatic positioners (if fitted) are set to Auto.

- 10. Power on the control panel and wait for the Spirax Sarco welcome page.
  - Continue the SAT test up to and including 6.1.13 Generator Manual Operation.
  - Perform the first cleaning cycle (see 4.1.2 cleaning cycles).
  - Open the plant steam manual isolation valve (if fitted) to let steam into the package.
- 11. Tap the welcome page to view the Home Screen.
- 12. At the home screen, select the Main Menu button.



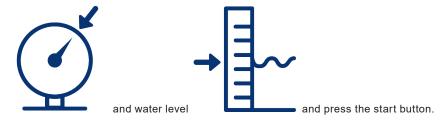
13. Select the System Menu button.



14. Select the Service screen button.



- 15. Select "First Start Up" button and confirm.
- 16. Input the correct clean steam pressure set point



- 17. Follow the on screen instructions.
- **18.** If, as part of an integrity test, a leak is detected, repair the leak and repeat the test. It may be necessary to turn off the control panel to fix the leak. Repeat steps 17-21 to restart the commissioning sequence and re-check for any leaks.

19. At the PID Tuning screen, the control system can now simulate high loads and low loads to allow the PID settings to be changed to ensure correct running of the unit.



20. At least one high demand simulation and one low demand simulation is required to complete the commissioning sequence. Select the green tick button to complete.



The commissioning sequence is now complete and the unit will continue to run at the selected pressure and level set points.

The default settings loaded during the commissioning sequence should be sufficient for the majority of simple applications. However, process settings and alarm settings should always be adjusted to suit individual applications and installations.

Once the commissioning sequence has been completed, the settings should be saved from the Factory settings screen. These settings can be updated or loaded from the Factory settings screen on the HMI.



- 21. Once the CSG-FB is running at the operating pressure, perform the second cleaning cycle (see 4.1.2 cleaning cycles), and then the CAH01 Blowdown Controller can be calibrated. Refer to IM-P693-39 BCR3150 Blowdown Controller to do this. Note If the operating pressure of the CSG-FB is changed, the CAH01 Blowdown Controller will need to be recalibrated. See 4.6 Changing the operating pressure.
- 22. Complete the remaining SAT tests and the Test Summary Sheet.

### 4.3 Start-up procedure

Once the commissioning procedure is complete, the CSG-FB can now be started from the Home screen.

- If automated plant steam isolation valves have been selected, open any manually controlled valves upstream.
- Follow any on screen instructions.



### 4.4 Shut-down procedure

Once the unit has begun its start-up sequence, the start button is replaced with the Stop button.

Follow any on screen instructions.



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### 4.5 Ambient conditions

When the unit is out of service in a low ambient temperature space, with a risk of freezing, it is necessary to completely empty the unit.



Ice inside the generator and inside primary steam line/condensate and feedwater can severely damage the equipment

**4.6 Changing the operating pressure**When a change is required to the CSG\_FB operating pressure, some of the equipment will need recalibration. Ensure the following points are met every time there is a change to the operating pressure:

- Set pressure in Babystar expansion vessel to 0.7x pump pressure (only when pump is specified).
- Calibrate TDS blowdown controller (when conductivity probe is spec'd) .
- Tune PID settings for the operating conditions.
- May require different valve trims in feedwater control valve and plant steam control valve.

## 5. System controls

The CSG-FB control system has a range of controls and functions to ensure the safe and stable running of the unit. Not all functions are available depending upon the configuration of the CSG-FB, these are denoted by the \* symbol.

### 5.1 Runtime controls

Runtime controls affect the response of the CSG-FB and are only active whist the unit is 'running'. During standby, these controls are not enabled.

### 5.1.1 Automated start-up

The Automated start-up sequence controls the safe start-up of the CSG-FB from cold and empty condition all the way through to fully pressurised and correct water level.

Detailed instructions can be provided by a Spirax Sarco engineer, however a simplified sequence can be found below.

- Raise water level to low level.
- Open automated clean steam outlet isolation valve (if fitted).
- Open automated plant steam isolation valve (if fitted).
- Control valve opens a small amount to warm up unit.
- 105 °C (221 °F) clean steam temperature is measured.
- 0.5 bar g (7.25 psi g) clean steam pressure is measured.
- Ramp up pressure to set point.
- Raise water level to set point.
- Check for pressure and water at correct set point.
- End sequence and start Run sequence.

### 5.1.2 Automated recovery

If the CSG-FB is still hot or pressurised from previous use, the control system can restart the unit without having to gently warm up the heating coils.

Detailed instructions can be provided by a Spirax Sarco engineer, however a simplified sequence can be found below.

- Maintain current water level or raise to low level.
- Open automated clean steam outlet isolation valve (if fitted).
- Open automated plant steam isolation valve (if fitted).
- Ramp up pressure to set point.
- Raise water level to set point.

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- Check for pressure and water at correct set point.
- End sequence and start Run sequence.





CSG-FB Clean steam generation system for Food & Beverage

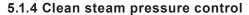
### 5.1.3 Automated sequenced shut-down

The automated shut-down sequence ensures that he unit is in an optimal condition such that, when it begins the start-up sequence, the time taken is to reach running conditions is as little as possible.

This includes reducing the water level to the 'low level' so that less time is required to reach saturation temperature.

Detailed instructions can be provided by a Spirax Sarco engineer, however a simplified sequence can be found below.

- Reduce water level to low level or wait for timer limit.
- Ramp down steam set point to 0.
- Close automated plant steam inlet (if fitted).
- Wait for water temperature to drop below 110 °C (212 °F).
- Stop water control.
- Close outlet isolation valve (if fitted).
- End sequence and start standby.



Control of the clean steam pressure is maintained by use of a PID control loop program in the PLC using pressure sensor PA21 as the process variable. See section 7 for component map. The steam PID set point (set during commission sequence) can be adjusted from the Process Settings screen. The steam PID control value is sent directly to the steam control valve VB31.

The Steam PID set point value can be overridden by the PLC during several processes. These include Ramp up/down (see section 5.1.7), Forward controls (see section 5.1.8) and PID tuning (see section 5.3).



### 5.1.5 Water level control

Control of the water level within the clean steam side of the CSG-FB in maintained by use of a PID control loop program in the PLC using level sensor LA11 as the process variable. The water level PID set point (set during commissioning sequence) can be adjusted from the Process settings screen. The water level PID control value is sent directly to the water control valve VB01. If a pre-heater is fitted, the water control valve will maintain a minimum opening (5% default valve) to reduce thermal cycle fatigue on the pre-heater.

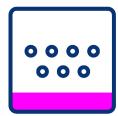
The water level PID set point can be overridden by the PLC during several processes.

These include Forward controls (see section 5.1.8), Automated start-up (see section 5.1.1), Automated recovery (see section 5.1.2) and Automated shutdown (see section 5.1.3).



### 5.1.6 TDS control

Some TDS controls are only available with the correct options fitted when ordering the CSG-FB. The following options may be available on screen if fitted. All automated TDS controls are only enabled when in Run mode. All settings are accessible from the TDS Settings screen in the Process settings area.



### 5.1.6.1 Interval control

Available across all TDS control options, Interval control relies on a 2 timers to open and close the TDS valve VE12.

If either of the conductivity sensor options are fitted, a limit value for the TDS is still be set on screen and used for process diagnostics.



### 5.1.6.2 Pulsed hysteresis control\*

With the inclusion of a conductivity sensor CA11 fitted in the TDS blowdown line of the CSG-FB, the conductivity of the water can only be monitored when the TDS valve VE12 is open. The interval and duration of these checks must be set to allow a reliable TDS value to be read.

If, whilst the TDS valve is open, the conductivity reading is above the TDS setpoint, the valve will remain open until the conductivity reading reduces by the Hysteresis set-point.

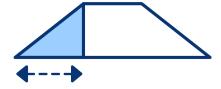


### 5.1.7 Ramp up/down

At the initiation of the Clean Steam pressure control, the set-point sent to the PID program is always ramped up from 0 to the desired set-point over a period of time. This ramp up is used in the automated start-up and recovery sequences.

Similarly, if the clean steam pressure set-point is altered whilst the CSG-FB is running, the ramp sequence will alter the set-point over the ramp period.

The ramp up and ramp down time period can be altered on the Process Settings screen.



### 5.1.8 Forward controls

Forward controls are used to anticipate extra-ordinary running conditions in order to ensure safe and reliable running of the CSG-FB. There are two conditions that are monitored and two respective controls processes designed to handle them. The Forward Controls settings page can be found in the Process Settings area.



#### 5.1.8.1 Rapid high demand

If a significant and prolonged period of high demand results in a drop of Clean Steam pressure PA21, then the water level set-point is temporarily raised. This is designed to anticipate the rapid level loss due to flash boiling of the water in the CSG-FB due to the drop in pressure

The values used for the Clean Steam pressure drop, duration of the drop, the raise in water level set-point and the duration of the set-point raise can all be set from the Forward Controls settings screen.



### 5.1.8.2 Rapid low demand

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If a rapid spike in Clean Steam pressure PA21 is detected, then the set-point used for the Clean Steam pressure is temporarily lowered. This is designed to reduce the amount of energy in the CSG-FB and reduce the risk of over-pressurisation.

The values used for the Clean Steam pressure raise rate, reduction of the Clean Steam pressure set-point and duration of the set-point raise can all be set from the Forward Controls settings screen.



### 5.1.9 Water pump\*

If the integrated booster pump is fitted, CSG-FB can independently control water pressure fed directly to the Clean Steam side. The control signal sent to the pump is a target pressure to which the pump drives to. The target pressure is calculated as the pressure currently detected Clean Steam Pressure PA21 + Pump offset. The pump can also be set to maintain a continuous pressure rather than an offset. This is option is only available at commissioning by a Spirax Sarco Engineer. The Pump offset or fixed setpoint can be set from the Water PID settings page in the Process Settings area.



As the pump has its own control system, no bypass loop is required to prevent over-pressurisation.

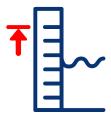
### 5.1.10 Ball Valve anti-binding\*

The ball valve anti-binding sequence ensures that ball valves which are subjected to prolonged periods in the open position do not stick. To do this, any ball valves fitted to the CSG-FB that are in the open position at midnight each day are given a closed signal for 1 second. After this 1 second closed signal, valves will return to their open position.



### 5.1.11 Water level overflow\*

If a pre-heater is fitted and the water level reaches the overflow level setpoint whilst in Run mode, the TDS valve (VE12) will open. This will override any TDS control as stated in 5.1.6. Once the water level has dropped below the overflow level setpoint, the TDS valve (VE12) will revert to normal TDS control.



### 5.1.12 Level Cutoff\*

If a pre-heat is fitted and the water level reaches the level cutoff setpoint whilst in Run mode, the water level control valve (VB01) will try to move to 0%, overriding the normal PID control signal for the minimum opening value. When the level drops below the level cutoff setpoint, normal PID will resume and the minimum opening position will return to the previous setting.

The level cutoff setpoint can be the same position or greater than the water level overflow setpoint, but cannot be lower.

### 5.2 Manual controls

All manual controls are accessible from the Override screen in the System area. All fitted automated valves fitted to the CSG-FB are able to be controlled manually whist the system is in Standby mode. Whilst the system is in any other mode, manual controls are not available.

On/off valves can be opened or closed using their respective toggle button on the screen. Control valves can be moved to a specified position once the valve has been enabled. Disabling the valve will return the valve to closed position. Whist manual controls are enabled, the CSG-FB will not begin Automated Start-up or Recovery. All manual controls must be reset before continuing. A warning is displayed if the clean steam temperature inside the CSG-FB has exceeded 100 °C (212 °F). This is to prevent accidental discharge of hot water or steam



### 5.3 PID Tuning

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PID Tuning is a series of processes that allow the system to simulate loads rises and drops on a running CSG-FB. In order to do this, the PID Tuning sequence reduces the current Clean Steam Pressure set-point by 1 bar g (14.5 psi g).

Once the CSG-FB is running at the PID Tuning set-point, the user can either instantaneously; increase the set-point by 0.5 bar g (7.3 psi g) to simulate high demand, or decrease the set-point by 0.5 bar g (7.3 psi g) to simulate low demand. With either of the simulations, the PID controller will now react accordingly allowing the user to set P, I and D values for both water control and steam control to ensure safe and stable running.



The PID Tuning screen is accessible as part of the commissioning sequence, from standby by selecting the 'PID Tuning Sequence' button, and whilst running by selecting 'Running PID Tuning'.

If PID tuning is initiated from standby or commissioning, the CSG-FB will start normally using the Automated Start-up sequence as described in section 4.2.

If Running PID tuning is selected, the system will reduce the clean steam pressure set-point by 1 bar g (14.5 psi g) and the PID tuning screen will be visible.

If a system has been oversized and the valve is operating at a fraction of the opening percentage, changing the trim of the control valve may help to improve the stability of system.

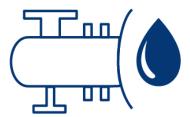
### 5.4 Optional functions

All functions in this section are part of the optional features packs and will not be available without the correct configuration.

#### 5.4.1 Integrity test\*

The integrity test option includes all the necessary valves and measurement equipment to fully isolate the inlet steam side of the CSG-FB from the Steam Control valve VB31 to the Condensate Isolation valve VE51 and perform a pneumatic pressure decay test. This test, when selected will be conducted at the beginning of the next Automated Start-up sequence.

At the end of a failed Integrity Test, the user will be prompted to either re-test, stop the start-up sequence or ignore the test and continue the Automated Start-up. Successful test will not provide any feedback and continue with the Automated Start-up sequence.



An Integrity test will always be performed at the First Start-up as part of the commissioning sequence. This test cannot be ignored. The Integrity test can only be re-started or stop the Automated Start-up sequence entirely.

#### 5.4.2 Service sequence\*

In order to facilitate the safe and easy maintenance of the CSG-FB, a guided service sequence is available to give a servicing engineer the ability to verify valve operation and clean the heating elements.

Whilst the service sequence is in operation, the CSG-FB cannot go into run mode or begin Automated Start-up.

The Service Sequence initialisation is located in the Service screen in the System area. Operators are instructed to manually isolate all external connections to and from the CSG-FB. This includes plant steam, drain, water, condensate and clean steam lines.



In order to ensure that components are safe to operate independently, a series of temperature and pressure sensors are located throughout the CSG-FB. If a temperature above 25 °C (77 °F) or pressure of 0.1 bar g (1.45 psi g) is detected at any point, all controls are automatically set to a safe position and the service sequence is halted.

Prior to and during the 'Cleaning' phase, the screen will indicate a safe (green), not safe (red) indicator next to each sensor monitored around the CSG-FB to allow the engineer to identify if it is safe to remove components on the unit. At this stage, if the control panel is powered down, the service sequence is retained within the memory of the controller and will return to the same point when power is returned to the panel. This ensures that the Automated Start-up sequence cannot be initiated if components are missing from the CSG-FB.

### 5.4.3 Performance monitoring\*

Performance monitoring is a series of sampling, calculation and comparison algorithms that map the performance of the CSG-FB over the full range of operation flow ranges. The flow ranges for each model of the CSG-FB are preloaded into the program and are automatically loaded during the commissioning sequence. With a performance map, the performance of the CSG-FB can be monitored for leaks in or scaling on the heating elements.



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The sampling period is limited to a maximum of 10 samples over the flow range or 100 hours of running. After this period the CSG-FB is assumed to no longer be operating under best conditions. Without a minimum of 3 samples, the calculation and comparison algorithms will not operate. Once sufficient data has been collected and the calculation algorithm has been allowed to run, the comparison algorithm can now compare the current run conditions with the ideal model created by the sampling algorithm.

The Performance Ratio Fault Tolerance value is a percentage difference when comparing the mapped value to the current sampled value. Sample exceeding the positive tolerance value are experiencing a drop in performance (typically due to scale build up), while samples dropping below the negative tolerance value are experiencing abnormal increase in energy transfer (typically due to a leak from the plant steam directly into the clean steam). Respective alarms are shown in the alarm screens when tolerances are exceeded. Settings, live readouts and mapped data from the Performance Monitoring algorithms can be found on the Performance Data area of the HMI.

**HINT:** Key to the accuracy of the Performance Monitoring is the accuracy of the sample data. Specifically ensuring that the measured water flow is as steady as possible. To facilitate this, a series of data filters are available to ensure that flow readings are kept free from anomalous spikes and drops.

CSG-FB Clean steam generation system for Food & Beverage

### 5.5 Emergency stop

The emergency stop program constantly monitors a set of diagnostic systems and will prevent the running of the CSG-FB if any of these diagnostics triggers and alarm. The emergency stop can only reset and allow the running of the system when the cause of the alarm is cleared. In addition to the cleared alarms, the Reset pushbutton must also be pressed to clear the Emergency Stop.



When the emergency stop is triggered, the status of the CSG-FB is changed directly to 'Emergency Stop', overriding any previous run status. Additionally, all automated isolation valves are reset, control valves are closed and the water pump (if fitted) is disabled. The diagnostics systems monitored vary depending upon the current run status. For any run status other than Running (i.e. Automated start-up, restart, sequenced shutdown, integrity test and standby) the systems are listed below. See section 6 for more details on individual diagnostics.

- Emergency stop push button
- Major Instrument failure
- Steam control valve failure
- Water control valve failure
- Water pump failure\*
- Process limit switches
- Air pressure failure\*
- Water supply failure.\*
- Electric valve condition alarm

When the CSG-FB is in Running mode, the following alarms are monitored:

- = Emergency stop push button
- Major Instrument failure
- Steam control valve failure
- Water control valve failure
- Water pump failure\*
- Process limit switches
- Air pressure failure\*
- Water level low limit\*
- Electric valve condition alarm
- Supply pressure failure\*
- Water level control failure
- Water supply failure\*
- Water level high limit
- Optional E-stops

## 6. Diagnostics

Not all diagnostics are available depending upon the configuration of the CSG-FB, these are denoted by the\* symbol.

### 6.1 Control bands

Clean Steam Pressure Control and Water Level Control are both monitored by separate Control Bands, however both control bands operate the same way.

Control Bands monitor their respective process value and compare to the set-point. Upper and lower bands are defined by percentage value from the set-point. If the process value exceeds either the high or low band tolerances a timer is started. If the timer exceeds the Band Alert time a Control Band Alert is issued to the Alarms screen.



If the process value continues to exceed the band tolerances and the timer continues past the Band Alarm time, then a Control Band Alarm is issued to the Alarms screen. If the process value returns to within the band tolerances, the timer is reset.

Control Bands only monitor in Run mode and not in the PID Tuning sequence. Alarms and Alerts reset when the process value returns to within the upper and lower bands. When water level high band alarm is triggered and if a pre-heater is fitted, the water control valve minimum opening is set to 0% to eliminate the possibility of over filling the CSG-FB.

**Note:** Control Band alarms are used by other diagnostic systems. Correct setup at commissioning is critical to robust controls, accurate diagnostics and reduction of nuisance alarms.

## 6.2 Control capacity

The Control capacity diagnostic monitors both the control value from the PID program and the Control band high alarm for the respective process. This provides engineers with a tool to identify if the capacity of either of the control system is at it's limit and thus impacting performance of the CSG-FB.

Clean steam pressure control and Water level control are both monitored by separate Control Capacity diagnostics, however both operate the same way.

If the control valve is fully open for a period of time and the Control band high alarm is active, then the Control Capacity alarm is triggered. If the control valve is fully open for a period of time and the Control Band high alarm is not active, the Control capacity alert is triggered.

Alarms and Alerts reset when the control valve closes from being fully open.



## 6.3 Water Level Failure

The Water Level Failure diagnostic monitors the High Water Level Control system (see section 5.1.11). If the High Water Level cycle is triggered a number of times within a certain time period, the Water Level Failure alarm is triggered.

The number of repeated triggers and timer period are editable on the HMI.

The alarm is only reset when the Reset pushbutton is pressed.

### 6.4 High water limit

The High Water limit diagnostic monitors the Level sensor LA11 to stop the CSG-FB over filling. When the water level sensor reads the measurable limit, the High Water Level alarm is triggered.

The alarm is reset when the water level reduces below the measurable limit.

When high water limit is triggered and if a pre-heater is fitted, the water control valve minimum opening is set to 0% to eliminate the possibility of filling the CSG-FB.



## 6.5 Panel temperature limit

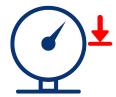
The panel temperature of the CSG-FB is monitored by a PT100 temperature sensor located inside cable trunking of the electrical panel TAX1. If the temperature exceeds the maximum ambient operating temperature of 55 °C (131 °F), the Panel Temperature Alarm is triggered.

The alarm is reset when the measured temperature reduces below 50 °C (122 °F).

### 6.6 High pressure limit

Each CSG-FB is fitted with a mechanical pressure switch PD21 set to the maximum operating pressure for the unit. This switch is set by the manufacturer prior to dispatch. This pressure switch triggers the Process limit switch alarm.

The alarm is reset when the clean steam pressure is low enough for the mechanical pressure switch to reset.



#### 6.7 Low water level limit\*

The Low water level limit diagnostic prevents the exposure of the heating elements.

If the level sensor LA11 gives a reading of less than 40% the Low water level limit alarm is triggered.

The alarm is reset by the water level raising enough to be above 40% on the level sensor.



## 6.8 Water pump fault\*

The optional integrated water pump MB01 provides an simple diagnostic feedback signal MD01 which is only triggered when there is a fault with the pump or the control of the pump pressure.

The alarm is cleared when the fault is cleared from the water pump.



## 6.9 Water supply failure\*

The Water supply failure diagnostic monitors the water supply pressure PA01 and only activated when the integrated water pump is not fitted.

When active, the water supply pressure is compared to the control pressure that would be sent to the integrated pump (see section 5.1.9). If the supply pressure is below the control signal, the Water supply failure alarm is triggered.

The alarm is cleared when the supply pressure exceeds the control signal that is generated for the water pump.

### 6.10 Pneumatic supply failure\*

When fitted, the Pneumatic supply pressure switch PDX1 is used to monitor the compressed air supply to the CSG-FB. If the air supply pressure drops below the minimum required pressure, the alarm is triggered.

The alarm is cleared when the pneumatic supply pressure increases above the minimum required pressure.

## 6.11 Supply steam failure\*

The Supply steam failure diagnostic monitors the control signal sent to the Steam control valve VB31 and the Steam inlet pressure PA13 whilst in the 'Running' state. When the control signal requests the control valve to be fully open for longer than 60 seconds and the Steam Inlet pressure is below the current clean steam oressure set-point. The alarm is triggered.

The alarm is cleared once the pressure rises above the clean steam pressure set-point.

#### 6.12 TDS limit\*

When fitted with a conductivity sensor CA11, the TDS limit diagnostic monitors the conductivity and will trigger an alarm if the TDS set-point is exceeded for a period of time.

The alarm is cleared when the measured conductivity is reduced below the TDS set-point.



## 6.13 TDS hysteresis fault\*

The TDS hysteresis fault diagnostic closely monitors the TDS control system, specifically the Hysteresis controls. When hysteresis is engaged and the TDS valve is opened, a timer is started. If the timer expires before the measured conductivity reduces by the hysteresis setting, the alarm is triggered.

The alarm is reset when the measured conductivity reduces by the hysteresis setting.



## 6.14 Trap alarms\*

The Trap alarm diagnostics can be split into two conditions based around the two alarms. The alarm for either condition is reset by pressing the Reset pushbutton.



#### 6.14.1 Trap fail open

During normal running conditions, the trap of the CSG-FB will be constantly discharging condensate. As such a failed open trap would not be easily detectable. However, at low flow conditions, it is easier to identify the trap discharging excessive amount of condensate and eventually live steam.



When a pre-heater is not fitted and the Trap Failed Open alarm is triggered when the control valve is only open a small amount, and the condensate temperature sensor TA51 and the drain temperature sensor TA52 are similar temperatures.

The maximum valve temperature and maximum difference between temperature sensors can be set on the HMI.

### 6.14.2 Trap fail closed

When a pre-heater is not fitted and the Trap failed closed alarm monitors the drain temperature sensor TA52. Based on the below calculation, the minimum operating temperature of the drain condensate after the trap can be determined. If, whilst in Running status, the condensate temperature drops below this temperature, the Trap Failed Closed alarm will activate.



Note: there are many causes of blockages in the condensate line that can cause the measured drain temperature to drop below minimum operating condensate temperature. If after investigation, the trap is operating properly, there may be another cause for the backup of condensate, including external to the CSG-FB.

## 6.14.3 Pre-heater

### 6.14.3.1 Trap fail open

The trap fail open alarm is triggered with a pre-heater when both the water control valve and the steam control valve are only open a small amount and when the condensate temperature sensor TA51 and then Plant steam temperature sensor TA31 are similar temperatures. The maximum values for the valve positions and temperature differences can be set on the HMI.

#### 6.14.3.2 Trap fail closed

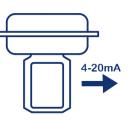
The trap fail closed alarm is triggered with a pre-heater when the water control valve is open above a minimum value and there is a different between the water inlet temperature sensor TA01 and the water outlet temperature sensor TA11. The minimum valve position and the minimum temperature difference can be set on the HMI.

#### 6.15 Valve feedback\*

The Steam control valve VB31 and the Water level control valve VB01 are both monitored by separate Valve Feedback diagnostics, however both operate the same way. The valve feedback diagnostics are disabled during the Service Sequence (see section 5.4.2).

The valve feedback diagnostic monitors the control values sent to the control valve compares this to the valve feedback signal for their respective control valves (Steam control valve feedback VA31, Water level control valve feedback VA01). A positive and negative tolerance from the control signal is calculated. If the valve feedback is not within that tolerance, a timer is started. If the timer expires, the alarm is triggered.

The alarm is reset when the control valve feedback reads within the position tolerance.



## 6.16 Isolation valve feedback\*

The Steam inlet VE31, Clean steam outlet VE01, Bottom drain valve VE11 are independently monitored by separate Isolation valve feedback diagnostics.

#### 6.16.1 Fail closed

If the valve does not rotate enough to come off the valve closed limit switch within a time limit when commanded, the valve failed closed alarm is triggered.

The alarm is reset when the valve rotates enough to turn off the valve closed limit switch.

### 6.16.2 Fail open

If the valve does not rotate enough to come off the valve open limit switch within a time limit when commanded, the valve failed open alarm is triggered.

The alarm is reset when the valve rotates enough to turn off the valve open limit switch.



#### 6.16.3 Partial open failure

If, when commanded, the valve takes too long to transition from closed to open, or from open to closed, the Partial open failure alarm is triggered.

The alarm is reset of the valve completes the rotation and triggers the correct limit switch.

#### 6.16.4 Open speed

If, when commanded, the valve opens too quickly, the Open speed alarm is triggered. The alarm is reset when the correct valve opening speed is achieved.

#### 6.17 Analogue input diagnostic

The Analogue input diagnostic is able to detect if an analogue input signal has been electrically disconnected from the system (sensor failure, wires disconnected, etc), or if the signal wires have been directly connected (wires pinched or damaged). The Open circuit alarm and Short circuit alarms are triggered respectively.

The alarms are reset when a correct input signal is detected.

### 6.18 Pre-heater thermal cycle

All pre-heaters fitted to a CSG-FB are supplied with a temperature sensor on the condensate outlet pipe (TA51). This is the area of the pre-heater that is subject to the greatest thermal fluctuations.

The CSG-OS monitors the condensate temperature for rapid swings.

The diagnostic feature is able to differentiate between positive and negative temperature cycles and records each. Once the counter has reached the maximum limit, the pre-heater should be replaced as per section B.6 to avoid any leaks due to thermal stress cracks.

Using the run time since installation, the diagnostics is also able to predict the earliest point where stress cracking is expected to occur.

This counter can be reset when the pre-heater is replaced.



## 6.19 Optional E-stop triggers

All alarms, not already included in the Emergency stop sequence (see section 5.5), have the option of triggering an emergency stop. When enabled, the alarms must be cleared before the emergency stop sequence can be reset.

#### 6.20 Umbrella alarms

Umbrella alarms are not directly displayed on the Alarms page of the HMI. These alarms are collective names given to alarms used in the Emergency stop sequence (see section 5.5)

#### 6.20.1 Major instrument fault

The Major instrument fault covers the analogue input alarms for all sensors that are essential the safe running of the CSG-FB. If any of these analogue input alarms are triggered, the Emergency Stop sequence will be started and will not be able to be reset until the alarms are cleared.

The following Analogue Input Diagnostic alarms are included in the Major Instrument Fault umbrella alarms:

- Clean steam temperature TA21
- Control panel temperature TAX1
- Water pressure PA01‡
- Clean steam pressure PA21
- Water level LA11

#### 6.20.2 Steam control valve failure

The Steam control valve failure covers all diagnostics related to the Steam control valve VB31. If any of the alarms associated with these diagnostics are triggered, the Emergency stop sequence will be started and will not be able to be reset until the alarms are cleared.

The following diagnostic alarms are included in the Steam control valve failure umbrella alarm:

- Valve Feedback analogue input diagnostics VA31
- Valve Feedback diagnostic VA31

### 6.20.3 Water level control valve failure

The Water level control valve failure covers all diagnostics related to the Water level control valve (VB01). If any of the alarms associated with these diagnostics are triggered, the Emergency stop sequence will be started and will not be able to be reset until the alarms are cleared.

The following diagnostic alarms are included in the Water level control valve failure umbrella alarm:

- Valve feedback analogue input diagnostics VA01
- Valve feedback diagnostic VA01



# 7. Troubleshooting

Alarm	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
1	ALA_PERF_CACL	Heat exchanger scaling alarm	-	Begin to lose flow capacity	More primary steam required	Scale formation on heating element
2	ALA_PERF_LEAK	Supply steam leaking through to clean side alarm	-	-	Over pressure during low flow conditions	Leaking from primary to secondary side
			Leak pipe joints			Leak in pipe joints
3	ALA_TEST_LEAK	Cold leak test alarm	Leak in steam control valve	Ceased production of clean steam	Emergency stop displayed	Leak in steam control valve
			Leaks in Integrity test valves			Leak in isolation valves
4	ALARM_SERV_ STOP	Temperature or pressure alarm in service sequence	Hot pipes		Temperature or pressure detected	System isolation not complete
5	CA11_ANLG_ALA_	Water conductivity	Cables removed		Flashing	Wire removed from sensor  Sensor failure
ð	OPEN	Analog input alarm circuit open	from sensor	-	conductivity readings	BC3250 controller failure

	С	omponent				Cause		Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
-	-	-	-	-	Poor water quality/water hardness			Remove and clean heating elements
								Improve water quality
						Manufacturin	g fault	Replace heating element
-	-	-	-	-		Fatigue	3	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
-	-	-	-	-		-		Inspect pipe joints
VA31	Steam control valve	Anaolgue input	3	1		-		Inspect steam control valve
-	-	-	-	-		-		Inspect isolation valves
					7	COND_ TEMP_HI	Condensate temperature hot	
					11	FEED_PRES_ HI	Feedwater pressurised	
					12	FEED_TEMP_ HI	Feedwater temperature hot	
					25	PRI_PRES_ HI	Primary side pressurised	
-	-	-	-	-	27	PRI_TEMP_HI	Primary side temperature hot	Inspect isolation valves
					32	SEC_PRES_ HI	Secondary side pressurised	
					33	SEC_TEMP_ HI	Clean steam temperature hot	
					62	WASTE_ TEMP_HI	Waste steam temperature hot	
					64	WASTE_ TEMP_HI	Water in temperature hot	
						Operator e	rror	Replace cable
 CA11	Conductivity sensor	Analogue input	1	1				Replace sensor
					R	efer to technical de	ocumentation	Replace controller

Alarm	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
		Water conductivity			Flashing	Wire pinched or kinked
6	CATI_ANLG_ALA_   Analog input alarm   Pinched cabl		Pinched cable from sensor	-	conductivity	Sensor failure
		onort orroad			iodamigo	BC3250 controller failure
7	COND_TEMP_HI	Condensate temperature hot	Temperature exceeds 40 °C/104 °F	-	High condensate temperature alarm	System isolation not complete
		Feedwater flow rate			Flashing	Wire removed from sensor
9	FA01_ANLG_ALA_ OPEN	Analog input alarm circuit open	Cables removed from sensor	-	conductivity	Sensor failure
		circuit open			readings	BC3250 controller failure
		Feedwater flow rate			Flashing	Wire pinched or kinked
10	FA01_ANLG_ALA_ SHRT	temperature Analog input alarm short	Pinched cable from sensor	-	conductivity	Sensor failure
		circuit			Toddings	BC3250 controller failure
11	FEED_PRES_HI	Feedwater	Pressure exceeds	-	Warning displayed	- Service sequence
		pressurised	0.1 bar g/ 1.45 psi g		Emergency stop	
12	FEED_TEMP_HI	Feedwater temperature hot	Temperature exceeds 40 °C/104 °F	-	Warning displayed  Emergency stop	Service sequence
						Wire removed from sensor
		Danel temperature			Emergency stop	Sensor failure
13	LA11_ANLG_ALA_ OPEN	Panel temperature analogue input alarm circuit open	Cables removed from sensor	Ceased production of clean steam	displayed on HMI/ Flashing conductivity readings	BC3250 controller failure
					reauriys	Sensor not calibrated
						Wire pinched or kinked
					Emergency stop	Sensor failure
14	LA11_ANLG_ALA_ SHRT		Pinched cable from sensor	Ceased production of clean steam	displayed on HMI/ Flashing conductivity	BC3250 controller failure
				sensor of clean steam		Sensor not calibrated

	C	omponent				Cause	)	Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
					Operator error		error	Replace cable
CA11	Conductivity sensor	Analogue input	1	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
TA41	Temperature sensor	Analogue input	4	1		Operator e	error	Close isolation valve VM51
						Operator e	error	Replace cable
FA01	Flowmeter	Analogue input	0	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
FA01	Flowmeter	Analogue input	0	1	R	efer to technical d	ocumentation	Replace sensor
		·			Refer to technical documentation		Replace controller	
-	-	-	-	-	Ins	ufficient isolation o	during servicing	Work and check isolation valves
-	-	-	-	-	Ins	ufficient isolation o	during servicing	Work and check isolation valves
						Operator e	error	Replace cable
					R	efer to technical d	ocumentation	Replace sensor
LA11	Level sensor	Analogue input	1	1	R	efer to technical d	ocumentation	Replace controller
					Sei	nsor transmitting le	ess than 3.8mA	Check HMI for mA reading, lower sensor until lowest point on scale reads 4mA
						Operator e	error	Replace cable
					R	efer to technical d	ocumentation	Replace sensor
LA11	Level sensor	Analogue input	1	1	R	efer to technical d	ocumentation	Replace controller
					Ser	nsor transmitting m	nore than 20mA	Check HMI for mA reading, (when the generator is empty) lower sensor until lowest point on scale reads 4mA

Alarm	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
					Emergency stop	Wire removed from sensor
16	PA01_ANLG_ALA_ OPEN	ODEN analogue input from consor of clean steam	displayed on HMI/ Flashing conductivity	Sensor failure		
		alarm circuit open			readings	BC3250 controller failure
		Panel temperature			Emergencey stop displayed on HMI/	Wire pinched or kinked
17	PA01_ANLG_ALA_ SHRT	analogue input alarm short circuit	Pinched cable from sensor	Ceased production of clean steam	Flashing conductivity	Sensor failure
		alailli short chedit			readings	BC3250 controller failure
		Danel temperature			Emergency stop	Wire removed from sensor
18	PA21_ANLG_ALA_ OPEN	Panel temperature analogue input	Cables removed from sensor	Ceased production of clean steam	displayed on HMI/ Flashing	Sensor failure
		alarm circuit open			conductivity readings	BC3250 controller failure
		Danel temperature			Emergency stop	Wire pinched or kinked
19	PA21_ANLG_ALA_ SHRT	Panel temperature analogue input alarm short circuit	Pinched cable from sensor	Ceased production of clean steam	displayed on HMI/ Flashing conductivity	Sensor failure
		alaim short circuit			readings	BC3250 controller failure
		Supply steam in			Flooking	Wire removed from sensor
20	PA31_ANLG_ALA_ OPEN	pressure Analog input alarm circuit	Cables removed from sensor	-	Flashing conductivity readings	Sensor failure
		open			readings	BC3250 controller failure
		Supply steam in			Flacking	Wire pinched or kinked
21	PA31_ANLG_ALA_ SHRT	pressure Analog input alarm short	Pinched cable from sensor	-	Flashing	Sensor failure
		circuit			readings	BC3250 controller failure
22	PRI_BAND_HI_ ALARM	Primary band HIGH alarm	-	Emergencey stop sequence-Ceased production of clean steam	Emergency stop displayed on HMI	Reduced primary pressure

	C	Component				Cause	)	Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
				· I				
						Operator e	error	Replace cable
PA01	Pressure sensor	Analogue input	0	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
PA01	Pressure sensor	Analogue input	0	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
PA21	Pressure sensor	Analogue input	2	1	R	efer to technical d	ocumentation	Replace sensor
					Refer to technical documentation		Replace controller	
						Operator e	error	Replace cable
PA21	Pressure sensor	Analogue input	2	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
PA31	Pressure sensor	Analogue input	3	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
					Operator error		Replace cable	
PA31	Pressure sensor	Analogue input	3	1	R	efer to technical d	ocumentation	Replace sensor
					Refer to technical documentation		Replace controller	
						<u>.</u>		Re-tune system
-	-	-	-	-		Setpoint not a	chieved	Leaking control valve

Alarm	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
		1	1			
23	PRI_BAND_LOW_ ALARM	Primary band LOW alarm	Control valve failed closed	Emergencey stop sequence-Ceased production of clean steam	Emergency stop displayed on HMI	Customer steam supply
24	PRI_CAP_ALARM	Primary control capacity alarm	Valve over 99% open	Target clean steam pressure not achieved	Alarm displayed on HMI	Steam demand exceeds CSG capacity.
25	PRI_PRES_HI	Primary side pressurised	Pressure exceeds 0.1 bar g/ 1.45 psi g		Emergency stop displayed on HMI	Service sequence
26	PRI_PRES_LOW	Primary pressure low alarm	Valve 100% open	Emergencey stop sequence-Ceased production of clean steam	Emergency stop displayed on HMI	Primary pressure PA31 lower than setpoint for clean steam pressure
27	PRI_TEMP_HI	Primary side temperature hot	Temperature exceeds 40 °C/104 °F	-	-	-
28	SEC_BAND_HI_ ALARM	Secondary band HIGH alarm	-	-	Alarm displayed on HMI	Leaking within valve
	/ L/ (L/ (L/ (L/ (L/ (L/ (L/ (L/ (L/ (L/	THOIT didini			11001	PID Settings

	С	omponent				Cause		Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
					Codensate blockage			Tune PID
-	-	-	-	-	Insufficient customer steam supply/ Qaulity of inlet steam			Fix Inlet steam supply
-	-	-	-	-	Insufficient capacity			Review IMI to check capacities
-	-	-	-	-	Incorrectly isolated valves		Check isolation valves	
PA31	Pressure sensor	-	-	-	In	sufficient custome	r steam suppy	Increase supply of inlet steam
-		-	-	-	-		-	
VA01	Water control valve	Analogue input	0	1	Water control valve stuck open		Inspect water control valve to identify cause	
						Poor PID Se	ttings	Adjust PID settings

Alarm number	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
						Water supply not sufficent
			No noise/ pump not spinning	No feedwater pressure	Water pump failure alarm	Air lock in water pump
						Power loss to pump
						Pump mechanical/ electrical failure
			Valve closed when not instructed		Water level low alarm Valve	For more
			Reduced water level on visual boiler sight glass	-	feedback alarm (OPT)	information see alarm 60
29	SEC_BAND_LOW_ ALARM	Secondary band LOW alarm	Boiler water being dumped to drain, potential for flash steam		Water level low alarm Valve feedback alarm (OPT)	Valve failure
			Excess Steam coming from drain Water level indicator low Sound from valve	Potential reduced CSG capacity More water consumption	-	Debris/ Wear
						TDS settings too Low
			Possible reduced pressure on pressure dial	-	-	Inlet water supply
30	SEC_CAP_ALARM	Secondary control capacity alarm	Valve over 99% open	Target clean steam pressure not achieved	Alarm on HMI	Steam demand exceeds CSG capacity
31	SEC_LVL_LOW	Secondary side boiler water level low	Level indicator low	Emergencey stop sequence-Ceased production of clean steam	Low water level alarm displayed, Emergency stop displayed on HMI	Water level lower than setpoint
32	SEC_PRES_HI	Secondary side pressurised	Pressure exceeds 0.1 bar g/ 1.45 psi g	-	Emergency Stop displayed on HMI	Service sequence
33	SEC_TEMP_HI	Clean steam temperature hot	Temperature exceeds 40 °C/104 °F	-	-	Temperature exceeds 40 °C/104 °F

	C	omponent				Cause		Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
						-		Check water supply (Pressure and ensure no debris-Check strainers/ Filters)
MB01 MD01	Pump	Analogue output Digital	0	1		-		Check air bleed
		input				-		Check power status
						Pump fail	ure	Refer to pump IMI
	Supply water	Analogue			Fo	r more informatior	ı see Alarm 60	For more Information see alarm 60
VB01	control valve	output	0	1				
VE11	Drain valve	Digital output	1	1		Visual inspection		Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
						Wear of s	eat	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
VE12	TDS control valve	Digital output	1	2		Debris in pi	peline	Check strainer screen on water inlet. Check for debris origin.
						TDS valve stu	ck open	Visit TDS Blowdown section in IMI for details. Check input water conductivity.
-	-	-	-	-		Inlet water supp	oly failure	Check inlet water supply for any blockages
-	-	-	-	-		Insufficient capacity		Review IMI to check capacities
-	-	-	-	-				
-	-	-	-	-	Isolation valves in service sequence		Check isolation valves	
-	-	-	-	-		-		-

TA01_ANLG_ALA_ OPEN	Fault
TA01_ANLG_ALA_ OPEN	
TA01_ANLG_ALA_ OPEN	
34 OPEN temperature Analog cables removed - conductivity readings	e removed from sensor
I Onen I I I I I I I I I I I I I I I I I I	ensor failure
	3250 controller failure
Feedwater Flashing	ire pinched or kinked
35 SHRT input alarm short sensor - conductivity sensor	ensor failure
l circuit	3250 controller failure
Emergency Stop	e removed from sensor
TA0X_ANLG_ALA_ OPEN  TA0X_ANLG_ALA_ OPEN  Panel temperature analogue input alarm circuit open  Cables removed from sensor production of clean conductivity  Cables removed from sensor production of clean conductivity	ensor failure
	3250 controller failure
Emergencey stop Emergencey Stop	ire pinched or kinked
TANY ANI C ALA Parier temperature   Pinched cable from   sequence Ceased   displayed on Hilli	ensor failure
l steam ' '	3250 controller failure
	High panel temperature
Water in	e removed from sensor
TA11_ANLG_ALA_ OPEN	ensor failure
I Open I I I I I I I I I I I I I I I I I I I	3250 controller failure
Water in Fleshing	ire pinched or kinked
40 TA11_ANLG_ALA_ temperature Analog Pinched cable from SHRT input alarm short sensor - Conductivity S	ensor failure
circuit readings BC:	3250 controller failure

	С	omponent				Cause	<b>)</b>	Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
					Operator error			Replace cable
TA01	Temperature sensor	Analogue input	0	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
TA01	Temperature sensor	Analogue input	0	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
TAX1	Temperature of panel	Analogue input	0	1	R	efer to technical d	ocumentation	Replace sensor
					Refer to technical documentation		Replace controller	
						Operator e	error	Replace cable
TAX1	Temperature of panel	Analogue input	0	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
TAX1	Temperature of panel	Analogue Input	Χ	1		High ambient te	mperature	Reduce environment temperature
						Operator e	error	Replace cable
TA11	Temperature sensor	Analogue input	1	1	R	efer to technical d	ocumentation	Replace sensor
					Refer to technical documentation		Replace controller	
						Operator e	error	Replace cable
TA11	Temperature sensor	Analogue input	1	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller

Alarm	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
		Clean steam		Emergencey stop	Emergency Stop	Wire removed from sensor
41	TA21_ANLG_ALA_ OPEN	temperature Analog input alarm circuit	Cables removed from sensor	sequence-Ceased production of clean	displayed on HMI/ Flashing conductivity	Sensor failure
		open		steam	readings	BC3250 controller failure
		Clean steam		Emergencey stop	Emergency Stop displayed on HMI/	Wire pinched or kinked
42	TA21_ANLG_ALA_ SHRT	temperature Analog input alarm short	Pinched cable from sensor	sequence-Ceased production of clean	Flashing conductivity	Sensor failure
		circuit		steam	readings	BC3250 controller failure
		Supply steam			Flashing	Wire removed from sensor
43	TA31_ANLG_ALA_ OPEN	temperature Analog input alarm circuit	Cables removed from sensor	-	conductivity readings	Sensor failure
		open			readings	BC3250 controller failure
		Supply steam			Floobing	Wire pinched or kinked
44	TA31_ANLG_ALA_ SHRT	temperature Analog input alarm short	Pinched cable from sensor	-	Flashing conductivity readings	Sensor failure
		circuit			readings	BC3250 controller failure
		Supply waste			Flashing	Wire removed from sensor
45	TA41_ANLG_ALA_ OPEN	temperature Analog input alarm circuit	Cables removed from sensor	-	conductivity readings	Sensor failure
		open			Toddings	BC3250 controller failure
		Supply waste			Floobing	Wire pinched or kinked
46	TA41_ANLG_ALA_ SHRT	temperature Analog input alarm short	Pinched cable from sensor	-	Flashing conductivity	Sensor failure
		circuit			readings	BC3250 controller failure
		Condensate out			Florities	Wire removed from sensor
47	TA51_ANLG_ALA_ OPEN	temperature Analog input alarm circuit	Cables removed from sensor	-	Flashing conductivity	Sensor failure
		open open			readings	BC3250 controller failure

	C	component				Cause	)	Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
						Operator e	error	Replace cable
TA21	Temperature sensor	Analogue input	2	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
TA21	Temperature sensor	Analogue input	2	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
TA31	Temperature sensor	Analogue input	3	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
TA31	Temperature sensor	Analogue input	3	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
TA41	Temperature sensor	Analogue input	4	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
TA41	Temperature sensor	Analogue input	4	1	Refer to technical documentation		Replace sensor	
					Refer to technical documentation		Replace controller	
					Operator error		Replace cable	
TA51	Temperature sensor	Analogue input	5	1	R	efer to technical d	ocumentation	Replace sensor
		,			R	efer to technical d	ocumentation	Replace controller

Alarm	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
		Condensate out			Flashing	Wire pinched or kinked
48	TA51_ANLG_ALA_ SHRT	temperature Analog input alarm short	Pinched cable from sensor	-	conductivity	Sensor failure
		circuit			readings	BC3250 controller failure
		Drain temperature			Flashing	Wire removed from sensor
49	TA52_ANLG_ALA_ OPEN	analogue input alarm circuit open	Cables removed from sensor	-	conductivity	Sensor failure
		a.a.m onount opon			.caagc	BC3250 controller failure
		Drain temperature			Flashing	Wire pinched or kinked
50	TA52_ANLG_ALA_ SHRT	analogue input	Pinched cable from sensor	-	conductivity	Sensor failure
		diami short shoul			roddingo	BC3250 controller failure
51	TDS_HI	TDS failure	-	High levels of	TDS alarm displayed	TDS set point exceeded
31	103_пі	1 D3 Tallule	-	conductivity	TDS alaitii displayed	Invalid time duration entry
52	TDS_HYS_FAIL	TDS hysteresis fault	Continuous Blowdown	-	TDS hysteresis alarm displayed	TDS hysteresis setpoint not achieved
54	TRAP_FAIL_CLOSE	Trap failure close	Cold before trap, steam collapse/ waterhammer on start up (noise at primary inlet)	Startup not achieved	No alarm	No steam in heat exchanger to heat water
			-	Rapid loss of clean steam pressure	Trap Failed Closed Alarm on HMI	Rapid build-up of condensate
55	TRAP_FAIL_OPEN	Trap Failure Open	High temperature/ WaterHammer/ Pressurised Condensate return system	Increase in Supply water temperature and pressure	Trap Fail open alarm displayed on HMI	Condensate travelling uncontrolled through trap
			Increase in steam consumption	Pressurised condensate return system		

	С	omponent			Cause			Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
						Operator e	Replace cable	
TA51	Temperature sensor	Analogue input	5	1	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
TA52	Temperature sensor	Analogue input	5	2	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
TA52	Temperature sensor	Analogue input	5	2	R	efer to technical d	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
VE12	TDS valve	Disital autout	1	2		TDS set point e	exceeded	Take action to reduce TDS, if necessary adjust setpoint Visit
VEIZ	105 valve	Digital output	1	2		Input error o	n HMI	TDS blowdown section in IMI for details
						Input error o	n HMI	Adjust setpoint whilst referring to IMI
VE12	TDS valve	Digital output	1	2		Partially block	ed valve	Inspect blocked valve
						Restrictions in t	olowdown	Inspect any blockages in blowdown
QU51	Steam trap	Uncontrolled	5	1	Blocka	Blockage in condensate line during start-up		Identify blockages
					Blockage in condensate line during operation			
QU51	Steam trap	Uncontrolled	5	1		Wear of s Debris in pi <sub>l</sub>		Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.

Alarm	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
		Water level control			Flashing	Wire removed from sensor
56	VA01_ANLG_ALA_ OPEN	valve feedback Analog input alarm	Cables removed from sensor	-	conductivity	Sensor failure
	· ·	circuit open			readings	BC3250 controller failure
		Water level control			Flashing	Wire pinched or kinked
57	VA01_ANLG_ALA_ valve feedback SHRT Analog input alar		Pinched cable from sensor	-	conductivity	Sensor failure
		short circuit			readings	BC3250 controller failure
		Supply steam in control valve			Flashing	Wire removed from sensor
58	VA31_ANLG_ALA_ OPEN	feedback Analog	Cables removed from sensor	-	conductivity	Sensor failure
		input alarm circuit open			readings	BC3250 controller failure
		Supply steam in control valve			Flashing	Wire pinched or kinked
59	VA31_ANLG_ALA_ SHRT	feedback Analog	Pinched cable from sensor	-	conductivity	Sensor failure
		input alarm short circuit			readings	BC3250 controller failure
			Valve not open when instructed.	-	Valve feedback alarm (OPT), Water level failure alarm,	Leaking seat/ plug
			matructeu.		Water level high alarm	Positioner failure
						Positioner calibration faulty
60	VB01_FBK	Feedwater control feedback error				Actuator failure
				Potential reduced	Water Level Low	Mechanically failed shut
			Valve closed when ot instructed.	CSG capacity. More	alarm, Valve feedback alarm	Positioner failure
				water consumption	(OPT)	Actuator failure
					Valve feedback	Valve failure
			Gauling Valve		alarm (OPT), Water level failure alarm, Water level high alarm	Positioner failure
	•	-	•		*	

	С	component				Cause	)	Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
					Operator error			Replace cable
VA01	Feedwater control valve	Analogue input	0	1	R	efer to technical de	ocumentation	Replace sensor
					R	efer to technical do	ocumentation	Replace controller
						Operator e	error	Replace cable
VA01	Feedwater control valve	Analogue input	0	1	R	efer to technical do	ocumentation	Replace sensor
					R	efer to technical d	ocumentation	Replace controller
						Operator e	error	Replace cable
VA31	Plant steam control valve	Analogue input	3	1	R	efer to technical do	ocumentation	Replace sensor
					R	efer to technical do	ocumentation	Replace controller
						Operator e	error	Replace cable
VA31	Plant steam control valve	Analogue input	3	1	R	efer to technical de	ocumentation	Replace sensor
		·			R	efer to technical do	ocumentation	Replace controller
						Wear of s	eat	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
						Debris in pip	peline	Check strainer screen on water inlet. Check for debris origin.
					Misn	natch between pos	sitioner and PLC	
					Mismato	th between position indicator position	ner and actual stem n and PLC	
VA01	Feedwater control valve	Analogue input	0	1	Mismatch between positioner and actual stem indicator position and PLC			
					Gailing of stem		Identify failed part with tag and schematic in IMI. Consult	
					Misn	natch between pos	sitioner and PLC	individual product IMI. Replace or repair failed part.
					Mismatch between positioner and actual stem indicator position and PLC			
				Gailing/ Wear of stem				
					Misn	natch between pos	sitioner and PLC	

Alarm	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
			Valve not open when	_	Valve feedback alarm (OPT), Water level failure alarm,	Leaking seat/ plug
			instructed.		Water level high alarm	Positioner failure
						Positioner calibration faulty
61	VB31_FBK	Steam in control feedback error				Actuator failure
				Potential reduced	Water Level Low	Mechanically failed shut
			Valve closed when not instructed	CSG capacity. More water consumption	alarm. Valve feedback alarm	Positioner failure
				·	(OPT)	Actuator failure
					Valve feedback alarm (OPT), Water	Valve failure
			Gauling valve		level failure alarm, Water level high alarm	Positioner failure
62	WASTE_TEMP_HI	Waste steam temperature hot	Temperature exceeds 40 °C/104 °F	Service sequence halted	-	Service sequence
						Power loss to pump
63	WATER_PUMP_ FAIL	Water pump failure	No Sound from	Reduced output of clean steam	Alarm displayed on HMI	Water supply not sufficient
	PAIL		water pump	clean steam	ПІМІ	Air lock in water pump
						Pump mechanical/ electrical failure
64	WATER_TEMP_HI	Water in temperature hot	Temperature exceeds 40 °C/104 °F	Service sequence halted	Alarm displayed on HMI	Service sequence
66	SEC_PRES_LIM	Secondary high pressure limit alarm	-	Emergency Stop Sequence- Ceased production of clean steam	Emergency stop displayed on HMI	Control issue

	C	Component				Cause	<b>.</b>	Action	
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION		
					Wear of seat			Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
						Debris in pi	peline	Check strainer screen on water inlet. Check for debris origin.	
					Misr	match between pos	sitioner and PLC		
					Mismato	ch between positio indicator position	ner and actual stem n and PLC		
VA01	Feedwater control valve	Analogue input	0	1	mismato	ch between positio indicator position	ner and actual stem n and PLC		
						Gailing of	stem	Identify failed part with tag and schematic in IMI. Consult	
					Misr	match between pos	sitioner and PLC	individual product IMI. Replace or repair failed part.	
					Mismato	ch between positio indicator position			
						Gailing/ Wear of stem			
-	-	-	-	-	Ins	ufficient isolation o	during servicing	Work and check isolation valves	
						-		Check power status	
MB01	Pump	Analogue output Digital	0	1	I	nsufficient water h	ead pressure	Check water supply (Ensure no debris, checking strainers and filters along with the pressure)	
MD01	·	input			Insufficient bleeding		Check air bleed		
					-		Refer to pump IMI-Suspect pump internal failure		
-	-	-	-	-	Insufficient isolation during servicing		Work and check isolation valves		
LD11	Level switch	Digital input	1	1		-		Check settings on pressure switch.	

Alarm number	Alarm PLC tag	Alarm description		Identfier		Fault
number			Physical	Process	System	
67	INITIALISE	PLC Start-up from power cycle	-	No Clean Steam Produced/CSG not operational	No display on HMI or partial display	Faulty PLC
68	WATER_LVL_HI	Water level high	Water Level exceeds	Inaccurate control of water control valve	Alarm displayed on	Water level exceeds
00	WATER_EVE_III	alarm	90%	Water control valve failed open	HMI	90%
69	WATER_LVL_ ALARM	Water level failure	TDS Valve opening outside of TDS control	-	Alarm displayed on HMI	Repeated high water level alarm on HMI
70	AIR_PRESS_FAIL	Air supply pressure fail	No valve movement	-	Alarm displayed on HMI	Insufficient Compressed Air
71	VE31_FAIL_OPEN	Plant isolation valve fail open	-	Start-up/ Shutdown sequence would halt	Alarm displayed on HMI	Leaking seat
			Actuator Indicator in incorrect Position			Actuator failure
72	VE31_FAIL_CLOSE	Plant isolation valve fail closed	Indicator displays closed when instructed to open	CSG does not start/ Loss of clean steam supply	Alarm displayed on HMI	Valve does not leave closed position when instructed
73	VE31_FAIL_STICK	Plant isolation valve fail stuck	Actuator indicator shows neither on/off	Start-up/ Shutdown sequence would halt	Alarm displayed on HMI	Leaking seat
						Actuator failure
74	VE31_FAIL_SPEED	Inlet Plant valve fail opening speed	Possible waterhammer in primary side	-	Alarm displayed on HMI	Unrestricted exhaust flow from actuator

	C	omponent				Cause		Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
-	-	-	-	-		PLC failu	ire	Contact SXS engineer
VA01	Feedwater	Analogue	0	1	65	WATER_VLV_ FAIL	Water control valve failure	Inaccurate control of water control valve
VAUT	control valve	input	U	ı	65	WATER_VLV_ FAIL	Water control valve failure	Water control valve failed open
-	-	-	-	-	Se	ee Alarm 68 for mo	re information	See Alarm 65 for more Information
PDX1	Air supply	Digital input	0	1	-			Restore air supply
VE31	Steam isolation valve	Digital output	3	1	Wear of seat		Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
	isolation valve				Debris in pipeline		Check strainer screen on water inlet. Check for debris origin.	
VE31	Steam isolation valve	Digital output	3	1	ı	nsufficient custom	er air supply	Check customers air supply line
VE31	Steam isolation valve	Digital output	3	1	Mismato	ch between positio indicator position	ner and actual stem n and PLC	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
					Wear of seat		Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
VE31	Steam isolation valve	Digital output	3	1	Debris in pipeline		Check strainer screen on water inlet. Check for debris origin.	
					Insufficient customer air supply		Check customers air supply line	
VE31	Steam isolation valve	Digital output	3	1	E	xhaust restrictor s	et incorrectly	Reset/ Replace exhaust restrictor

Alarm	Alarm PLC tag	Alarm description		Fault		
number			Physical	Process	System	
75	VE21_FAIL_OPEN	Outlet isolation valve fail open	-	Start-up/ Shutdown sequence would halt	Alarm displayed on HMI	Leaking seat
			Actuator Indicator in incorrect position			Actuator failure
76	VE21_FAIL_CLOSE	Outlet isolation valve fail closed	Indicator displays closed when instructed to open	CSG does not start/ Loss of clean steam supply	Alarm displayed on HMI	Valve does not leave closed position when instructed
77	VE21_FAIL_STICK	Outlet isolation valve fail stuck	Actuator indicator shows neither on/off	Start-up/ Shutdown sequence would halt	Alarm displayed on HMI	Leaking seat
						Actuator failure
78	VE21_FAIL_SPEED	Outlet isolation valve fail opening speed	Waterhammer	Sudden/ rapid pressure loss Risk of carryover	Alarm displayed on HMI	Unrestricted exhaust flow from actuator
						Failed open control valve
81	PRI_BAND_HI_ ALERT	Primary band high alert	-	High clean stem pressure	Alert displayed on HMI	Leaking control valve
	ALLINI	aiert		pressure	THVII	Leak in heat exchanger
						PID settings
						Valve positioning incorrect
82	PRI_BAND_LOW_ ALERT	Primary band low alert	Control valve closed for a given amount	Low clean steam	Alert displayed on	PID settings
	ALERI	aleit	of time	pressure	НМІ	Customer supply steam
						Restricted condensate flow

	С	omponent				Cause	)	Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
					Wear of seat			Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
VE21	Steam isolation valve	Digital output	2	1		Debris in pi	peline	Check strainer screen on water inlet. Check for debris origin.
					I	nsufficient custom	er air supply	Check customers air supply line
VE21	Isolation valve	Digital output	2	1	Mismato	ch between positio indicator position	ner and actual stem n and PLC	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
VE21	isolation valve	Digital output	2	1		Wear of s	eat	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
		3				Debris in pi	peline	Check strainer screen on water inlet. Check for debris origin.
					ı	nsufficient custom	er air supply	Check customers air supply line
VE21	isolation valve	Digital output	2	1	E	xhaust restrictor s	et incorrectly	Reset/ Replace exhaust restrictor
					Se	ee alarm 71 for mo	re information	See Alarm 71 for more Information
						-		Identify leak in control valve
						-		Identify leak in heat exchanger
						Incorrect PID	settings	Adjust PID setting if necessary
VA31	Steam control valve	Analogue input	3	1	-		Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
					Incorrect PID settings		Adjust PID setting if necessary	
-	-	-	-	-	-		Fix inlet steam supply	
						Debris in pi	peline	Remove debris from pipeline

Alarm number	Alarm PLC tag	Alarm description		Identfier	Fault		
number			Physical	Process	System		
			Val 000/	-	Alert displayed on HMI	Plant steam	
83	PRI_CAP_ALERT	Primary control capacity alert	Valve over 99% open for a given amount of time			Capacity incorrect	
						Restricted condensate flow	
						PID settings	
84	SEC_BAND_HI_ ALERT	Secondary band high alert	-	Possible carryover	Alert displayed on HMI	Leaking valve	
85	SEC_BAND_LOW_ ALERT	Secondary band low alert	-	-	Alert displayed on HMI	Positioner failure	
						PID settings	
86	SEC_CAP_ALERT	Secondary control capacity alert	-	-	Alert displayed on HMI	Insufficient water supply	
87	VE51_FAIL_SPEED	Condensate isolation valve fail opening speed	Waterhammer	Sudden/ rapid pressure loss Risk of carryover	Alarm displayed on HMI	Unrestricted exhaust flow from actuator	
				Emergency Stop	Emergency stop displayed on HMI	Clean steam thermistat tripped	
88	TEMP_LIM	Saturated pressure temperature limit	-	Sequence- Ceased production of clean steam		Low water level limit exceeded	
89	HMI_SYNC_ALARM	HMI Communications Fault	HMI Unresponsive	Optional: Emergency Stop Sequence- Ceased production of clean steam	HMI connection banner	Communication between PLC and HMI has been lost	
		Integrity test leak alarm	Leak pipe joints			Leak in pipe joints	
90	ALA_TEST_LEAK_ NEG		Leak in steam control valve	Ceased production of clean steam	Alarm displayed on HMI	Leak in steam control valve	
			Leaks in Integrity test valves			Leak in isolation valves	

Component				Cause			Action	
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
VA31	Plant steam control valve	Analogue input	3	1	Plant steam Insufficient		Fix Plant steam	
						Capacity inc	orrect	See IMI for correct capacities.
-	-	-	-	-	Debris in pipeline		Inspect pipeline and remove any debris	
					Inspect PID settings		Adjust PID settings if necessary	
-	-	-	-	-	-		Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
-	-	-	-	-	- Inspect PID settings		Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
							Adjust PID settings if necessary	
-	-	-	-	-	Debris in pipeline		Remove any debris from pipeline.	
VE51	isolation valve	Digital output	2	1	Exhaust restrictor set incorrectly		Reset/ Replace exhaust restrictor	
TD21	Temperature switch	Digital input	2	1	Clean steam temperature exceeds set limit		Investigate clean steam temperture source	
	SWITCH				Clea	n steam temperati	ure switch failure	Identify failed part with tag and schematic in IMI. Consult
					V	Vater level below a	ıllowanle limit	individual product IMI. Replace or repair failed part.
LD11	Level switch	Digital input	1	.   .		Water low level switch failure		Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.
						HMI Fail	ure	Replace HMI
-	HMI screeen	-	-	-	Connection fault with ethernet cable		Check ethernet ports for connection and communication lights	
-	-	-	-	-	-		Inspect pipe joints	
VA31	Steam control valve	Anaolgue input	3	1	-		Inspect steam control valve	
-	-	-	-	-	-		Inspect isolation valves	

Alarm	Alarm PLC tag	Alarm description		Identfier	Fault			
number			Physical	Process	System			
91	ALA_TEST_POS_ MAX	Integrity test count alarm	-	Ceased production of clean steam	Alarm displayed on HMI	Maximum number of integrity tests reached		
92	DRAIN_TEMP_HI	Drain temperature hot	Temperature exceeds 40 °C / 104 °F	Service sequence halted	Alarm displayed on HMI	Service sequence		
93	ESTOP_PB	Emergency stop button pressed	E-stop button locked in	Ceased production of clean steam	Emergency stop displayed on HMI	-		
94	PRE_CYCLE_LIMIT	Pre-heater thermal cycles limit	-	Possible stress cracks in pre-heater	Alarm displayed on HMI	-		
95	PRE_HP_TA11_ LOW	Preheater temperature low	Temperature falls below TA21 - 2.5°	Ceased production of clean steam	Alarm displayed on HMI	Preheater pressure too low		
96	PRE_HP_TA11_HI	Preheater temperature high	Temperature raises above TA21 + 2.5°	Ceased production of clean steam	Alarm displayed on HMI	Overpressure in the preheater		
	PRI_BAND_HI_ ALERT	Prirmary band high alert	-	High clean stem pressure	Alert displayed on HMI	Failed open control valve		
97						Leaking control valve		
						Leak in heat exchanger		
						PID settings		
			Control valve closed for a given amount of time				Valve positioning incorrect	
98	PRI_BAND_LOW_ ALERT			Low clean steam pressure	Alert displayed on HMI	PID settings		
						Customer supply steam		
						Restricted condensate flow		
		RI_CAP_ALERT Primary control capacity alert	Valve over 99% open for a given amount of time	-		Plant steam		
99	PRI_CAP_ALERT				Alert displayed on HMI	Capacity incorrect		
						Restricted condensate flow		

Component					Cause			Action
TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
-	-	-	-	-	Air pressure rises during integrity test requires customer decision before clean steam production can begin		Use on-screen pop-up screen	
TA52	Temperature sensor	Anaolgue input	5	2	Insufficent isolation during servicing		Work and check isolation valves	
-	-	-	-	-	User operated		Release e-stop button and press reset button	
-	-	-	-	-		nber of allowable to preheater has bee	hermal spikes for the n exceeded	Replace Pre-heater
TA11 and TA21	Temperature Sensor	Analogue input	1 and 2		Check preheater HE02 for scale and re-set VU33. Alarm could also be triggered due to poor PID tuning.		Reset VU33 and retune PID settings	
TA11 and TA21	Temperature Sensor	Analogue input	1 and 2		Mal-adjusted VU33 or primary side overpressure or poor PID tuning		Perform inspection on VU33 and primary steam control valve	
				,	See alarm 71 for more information		See Alarm 71 for more Information	
					-		Identify leak in control valve	
					-		Identify leak in heat exchanger	
					Incorrect PID settings		Adjust PID setting if necessary	
VA31	Steam control valve	Analogue input	3	1	-		Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
						Incorrect PID	settings	Adjust PID setting if necessary
-	-	-	-	-		-		Fix inlet steam supply
					Debris in pipeline		Remove debris from pipeline	
VA31	Plant steam control valve	Analogue input	3	1	Plant steam Insufficent		Fix Plant steam	
					Capacity incorrect  Debris in pipeline		See IMI for corrcet capacities.	
-	-	-	-	-			Inspect pipeline and remove any debris	

Alarm number	Alarm PLC tag	Alarm description		Identfier	Fault		
number				Physical Process Sy			
						PID settings	
100	SEC_BAND_HI_ ALERT	Secondary band high alert	-	Possible carryover	Alert displayed on HMI	Leaking valve	
101	SEC_BAND_LOW_ ALERT	Secondary band low alert	-	-	Alert displyayed on HMI	Positioner failure	
						PID settings	
102	SEC_CAP_ALERT	Secondary control capacity alert	-	-	Alert displayed on HMI	Insuffiecnt water supply	

	Component						Cause	Action	
	TAG number	Item description	Control type	Zone	Instance	Alarm No	ALARM PLC TAG	ALARM DESCRIPTION	
						Inspect PID settings			Adjust PID settings if necessary
	-	-	-	-	-		-	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
	-	,	,	-	-		-	Identify failed part with tag and schematic in IMI. Consult individual product IMI. Replace or repair failed part.	
						Inspect PID settings			Adjust PID settings if necessary
	-	-	-	-	-		Debris in pip	peline	Remove any debris from pipeline.

# 8. Maintenance

Before starting any maintenance operation, carefully read the general safety information in Section 1 of this document.



Before starting any installation or maintenance operation, make sure that power has been shut-off.

To carry out many maintenance procedures, the unit shall be isolated from the system. The unit can be re-inserted in the system only after completing all the procedures.

It is recommended that maintenance personnel carry out the shut-down and start-up procedures described in this manual.

After the maintenance activities is required a washing cycle with a CIP (cleaning in place), or other procedure required by the process/plant directives.

#### 8.1 General information

The maintenance of single system components must be carried out as indicated in the individual installation and maintenance manuals (IM).

#### 8.2 Inspection/replacement of the tube bundle of the generator

The U-shaped tube bundle is the core of the steam generator. It must be removed and inspected every two years or as established by the terms of the warranty. The plate of the tube bundle is secured between the flanges of the vessel of the generator and the primary steam head. It is fitted with two gaskets:

- 1 shell side of the generator, between the tube bundle plate and body/shell of the generator.
- 1 head side (2-passes), between the tube bundle plate and primary steam head.

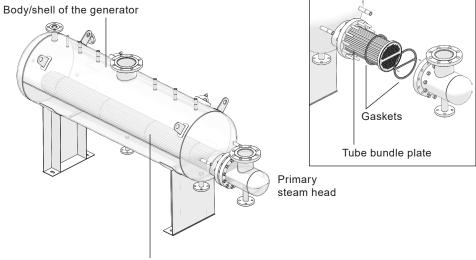


Fig. 8 "U" shaped tube bundle

#### 8.2.1 Disassembly of the tube bundle:

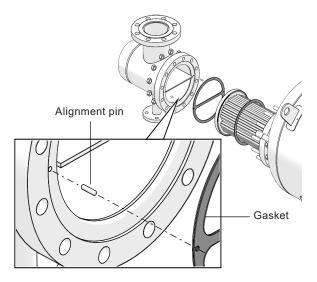
- Check that primary steam, condensate return line, feedwater inlet and clean steam outlet are isolated; that both circuits (primary
  and secondary) are not pressurized; that the generator has been completely drained and all components and surfaces are cold.
- Carefully remove the insulation from the header of the generator unscrewing the bolts on the aluminium cladding.
- Carefully disconnect the piping between the head of the generator and the primary steam inlet and condensate blowdown lines, with the utmost care so that no part of the line has damage.
- Separate the head from the generator, removing the bolts that secure it to the body.
- Carefully pull the tube bundle and hold it with the proper mechanical equipment slightly raised above the lower rim of the body flange, allowing a correct extraction without interferences.

#### 8.2.2 Inspection of the tube bundle:

- Inspect the tube bundle for scale and/or leaks. In the absence of leaks, remove scale and carefully clean the tube bundle before
  preparing this for installation.
- If detected, even a leakage, contact Spirax Sarco to repair or replace the tube bundle.

# 8.2.3 Re-assembly of the tube bundle:

- Remove the old gaskets, thoroughly clean mating surfaces and install two new gaskets: one between the tube plate and generator (shell side), the other with the sector divider between the tube plate and the head (head side).
- Carefully insert the tube bundle in the generator body, use alignment pins for correct positioning of head/gasket/bundle.



- After making sure that the tube is properly in place, assemble the primary steam head by aligning the divider at the dividing line between the two passes of the tubes (expected perfectly parallel to the horizontal plane), then tighten the bolts.
- Reconnect the inlet and outlet primary lines to the steam head. Check that these have been reconnected also where they may have been detached to facilitate extraction of the tube bundle.
- Carefully check all connections to detect any leaks during start-up.

# 8.3 Inspection/Replacement of the pressure safety switch

The safety pressure switch acts as a fail-safe for Spirax Sarco Clean Steam Generators. The alarm and shut down for high pressure is set at a value lower than the set of the safety valve. If the pressure safety switch mounted on the tank is not functioning correctly and must be replaced, follow the procedures outlined below.

#### 8.3.1 Disassembly of the pressure switch:

- Follow the shutdown procedure to take the unit off-line before attempting to replace the safety pressure switch.
- Turn off/disconnect all electric power before attempting any maintenance procedures.
- Check that primary steam, condensate return line, feedwater inlet, NCG vent and clean steam outlet are isolated; that both circuits (primary and secondary) are not pressurized; that the generator has been completely drained and all components and surfaces are cold
- Carefully disconnect the wires leading from/to the control cabinet.
- Loosen the connections until the pressure probe can be removed.

#### 8.3.2 Inspection of the pressure switch:

- Examine the probes for damage or incorrect positioning. For the exact procedure for examination, refer to the Spirax Sarco manual information included with the unit.

#### 8.3.3 Re-assembly of the pressure switch:

- To install a new unit, follow recommendations contained in the manufacturer's documentation.
- After ensuring that the unit is correctly installed, tighten the fittings.
- Follow the start-up procedures to put the unit back on-line. Carefully check all connections for any sign of leakage.

# 8.4 Replacement of the Pressure Safety Valve (Generator)

The pressure safety valve acts as a fail-safe for Spirax Sarco Compact Steam Generators. The valve will open for high pressure to protect the system from explosion. If the pressure safety valve mounted on the pressure vessel is not functioning correctly and must be replaced, follow the procedures outlined below.

#### 8.4.1 Disassembly of the safety valve:

- Follow the shutdown procedure to take the unit off-line before attempting to replace the safety pressure switch.
- Turn off/disconnect all electric power before attempting any maintenance procedures.
- Check that primary steam, condensate return line, feedwater inlet, NCG vent and clean steam outlet are isolated; that both circuits (primary and secondary) are not pressurized; that the generator has been completely drained and all components and surfaces are cold.
- After assuring that the pressure has been relieved from the tank, disconnect the vent line leading from the pressure relief valve to atmosphere (usually through the roof), and via a drip elbow, to drain.
- Carefully disconnect the pressure relief valve from between the generator vessel and feed tank.

#### 8.4.2 Re-assembly of the safety valve:

- Install the new valve. Follow recommendations contained in the manufacturer's documentation, local codes, or accepted contractor
  practices as to the use of joint compound or sealer at the connections.
- Reconnect the vent line leading from the pressure safety valve to atmosphere and, via drip elbow, to drain.
- Follow the start-up procedures to put the unit back on-line. Carefully check all connections for any sign of leakage.

#### 8.5 Inspection/Replacement of the pre-heater heat exchanger

If the pre-heater thermal cycle diagnostic indicates a replacement is required, follow the procedures outlined below. If the condensate outlet temperature sensor (TA51) has been disabled or faulty for an extended period of time, the pre-heater should be replaced every 2 years of regular use.

#### 8.5.1 Disassembly of the pre-heater:

- Follow the shutdown procedure to take the unit off-line before attempting to replace the pre-heater.
- Turn off/disconnect all electric power before attempting any maintenance procedures.
- Check that primary steam, condensate return line, feedwater inlet, NCG vent and clean steam outlet are isolated; that both circuits (plant and clean steam) are not pressurised; that the generator has been completely drained and all components and surfaces are cold.
- Loosen the connections until the pre-heater can be removed.

#### 8.5.2 Re-assembly of the pre-heater:

- To install a new unit follow recommendations contained in the manufactures documentation.
- After ensuring that the unit is correctly installed, tighten the fittings
- Follow the start-up procedures to put the unit back on-line. Carefully check all connections for any sign of leakage.

**8.6 Spare parts**For recommended spare parts for commissioning or maintenance, please contact our Service Department.

# 8.7 Recommend inspection

The following table indicate the suggested interval times for the inspection on the clean steam generator and of all the other components installed on the package.

Inspection	Refer to product IMI	Daily	Weekly	Quarter	
Blowdown		•			
Control valve	•				
Water level**		•			
Pressure level**				•	**
Level control	•				To verify the
Inlet and outlet line				•	difference between the measure of the
Pneumatic connections				•	transmittal agains the indicator
Electrical connection				•	the majoriti
Primary and secondary side pressure		•			
Safety valve	•				
Manual isolation valve			•		
Strainers				•	

# 8.8 Spirax Sarco Service maintenance

Spirax Sarco can provide on request of routine scheduled maintenance contract with the following steps. The maintenance contract usually includes two visits per year.

Maintenance Test	6 month visit	12 month visit	18 month visit	24 month visit
Visual inspection of control valves and actuators	•	•	•	•
Dismantle control valves, clean and visually inspect valve internals, replace valve stem seals		•		•
Check valve/actuator/positioners, zero and stroke, adjust if necessary	•		•	
Visual inspection of all wiring and terminations	•	•	•	•
Check all electrical connections for tightness	•	•	•	•
Ensure correct operation of pump (if present)		•		•
Pressure, temperature and level transmittal control		•		•
Functional inspection of safety components and PLC			•	•
Visual inspection of heat exchanger for external leakage	•	•	•	•
Tube bundle dismantled and inspection, gasket replacement				•
Preheater heat exchanger inspection (if present)				•
Check and clean all strainer screens, re-fit using new cap gaskets	•		•	
TDS test and probe check	•	•	•	•
TDS re-calibration		•		•
Fully functional test of the unit	•	•	•	•

# 9. Component map

The Components detailed below may not be fitted to all versions of the CSG-FB. Refer to section 9.2 for Component configuration lists. Optional items are designated with \*.

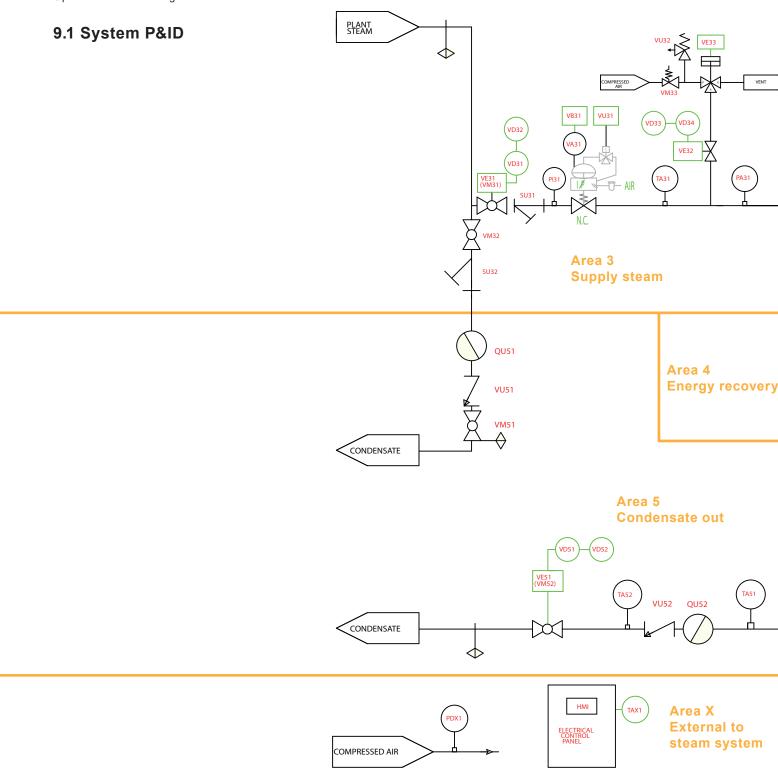
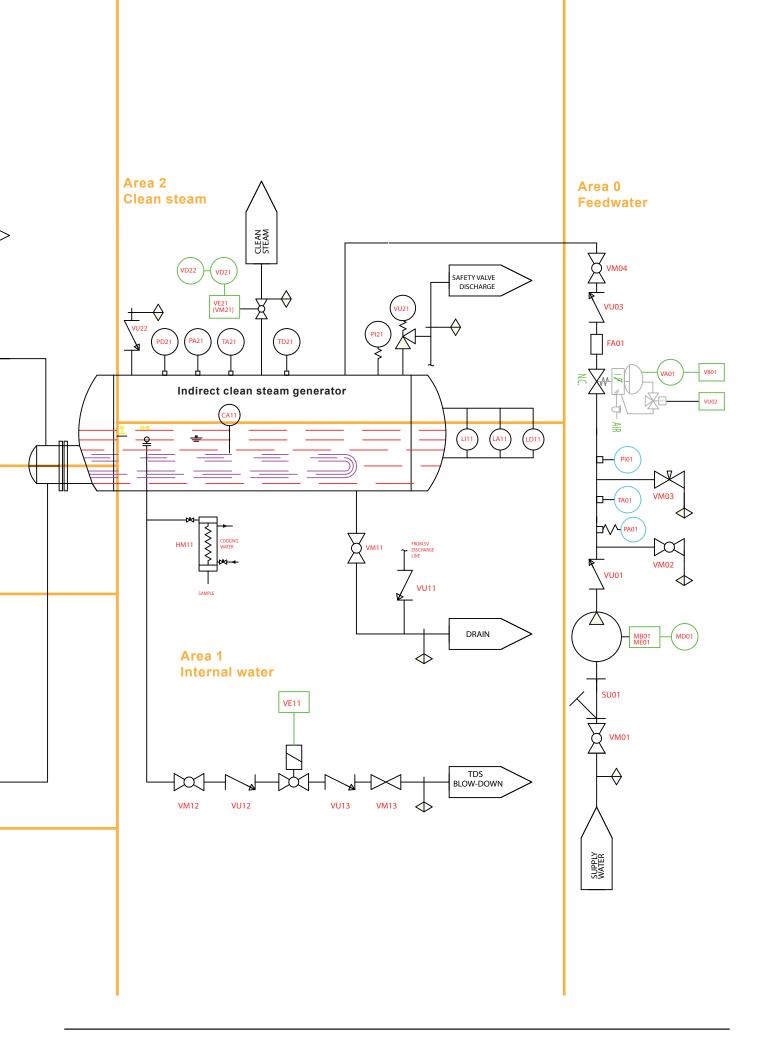


Fig. 9

CSG-FB Clean steam generation system for Food & Beverage



# 9.2 Component Configuration

The options available for the CSG-FB are listed in section 2.3. Many of the available options will utilise additional equipment fitted the system. The components specifically required for each option are listed below. Default items fitted as standard are identified with\*

#### Plant steam inlet isolation valve

Manual valve\*: VM31

Automated valve: VM31 replaced by VE31, VD31, and VD32

#### **TDS** control system

Timer control\*: VE11

Pulsed and continuous hysteresis control: VE12 and CA11

#### Feedwater pressurisation system

None\*

Integrated pump: MA01, MD01

#### Independent downstream plant protection

- None\*

Low level limit switch: LD11

Saturated temperature limit switch: TD21

#### **Intelligent Diagnostics**

- None\*

Integrity test: VM51 replace by VE51, VM11 replace by VE11, PA31, TA31, VE32, VE33

- Performance monitoring: TA01. TA21, TA31, TA51, TA52, FA01, PA31 and PA01

System diagnostics: VB01, VB31, PA31, TA01, TA11 (when pre-heater is fitted), TA31, TA51 and TA51 (when pre-heater is not fitted)

With pneumatic control or Integrity test: PDX1

- Without integrated pump: PA01

# Clean steam outlet isolation valve

- None\*

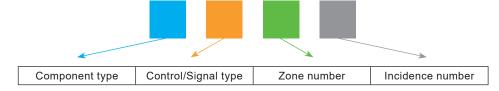
Manual Valve: VM21

Automated valve: VE21, VD21 and VD22

# 9.3 Component naming convention

The naming convention for the system map do not correlate to the specific parts and part numbers. The tag names are specific to the CSG-FB system and are not tied to specific component models. To identify a particular component, reference the component tag number to the Bill Of Materials for the specific model of CSG-FB.

The tag numbers can be deciphered to aid identification and location of the component on the CSG-FB.



#### 9.3.1 Component types

Opposite is a table of currently identified component types.

Letter	Component type
С	Conductivity
F	Flow sensor
Н	Heat exchanger (preheater, sample cooler, etc)
L	Level sensor
Р	Pressure sensor
Q	Trap (steam, air eliminator, etc)
s	Separator
Т	Temperature sensor
V	Valve (globe, ball, check, vacuum breaker, butterfly, etc)
w	Water vessel (pressure buffer, storage, etc)
Y	Strainer

# 9.3.2 Control/signal type

Opposite is a table of currently identified Control and Signal types. The direction of signals is always reference in relation to the PLC or process controller.

Letter	Control/Signal type
Α	Analogue input (signal)
В	Analogue output (control)
D	Digital input
E	Digital output
I	Indicator (non-electrical, dial, etc)
М	Manual control
U	Un-controlled (check valve, strainer, separator, etc)

# 9.3.3 Zone allocation

Zones are used to segregate areas of the package into sub-areas based around state changes of the process of the package.

Numbering of the Zones begins with the inlet flow of the process fluid at Zone 0. When the process fluid undergoes a change or state change, the Zone number increases until it leaves the CSG-FB.

The inlet of the control fluid begins with the next available Zone number. At each state change of the control fluid, increase the Zone number until the control fluid leaves the package.

Components located externally to the steam system are always labelled as Zone X.

#### 9.3.4 Incidence number

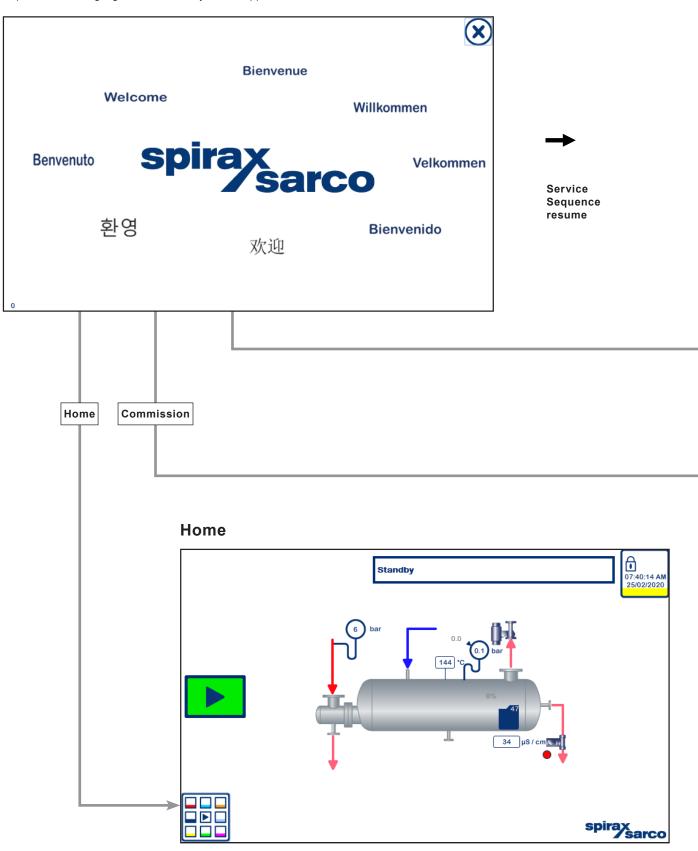
Where multiples of similar devices and parts occur in the same zone, incidence numbers are used to distinguish between them.

Starting points for incidence numbers always start from the component closest the entry of the Zone area.

e.g. On a condensate line, 2 manual valves are identified in Zone 5. The first of the manual valves to come into contact with the condensate as it passes through zone 5 will be given the Incidence number 1.

# 10. HMI map

The following map shows the screens available to all users. Some screens will require a security password to access. The minimum required level is highlighted with the Key shown opposite.



# Level key

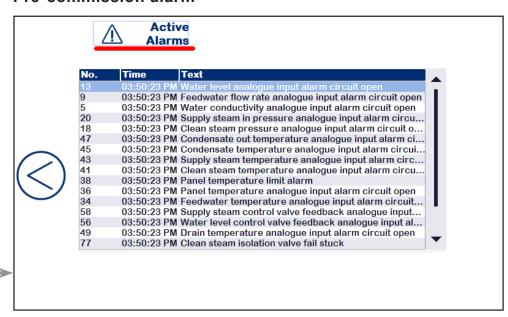




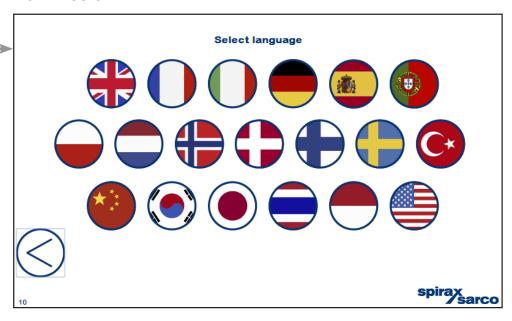


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# Pre-commission alarm

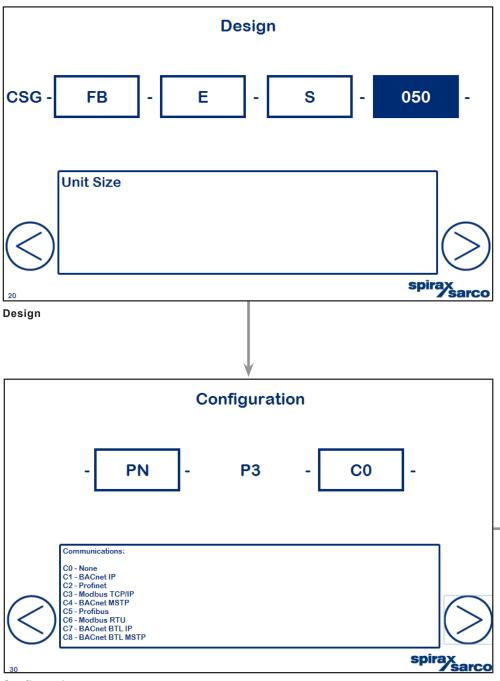


# Commission

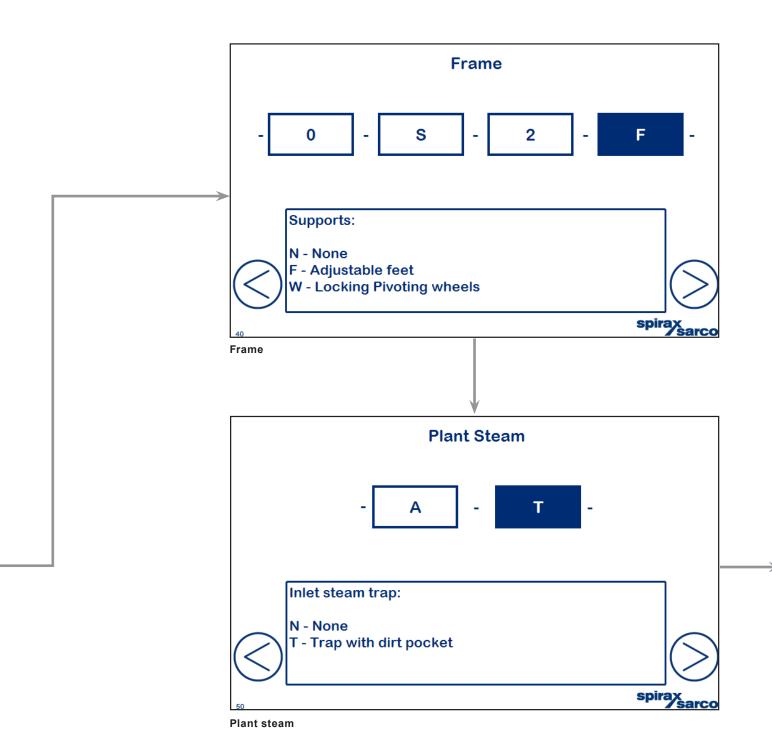


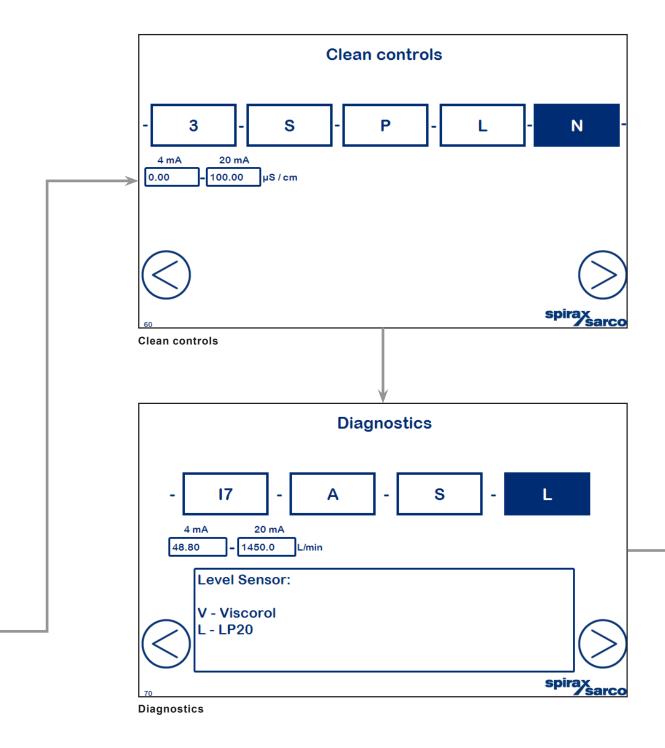
# 10.1 Commissioning screens

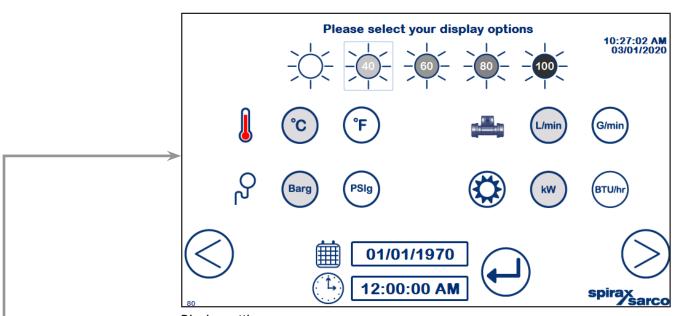
The commissioning screens allow users to input the configuration of the CSG-FB into the control system using the model specific nomenclature. These are generated at the point of ordering and must be referenced to ensure correct operation of the CSG-FB.



Configuration







CSG-FB Clean steam generation system for Food & Beverage

# 10.2 Home screen

The home screen (100) gives the user the ability to quickly view the essential parameters and run status of the CSG-FB. Additionally, more detailed parameters and process values are quickly and easily accessible.

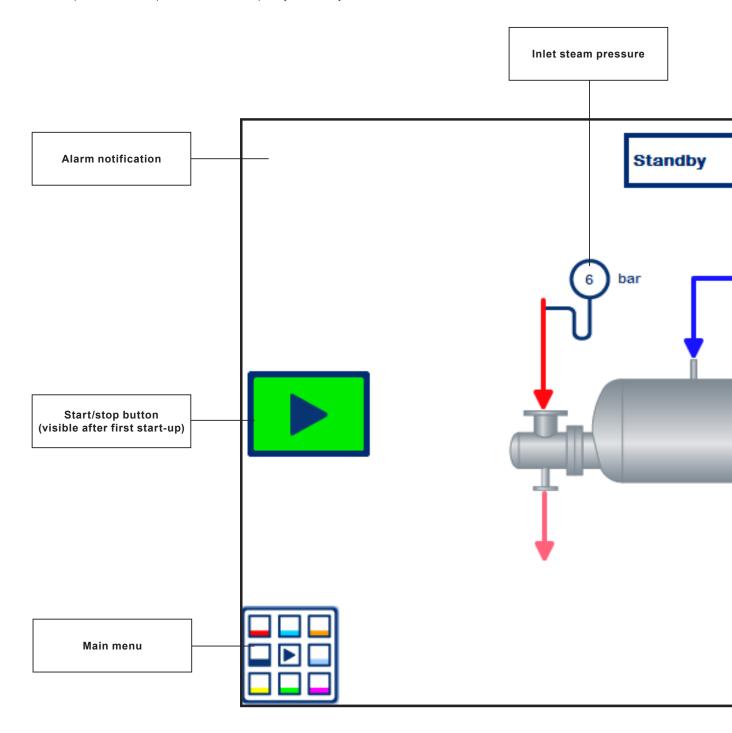
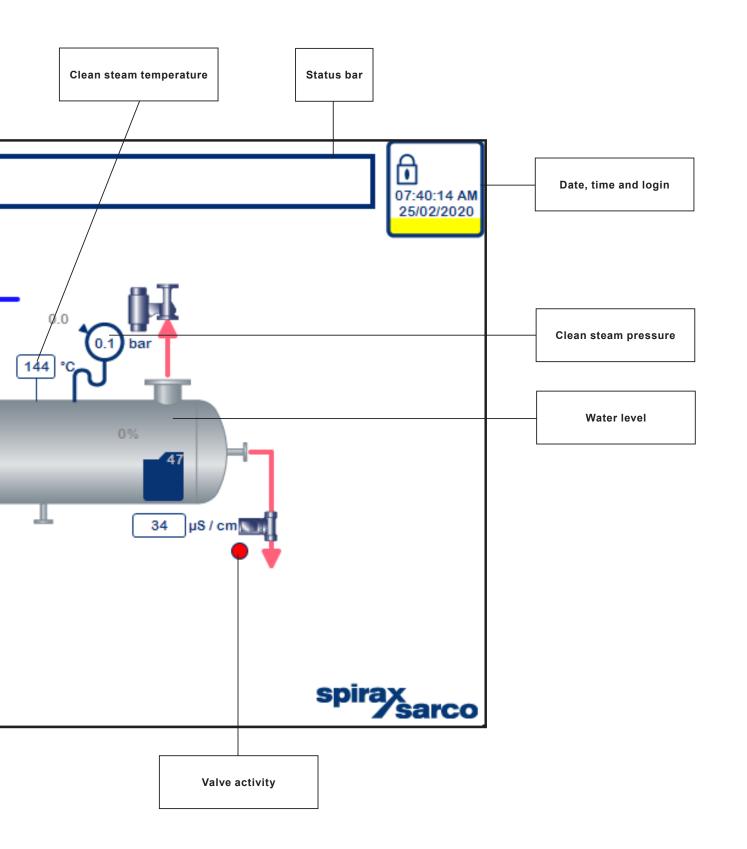


Fig. 10

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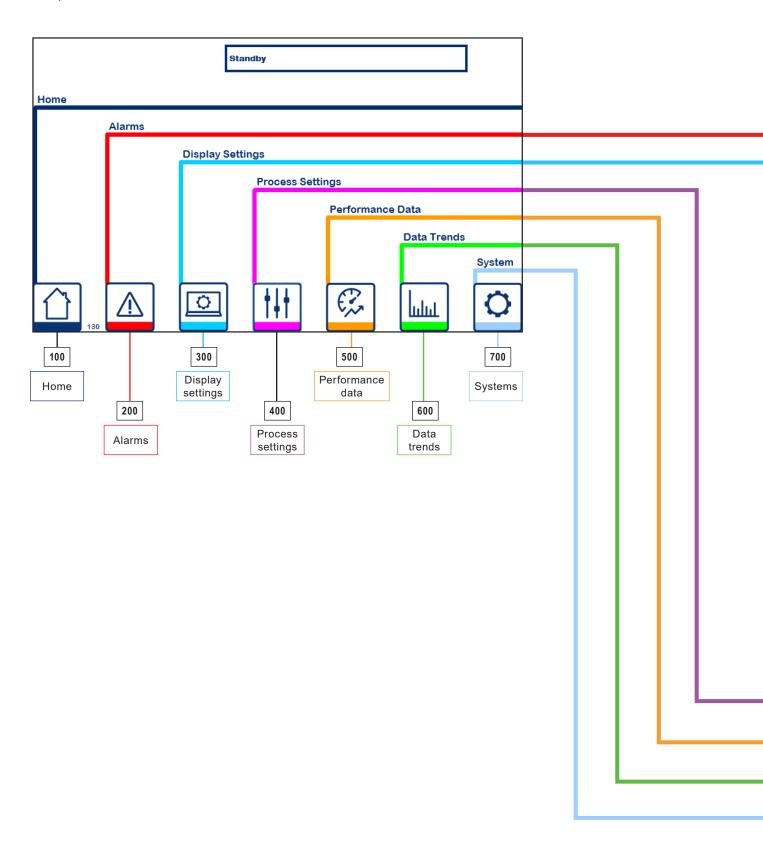
CSG-FB Clean steam generation system for Food & Beverage

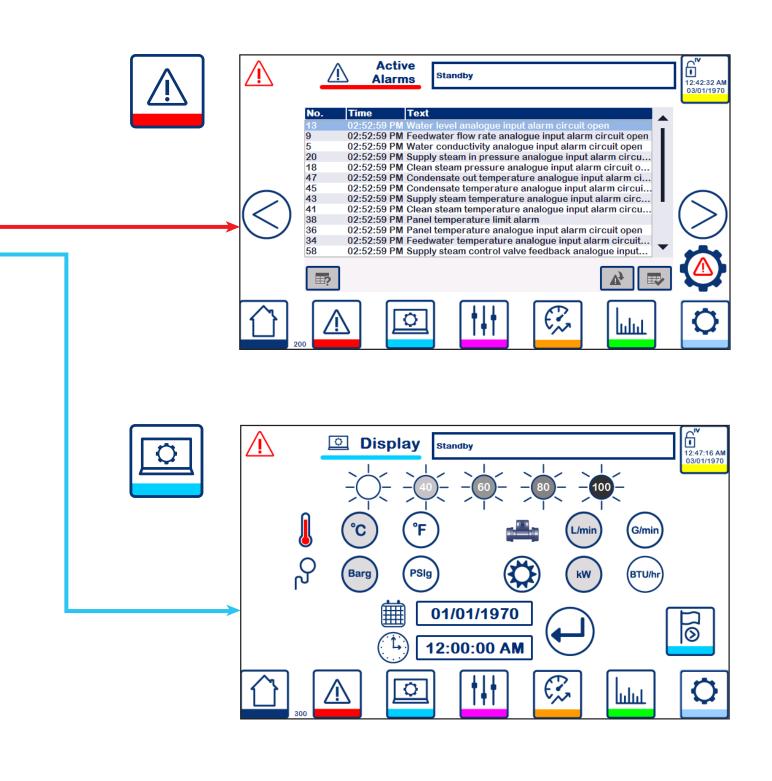


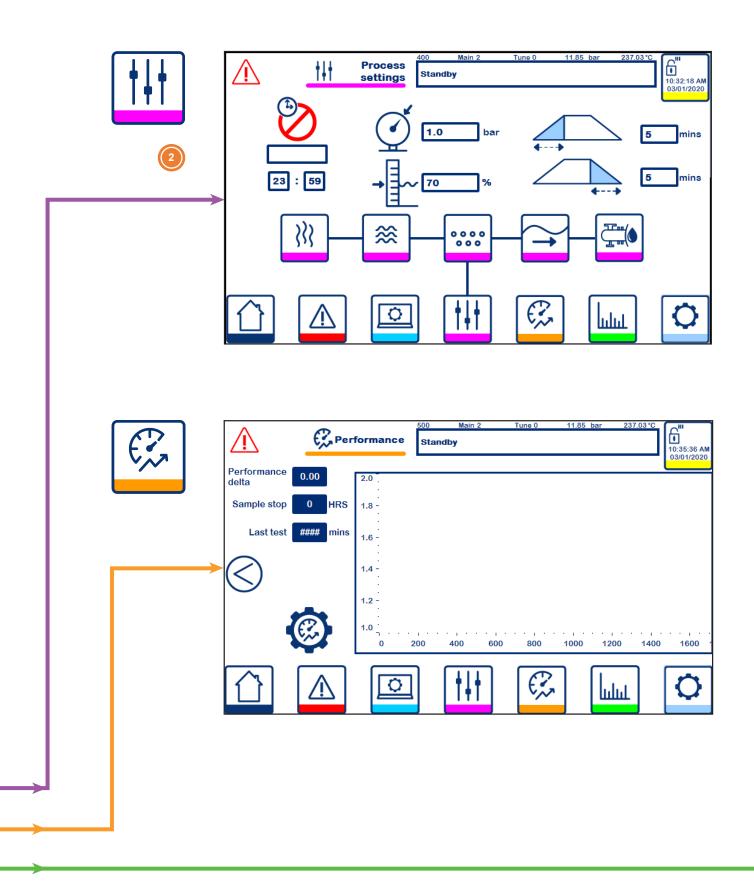
# 10.3 Main menu

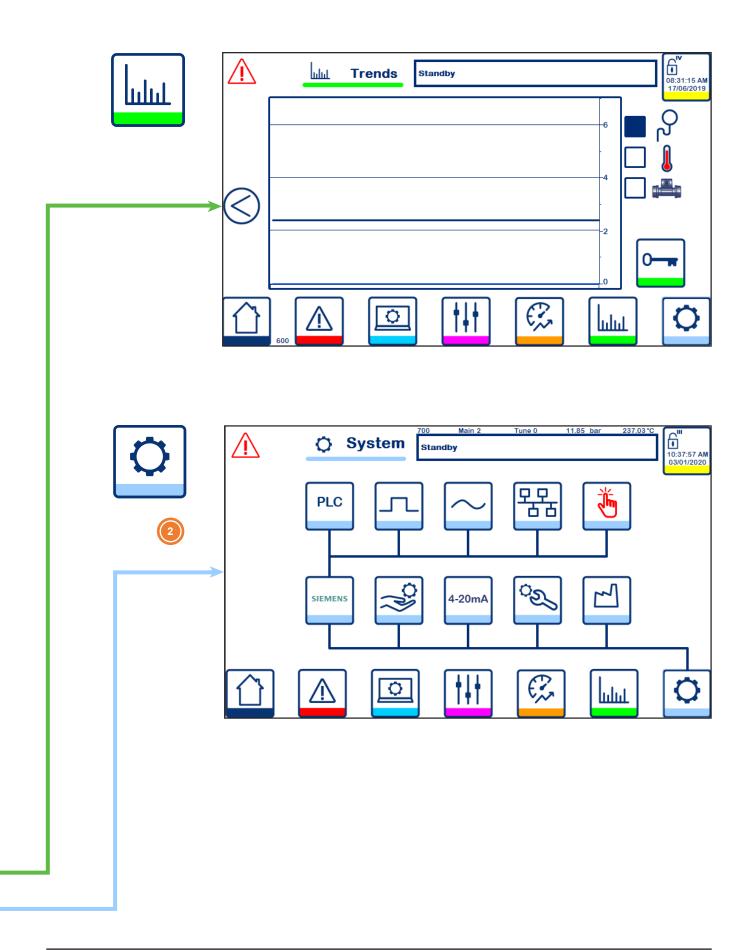
90

By selecting the Main Menu button from the Home screen, the user has access to settings, alarms and diagnostics screens. These are split in to 6 sub-menus as described below.







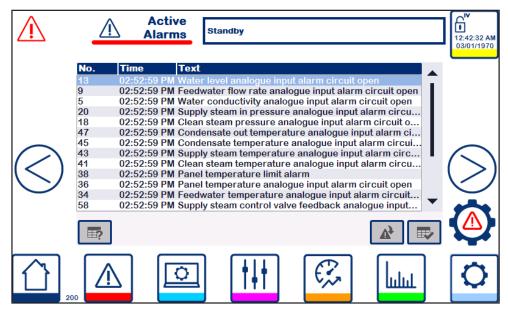


#### 10.4 Alarms

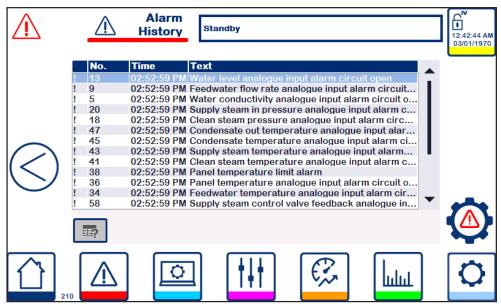
94

The alarm screens display active and historic alarms as well as all the settings for the diagnostics alarms.

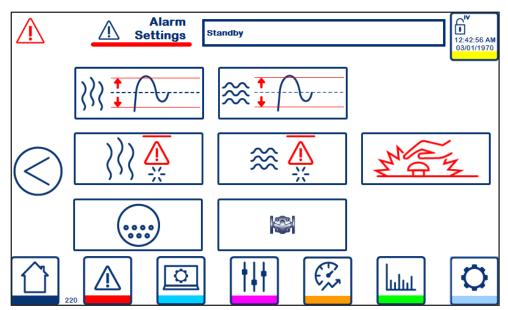




Active alarms (200) remains on screen until they are acknowledged by the user.



Alarms history (210) provides an historic log of previous alarms including time and date stamp for clarification and diagnosis. A rolling total of 1024 alarms are retained until a power cycle of the CSG-FB.

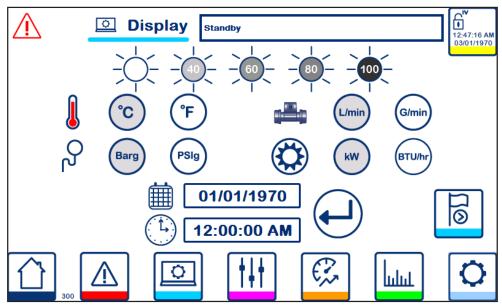


Alarm settings (220)

# 10.5 Display settings

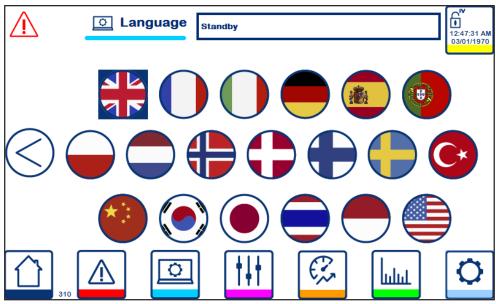
The display settings screen, as well as altering the display units for the HMI, the user can also alter the time, date and language.





Display settings (300)





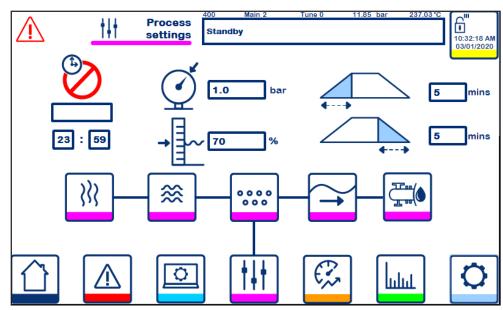
Language (310)

# 10.6 Process settings

The settings available across the process settings screens directly affect the running of the CSG-FB and the effective output of clean steam.



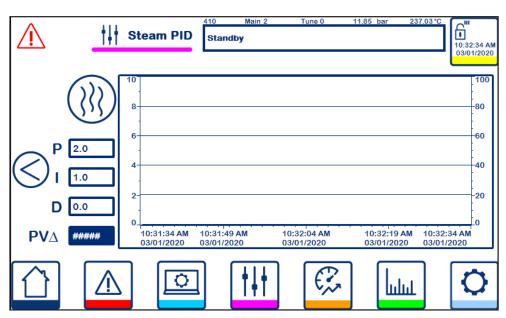




Main process set-points (400). Including clean steam pressure, water level, ramp up time and ramp down time.





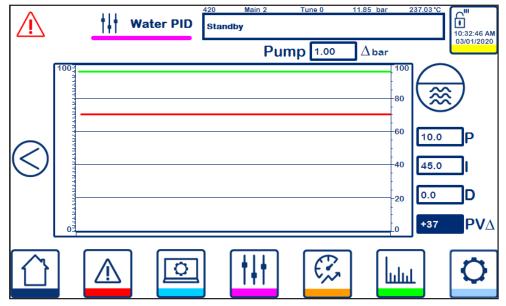


Steam PID settings (410) also includes a live PID graph showing the process and control values, and the process set-point.

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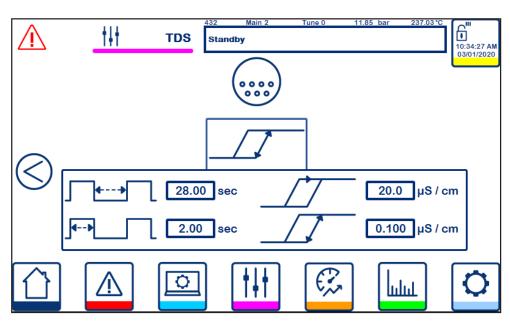




Water PID settings (420) also includes the pump offset value and a live PID graph showing the process and control values, and the process set-point.





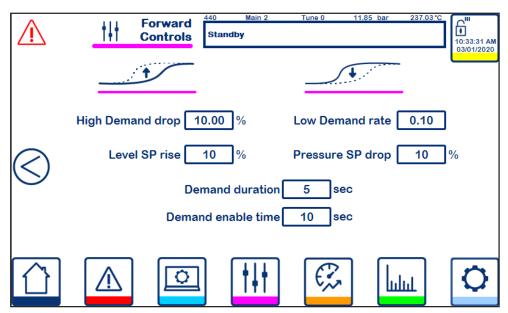


TDS settings (430-432) allows the user to set and select the TDS control they require.

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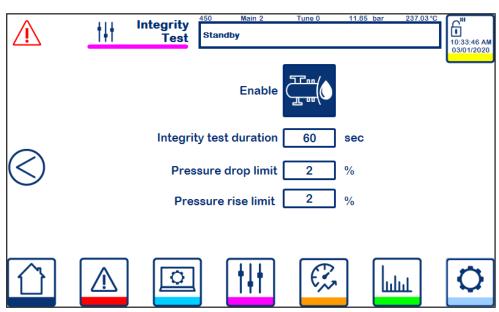




Forward controls (440)



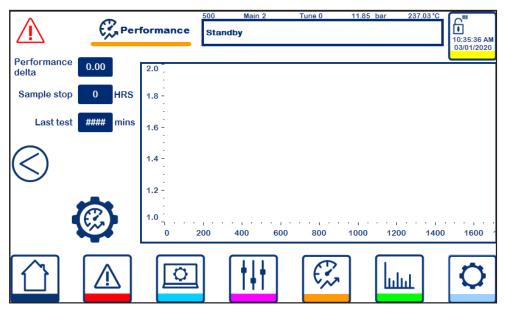




Integrity test (450)

#### 10.7 Performance data

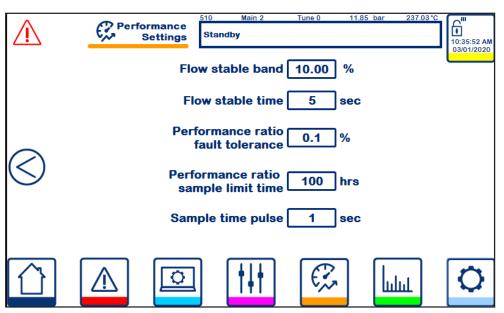
The performance data screen will only display the performance profile of the CSG-FB whist in Running mode and once sufficient data has been collected. If the Performance Monitoring options pack has not been installed, no information will be available.



Performance data (500), as well as showing the current performance profile of the CSG-FB also shows the current data sample and data times.



100



Performance data settings (510) allows users to alter the sampling process and performance tolerance.

# 10.8 Data trends

The live data displayed on the Trends screen is grouped in to similar process values.



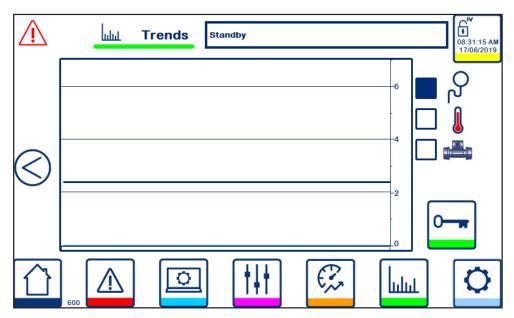
Pressure variables.
All currently installed pressure sensors.



Temperature variables. All currently installed temperature sensors.



Flow variable from FA01 if installed.



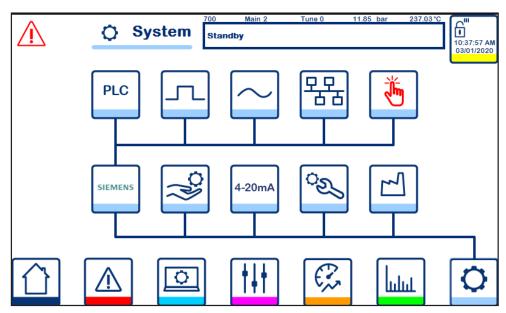
Trends (600) provided a live feed of the selected process variables.

# 10.9 System

System related controls and settings are available for the advanced user to alter the CSG-FB away from a pre-configured settings.

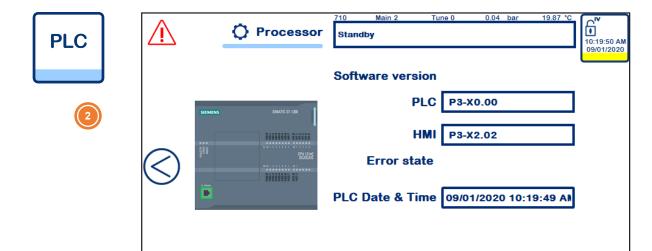






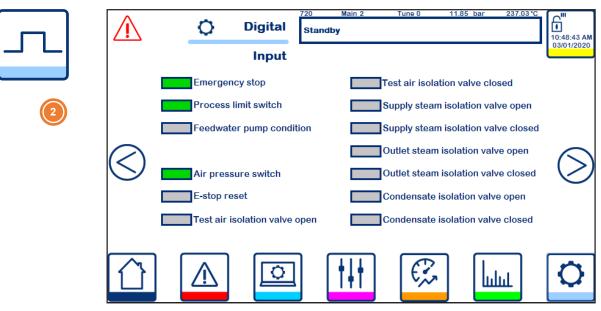
System sub menu (700)

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PLC status (710) displays any PLC error codes and the stored PLC date and time.

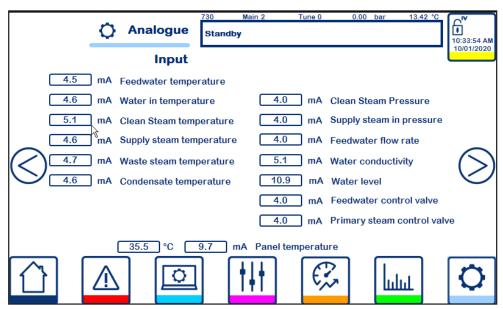
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Digital Input status (720) and digital output status (721)



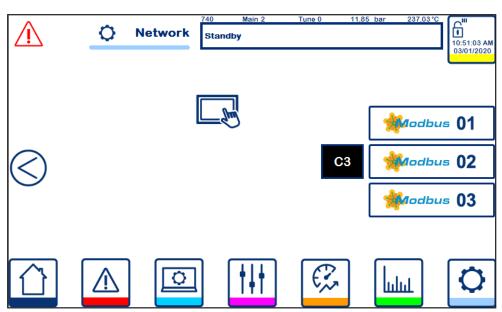




Analogue input status (730) and analogue output status (731)

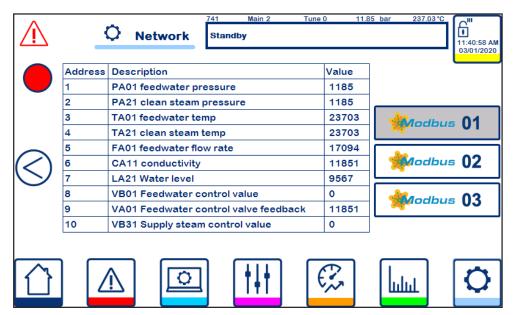






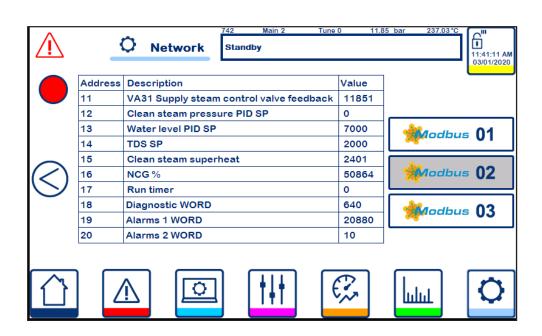
Network status (740)



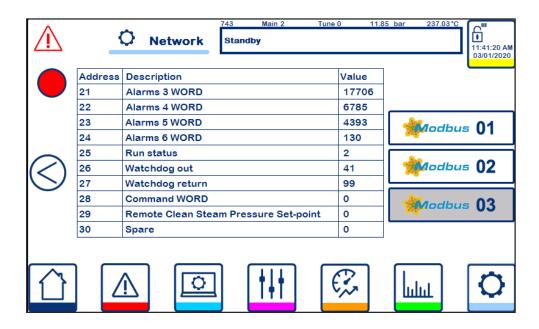


Communications tables and status (741-745)

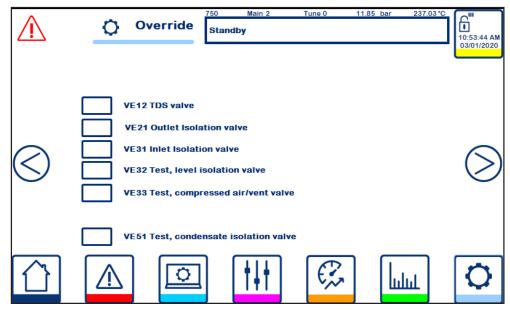












Digital override (750) open and close fitted and available isolation valves (only available in standby mode)



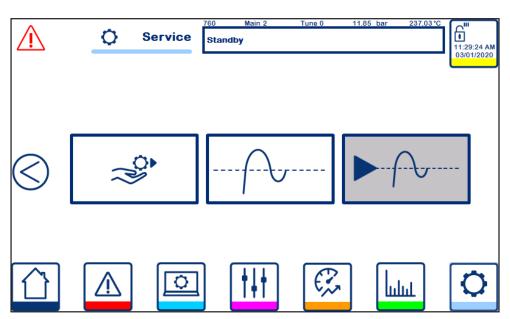




Analogue override (751) enable and move control valves to specific position. (only available in standby mode)



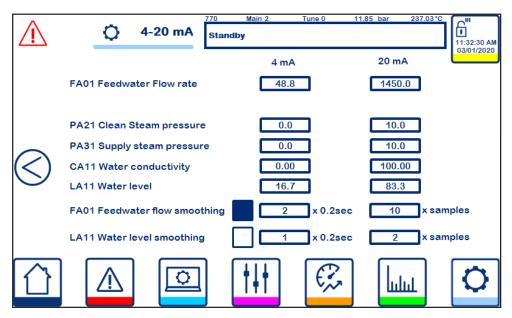




Service (760) allows users to begin service sequence‡, enter PID Tuning mode (only available in standby mode) or Running Tuning mode (only available when in Run mode).



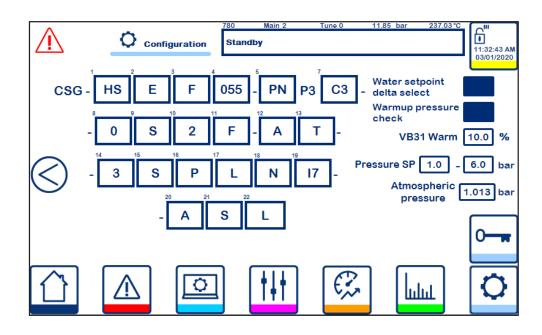




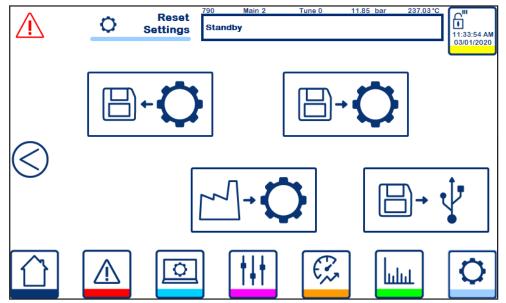
Scaling (770) allows alteration of the 4-20 mA input scaling and the input smoothing of FA01 and LA11 (only available in standby mode).





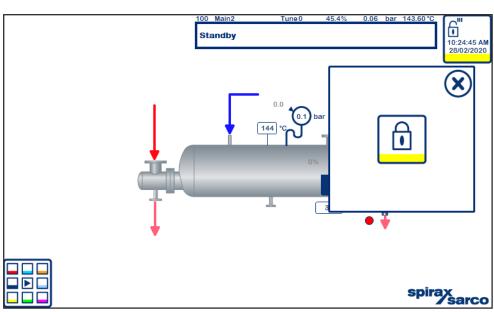






Factory reset (790) allows users to save, load and reset the current settings and configuration of the CSG-FB. (only available in standby mode)





Security screen (800), allows users to logoff from the current user.

# 11. Appendix

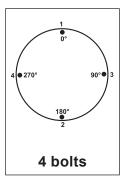
The torqueing procedure should follow the steps detailed in this Appendix:

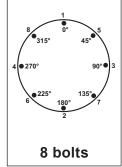
- Lubricate the bolt threads and the nut faces with a suitable lubricant.
- Insert the bolts through the flanges and finger tighten the nuts.
- Number all bolts so that torqueing requirements can be followed.
- Apply torque in 20%, 1/5 steps of required final torque, loading all bolts at each step before proceeding to the next step.
- Use rotational tightening until all bolts are stable at final torque level.

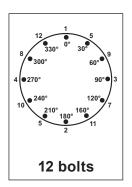
The torque tightening values for the clean steam generator header and deareator flanges are detailed in the following table:

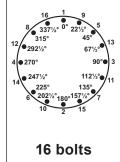
	Hea	der flange b	olts	Deaerator flange bolts			
	Quantity Ø Torque* (N m)		Quantity Ø		Torque* (N m)		
GVS400	4	M14	25	12	M20	50	
GVS500	8	M16	40	12	M24	80	
GVS601	12	M16	45	16	M27	125	
GVS602	12	M16	45	16	M27	125	

<sup>\*</sup> Gaskets as per original spare parts









Sequential Order	Rotational Order
1-2	1
3-4	3
	2
	4

Sequential Order	Rotation: Order
1-2	1
3-4	5
5-6	3
7-8	7
	2
	6
	4
	8

Sequential	Rotationa
Order	Order
1-2	1
3-4	5
5-6	9
7-8 9-10	3
11-12	7
	11
	2
	6
	10
	4
	8
	12

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	Setting	Units	Lower limit	Upper limit	Default	Setting
	Alarm settings					
}}}	Clean steam pressure band alarr	n				
1	High band	%	1.0	10.0	10.0	
•	Low band	%	1.0	10.0	10.0	
	Alert time	sec	1	30	10	
	Alarm time	sec	30	180	30	
<b>≋:</b> /∿	Water level band alarm					
·•	High band	%	1.0	10.0	10.0	
<b>.</b>	Low band	%	1.0	10.0	10.0	
	Alert time	sec	1	30	10	
	Alarm time	sec	30	180	30	
\\\\\ <u>\</u>	Clean steam control capacity ala	ırm				
	Alert time	sec	1	60	30	
<u>^</u>	Alarm time	sec	1	60	60	
<b>≈</b> <del></del> <del>\</del> <del>\</del> <del>\</del> <u>\</u> <del>\</del> <del>\</del>	Water level control capacity alar	m				
<u>^</u>	Alert time	sec	1	60	30	
<u> </u>	Alarm time	sec	1	60	60	
••••	TDS alarm					
<b></b>	TDS high time	sec	0	600	600	
<b>⊕</b>	Hysteresis time	sec	0	600	600	
	Water level band alarm					
<b>}}}<b> </b></b>	Trap fail open temperature difference	°C			15.0	
	Trap fail closed temperature	°C			15.0	
	Maximum water level valve opening	sec	0.0	20.0	5.0	
	Maximum clean steam valve opening	sec	0.0	20.0	10.0	
† † †	Process settings					
	Main process					
$\bigcirc$	Clean steam pressure	bar	1.0	6.0	1.0	
<b>→</b>	Water level	%	60	80	70	
<b>—</b>	Ramp up time	min	2	10	5	
4	Ramp down time	min	2	10	5	
	Timed shut-down	time	00:00	23:59	disabled	
3;3	Clean Steam PID					
	Proportional gain	-	1.0		2.0	
	Integral gain	-	0.0		1.0	
	Derivative gain	-	0.0		0.0	

	Setting	Units	Lower limit	Upper limit	Default	Setting
<b>**</b>	Water level PID					
	Proportional gain	-	1.0		10.0	
	Integral gain	-	0.0		45.0	
	Derivative gain	-	0.0		0.0	
	Pump pressure	∆bar	0.5	2.0	1.0	
0000	TDS (Interval only)					
<b></b>	Interval time	sec	5.00		28.00	
<b></b>	Duration time	sec	0.00		2.00	
0000	TDS (CP10)					
<b></b>	Interval time	sec	5.00		28.00	
<b>√</b>	Duration time	sec	0.00		2.00	
	TDS setpoint	μS	10.0		35.0	
	Hysteresis band	μS	0.001	20.000	0.100	
0000	TDS (CP32)					
<b></b>	Interval time	sec	5.00		28.00	
<b>√</b>	Duration time	sec	0.00		2.00	
	TDS setpoint	μS	10.0		35.0	
	Hysteresis band	μS	0.001	20.000	0.100	
$\widetilde{\hspace{1cm}}$	Forward Controls					
	High Demand drop	%	5.00	20.00	10.00	
	Level SP rise	%			10	
	Low Demand rate		0.00	1.00	0.10	
	Pressure SP drop	%			10	
	Demand duration	sec	1	10	5	
	Demand enable time	sec	1	60	10	
	Integrity test				Enable	
	Integrity test duration	sec			60	
	Pressure drop limit	%	-100	-1	-2	
	Pressure rise limit	%	100	1	2	
<b>®</b>	Performance Monitoring					
	Flow stable band	%			10.00	
	Flow stable time	sec			5	
	Performance ratio fault tolerance	%			0.1	
	Performance ratio sample limit time	hrs			100	
	Sample time pulse				1	
	Sample unie puise	sec				

	Setting	Units	Lower limit	Upper limit	Default	Setting
4-20mA	4-20mA					
	FA01 4mA	L/min			48.80	
	FA01 20mA	L/min			1450.0	
	PA01 4mA	bar			0.00	
	PA01 20mA	bar			10.0	
	PA21 4mA	bar			0.00	
	PA21 20mA	bar			10.0	
	PA31 4mA	bar			0.00	
	PA31 20mA	bar			10.0	
	CA11 4mA	μS			0.0	
	CA11 20mA	μS			100.0	
	LA11 4mA (Viscorol)	%			0.0	
	LA11 20mA (Viscorol)	%			100.0	
	LA11 4mA (LP20)	%			16.7	
	LA11 20mA (LP20)	%			83.3	
	FA01 Feedwater flow smoothing				Enable	
	FA01 smothing interval	0.2sec			2	
	FA01 smothing samples				10	
	LA11 Water level smoothing				Disable	
	LA11 smothing interval	0.2sec			1	
	LA11 smothing samples				2	
్ర్ప	Configuration					
	Water setpoint delta select  Warmup pressure check			Enable		
				Enable		
	VB31 warm	%			10.0	
	Pressure SP minimum	bar	0.0	10.0	1.0	
	Pressure SP maximum	bar	0.0	10.0	6.0	
	Atmospheric Pressure	barA			1.013	



# **Service**

For technical assistance contact our nearest Office or Agency or contact directly:

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# Warranty

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Ascertained partial or complete non-compliance with these regulations will result in forfeiture of the related warranty.